

# Property Library for Ammonia-Water Mixtures

## LibButan\_n

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## Property Functions

Functional Dependence	Function Name	Call from Fortran program	Property or Function	Unit of the result
$a = f(p, t, x)$	a_ptx_BUTN	APTxBUTN(P, T, X)	Thermal diffusivity	m <sup>2</sup> /s
$c_p = f(p, t, x)$	cp_ptx_BUTN	CPPTxBUTN(P, T, X)	Specific isobaric heat capacity	kJ/(kg K)
$c_v = f(p, t, x)$	cv_ptx_BUTN	CVPTxBUTN(P, T, X)	Specific isochoric heat capacity	kJ/(kg K)
$\eta = f(p, t, x)$	eta_ptx_BUTN	ETAPTxBUTN(P, T, X)	Dynamic viscosity	Pa s
$h = f(p, t, x)$	h_ptx_BUTN	HPTxBUTN(P, T, X)	Specific enthalpy	kJ/kg
$\kappa = f(p, t, x)$	kappa_ptx_BUTN	KAPTxBUTN(P, T, X)	Isentropic exponent	-
$\lambda = f(p, t, x)$	lambda_ptx_BUTN	LAMPTxBUTN(P, T, X)	Thermal conductivity	W/(m K)
$\nu = f(p, t, x)$	ny_ptx_BUTN	NYPTxBUTN(P, T, X)	Kinematic viscosity	m <sup>2</sup> /s
$p_{\text{mel}} = f(t)$	pmel_t_BUTN	PMELBUTN(T)	Melting pressure from temperature	bar
$p_s = f(t)$	ps_t_BUTN	PSTBUTN(T)	Vapor pressure from temperature	bar
$Pr = f(p, t, x)$	Pr_ptx_BUTN	PRPTxBUTN(P, T, X)	<i>Prandtl</i> -Number	-
$\rho = f(p, t, x)$	rho_ptx_BUTN	ROPTxBUTN(P, T, X)	Density	kg/m <sup>3</sup>
$s = f(p, t, x)$	s_ptx_BUTN	SPTxBUTN(P, T, X)	Specific entropy	kJ/(kg K)
$t = f(p, h)$	t_ph_BUTN	TPHBUTN(P, H)	Backward function: Temperature from pressure and enthalpy	°C
$t = f(p, s)$	t_ps_BUTN	TPSBUTN(P, S)	Backward function: Temperature from pressure and entropy	°C
$t_{\text{mel}} = f(p)$	tmel_p_BUTN	TMELBUTN(P)	Melting temperature from pressure	°C
$t_s = f(p)$	ts_p_BUTN	TSPBUTN(P)	Saturation temperature from pressure	°C
$u = f(p, t, x)$	u_ptx_BUTN	UPTxBUTN(P, T, X)	Specific internal energy	kJ/kg
$v = f(p, t, x)$	v_ptx_BUTN	VPTxBUTN(P, T, X)	Specific volume	m <sup>3</sup> /kg
$w = f(p, t, x)$	w_ptx_BUTN	WPTxBUTN(P, T, X)	Isentropic speed of sound	m/s
$x = f(p, h)$	x_ph_BUTN	XPHBUTN(P, H)	Backward function: Vapor fraction from pressure and enthalpy	kg/kg
$x = f(p, s)$	x_ps_BUTN	XPSBUTN(P, S)	Backward function: Vapor fraction from pressure and entropy	kg/kg
$z = f(p, t, x)$	z_ptx_BUTN	ZPTxBUTN(P, T, X)	Compression factor	-

**Units:**

$t$  in °C

$p$  in bar

$x$  in (kg of saturated steam)/(kg wet steam)

**Range of validity**

Temperature range: from  $t_{\text{mel}}(p)$  to 301.85 °C

Pressure range: from  $p_t = 6.53 \times 10^{-6}$  bar to 690 bar

**Reference state**

$h = 200$  kJ/kg and  $s = 1$  kJ/(kg K) at  $t = 0$  °C on the boiling curve ( $x = 0$ )

**Details on the vapor fraction  $x$  and on the calculation of wet steam**

The wet steam region is calculated automatically by the subprograms. For this purpose the following fixed details on the vapor fraction  $x$  are to be considered:

If the state point to be calculated is located in the single-phase region (liquid or superheated steam)  $x = -1$  must be entered as a pro-forma value.

If the state point to be calculated is located in the wet steam region, a value for  $x$  between 0 and 1 ( $x = 0$  for saturated liquid,  $x = 1$  for saturated steam) must be entered.

When calculating wet steam either the given value for  $t$  and  $p = -1000$  or the given value for  $p$  and  $t = -1000$  and in both cases the value for  $x$  between 0 and 1 must be entered.

If  $p$  and  $t$  and  $x$  are entered as given values, the program considers  $p$  and  $t$  to be appropriate to represent the vapor pressure curve.

If it is not true, the calculated result will be  $-1000$ .

Wet steam region: Temperature range from  $t_t = -138.255$  °C to  $t_c = 151.975$  °C

Pressure range from  $p_t = 6.53 \times 10^{-6}$  bar to 37.96 bar

**Hint!**

*If the input values are located outside the range of validity, the result for the calculated function will always be  $-1000$ . Please find more exact details on every function and its corresponding range of validity in the enclosed program documentation in chapter 3.*