

# Property Library for Ethanol

**LibC2H5OH**

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## Property Functions

Functional Dependence	Function Name	Call from Fortran Program	Property or Function	Unit of the Result
$a = f(p,t,x)$	a_ptx_C2H5OH	A_PTX_C2H5OH(P,T,X)	Thermal diffusivity	m <sup>2</sup> /s
$c_p = f(p,t,x)$	cp_ptx_C2H5OH	CP_PTX_C2H5OH(P,T,X)	Specific isobaric heat capacity	kJ/(kg K)
$\eta = f(p,t,x)$	eta_ptx_C2H5OH	ETA_PTX_C2H5OH(P,T,X)	Dynamic viscosity	Pa . s
$h = f(p,t,x)$	h_ptx_C2H5OH	H_PTX_C2H5OH(P,T,X)	Specific enthalpy	kJ/kg
$\kappa = f(p,t,x)$	ka_ptx_C2H5OH	KA_PTX_C2H5OH(P,T,X)	Isentropic exponent	-
$\lambda = f(p,t,x)$	lam_ptx_C2H5OH	LAM_PTX_C2H5OH(P,T,X)	Thermal conductivity	W/(m . K)
$\nu = f(p,t,x)$	ny_ptx_C2H5OH	NY_PTX_C2H5OH(P,T,X)	Kinematic viscosity	m <sup>2</sup> /s
$Pr = f(p,t,x)$	pr_ptx_C2H5OH	PR_PTX_C2H5OH(P,T,X)	Prandtl-number	-
$p_s = f(t)$	ps_t_C2H5OH	PST_C2H5OH(T)	Vapor pressure from temperature	bar
$\rho = f(p,t,x)$	rho_ptx_C2H5OH	RHO_PTX_C2H5OH(P,T,X)	Density	kg/m <sup>3</sup>
$s = f(p,t,x)$	s_ptx_C2H5OH	S_PTX_C2H5OH(P,T,X)	Specific entropy	kJ/(kg K)
$\sigma = f(t)$	sigma_t_C2H5OH	SIGMA_T_C2H5OH(T)	Surface tension from temperature	N/m
$t = f(p,h)$	t_ph_C2H5OH	T_PH_C2H5OH(P,H)	Backward function: Temperature from pressure and enthalpy	°C
$t = f(p,s)$	t_ps_C2H5OH	T_PS_C2H5OH(P,S)	Backward function: Temperature from pressure and entropy	°C
$t_s = f(p)$	ts_p_C2H5OH	TSP_C2H5OH(P)	Saturation temperature from pressure	°C
$u = f(p,t,x)$	u_ptx_C2H5OH	U_PTX_C2H5OH(P,T,X)	Specific internal energy	kJ/kg
$v = f(p,t,x)$	v_ptx_C2H5OH	V_PTX_C2H5OH(P,T,X)	Specific volume	m <sup>3</sup> /kg
$w = f(p,t,x)$	w_ptx_C2H5OH	W_PTX_C2H5OH(P,T,X)	Isentropic speed of sound	m/s

$x = f(p,h)$	x_ph_C2H5OH	X_PH_C2H5OH(P,H)	Backward function: Vapor fraction from pressure and enthalpy	kg/kg
$x = f(p,s)$	x_ps_C2H5OH	X_PS_C2H5OH(P,S)	Backward function: Vapor fraction from pressure and entropy	kg/kg

**Units:**

- $t$  in °C
- $p$  in bar
- $x$  in (kg saturated steam)/(kg wet steam)

### Range of validity

Temperature range: from - 114.15°C to 376.85 °C  
 Pressure range: from  $p_t = 7.2 \times 10^{-9}$  bar to 2800 bar

### Reference state

$h = 200 \text{ kJ/kg}$  and  $s = 1 \text{ kJ/(kg K)}$  at  $t = 0 \text{ }^\circ\text{C}$  on the saturated liquid line ( $x = 0$ )

### Details on the vapor fraction $x$

The wet steam region is calculated automatically by the subprograms. For this purpose the following fixed details on the vapor fraction  $x$  are to be considered:

#### Single-phase region

If the state point to be calculated is located in the single-phase region (liquid or superheated steam)  $x = -1$  must be entered as a pro-forma value.

#### Wet-steam region

If the state point to be calculated is located in the wet steam region, a value for  $x$  between 0 and 1 ( $x = 0$  for saturated liquid,  $x = 1$  for saturated steam) must be entered. In this case, the backward functions result in the appropriate value between 0 and 1 for  $x$ . When calculating wet steam either the given value for  $t$  and  $p = -1000$  or the given value for  $p$  and  $t = -1000$  and in both cases the value for  $x$  between 0 and 1 must be entered.

If  $p$  and  $t$  and  $x$  are entered as given values, the program considers  $p$  and  $t$  to be appropriate to represent the vapor pressure curve. If this is not the case the calculation for the property of the chosen function results in -1.

Wet steam region: Temperature ranges from  $t_{\min} = -114.15 \text{ }^\circ\text{C}$  to  $t_c = 241.56 \text{ }^\circ\text{C}$   
 Pressure ranges from  $p_{\min} = 7.2 \times 10^{-9}$  bar to  $p_c = 62.68 \text{ bar}$

### Note:

*If the input values are located outside the range of validity, the calculated function will always result in -1000. Please find more exact details on every function and its corresponding range of validity in the enclosed software documentation in Chapter 3.*