

# Property Library for Hydrogen Sulfide

LibH2S

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# **Property Functions**

Functional Dependence	Function Name	Call from Fortran Program	Property or Function	Unit of the Result
a = f(p,t,x)	a_ptx_H2S	A_PTX_H2S(P,T,X)	Thermal diffusivity	m²/s
$c_{p} = f(p,t,x)$	cp_ptx_H2S	CP_PTX_H2S(P,T,X)	Specific isobaric heat capacity	kJ/(kg K)
$c_{V} = f(p,t,x)$	cv_ptx_H2S	CV_PTX_H2S(P,T,X)	Specific isochoric heat capacity	kJ/(kg K)
$\eta = f(p,t,x)$	eta_ptx_H2S	ETA_PTX_H2S(P,T,X)	Dynamic viscosity	Pa.s
h = f(p,t,x)	h_ptx_H2S	H_PTX_H2S(P,T,X)	Specific enthalpy	kJ/kg
$\kappa = f(p,t,x)$	ka_ptx_H2S	KA_PTX_H2S(P,T,X)	Isentropic exponent	-
$\lambda = f(p,t,x)$	lam_ptx_H2S	LAM_PTX_H2S(P,T,X)	Thermal conductivity	W/(m . K)
v = f(p,t,x)	ny_ptx_H2S	NY_PTX_H2S(P,T,X)	Kinematic viscosity	m²/s
Pr = f(p,t,x)	pr_ptx_H2S	PR_PTX_H2S(P,T,X)	Prandtl-number	-
$p_s = f(t)$	ps_t_H2S	PS_T_H2S(T)	Vapor pressure from temperature	bar
$\rho$ = f( $p$ , $t$ , $x$ )	rho_ptx_H2S	RHO_PTX_H2S(P,T,X)	Density	kg/m <sup>3</sup>
s = f(p,t,x)	s_ptx_H2S	S_PTX_H2S(P,T,X)	Specific entropy	kJ/(kg K)
$\sigma$ = f(t)	sigma_t_H2S	SIGMA_T_H2S(T)	Surface tension from temperature	N/m
t = f(p,h)	t_ph_H2S	T_PH_H2S(P,H)	Backward function: Temperature from pressure and enthalpy	°C
t = f(p,s)	t_ps_H2S	T_PS_H2S(P,S)	Backward function: Temperature from pressure and entropy	°C
$t_{\rm S} = f(p)$	ts_p_H2S	TS_P_H2S(P)	Saturation temperature from pressure	°C
u = f(p,t,x)	u_ptx_H2S	U_PTX_H2S(P,T,X)	Specific internal energy	kJ/kg
v = f(p,t,x)	v_ptx_H2S	V_PTX_H2S(P,T,X)	Specific volume	m³/kg
w = f(p,t,x)	w_ptx_H2S	W_PTX_H2S(P,T,X)	Isentropic speed of sound	m/s

Functional Dependence	Function Name	Call from Fortran Program	Property or Function	Unit of the Result
x = f(p,h)	x_ph_H2S	X_PH_H2S(P,H)	Backward function: Vapor fraction from pressure and enthalpy	kg/kg
x = f(p,s)	x_ps_H2S	X_PS_H2S(P,S)	Backward function: Vapor fraction from pressure and entropy	kg/kg

Units:  $t \text{ in } ^{\circ}\text{C}$ 

*p* in bar

x in (kg saturated steam)/(kg wet steam)

# Range of validity

Temperature range: from - 85.45 °C to 486.85 °C Pressure range: from 0.23259 bar to 1700 bar

### Reference state

h = 0 kJ/kg and s = 0 kJ/(kg K) at p = 1,01325 bar on the saturated liquid line (x = 0)

## Details on the vapor fraction x

The wet steam region is calculated automatically by the subprograms. For this purpose the following fixed details on the vapor fraction x are to be considered:

#### Single-phase region

If the state point to be calculated is located in the single-phase region (liquid or superheated steam) x = -1 must be entered as a pro-forma value.

#### Wet-steam region

If the state point to be calculated is located in the wet steam region, a value for x between 0 and 1 (x = 0 for saturated liquid, x = 1 for saturated steam) must be entered. In this case, the backward functions result in the appropriate value between 0 and 1 for x. When calculating wet steam either the given value for t and t = -1000 or the given value for t and t = -1000 and in both cases the value for t between 0 and 1 must be entered.

If p and t and x are entered as given values, the program considers p and t to be appropriate to represent the vapor pressure curve. If this is not the case the calculation for the property of the chosen function results in -1.

Wet steam region: Temperature ranges from  $t_{min} = -85.45 \,^{\circ}\text{C}$  to  $t_{c} = 99.95 \,^{\circ}\text{C}$ 

Pressure ranges from  $p_{min} = 0.23259$  bar to  $p_{c} = 89.987$  bar

#### Note:

If the input values are located outside the range of validity, the calculated function will always result in –1000. Please find more exact details on every function and its corresponding range of validity in the enclosed program documentation in Chapter 3.