KCE
ThermoFluidProperties

Property Library for Standard Dry Air

FluidVIEW
with LibRealAir
for LabVIEW™

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Property Library of Ammonia-Water Mixtures
Including DLL and Add-on for LabVIEW™
FluidVIEW
LibRealAir

Contents

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0 Package Contents

0.1 Zip files for 32-bit LabVIEW™

In order to install FluidVIEW on a computer running a 32-bit version of LabVIEW™ the zip file **CD_FluidVIEW_LibRealAir.zip** is delivered. The directory structure of the archive is corresponding to the default directory of LabVIEW™.

The effects of the fifteen files, which are stored in the different directories of the zip archive, are shown in the Tables 0.1, 0.2, 0.3 and 0.4.

Table 0.1 Effects of the files located in the archive directory **CD_FluidVIEW_LibRealAir\vi.lib \FluidVIEW\LibRealAir**

Filename	Effects
LibRealAir.llb	LabVIEW™ library file, containing every function of the LibRealAir property library in the form of subprograms (SubVIs)

Table 0.2 Effects of the files located in the archive directory **CD_FluidVIEW_LibRealAir\menus \Categories\FluidVIEW**

Filename	Effects
dir.mnu	The palette view of LabVIEW™ is based on the palette files (*.mnu). They include the palette data (e. g. the display name, the palette icon, the palette description, the help information, the synchronize information and the items)

Table 0.3 Effects of the files located in the archive directory **CD_FluidVIEW_LibRealAir\source**

Filename	Effects
LibRealAir.dll	Dynamic-link library containing the algorithms for the calculation of the property functions of carbon dioxide
advapi32.dll	Runtime library
Dformd.dll	Runtime library for the Fortran DLL
Dforrt.dll	Runtime library for the Fortran DLL
LC.dll	Auxiliary library
msvcp60.dll	Runtime library
msvcrt.dll	Runtime library

Table 0.4 Effects of the files located in the archive directory **CD_FluidVIEW_LibRealAir\help \FluidVIEW-help**

Filename	Effects
FluidVIEW_LibRealAir.pdf	User's guide of the property library LibRealAir for the LabVIEW™ Add-On FluidVIEW
LibRealAir.chm	Help file with descriptions for each function
OpenLibRealAir_doc.vi	LabVIEW™ instrument to open the user's guide via the help menu
LibRealAir.txt	Text file to change the name of the menu item of the help file
OpenLibRealAir_doc.txt	Text file to change the name of the menu item of the file OpenLibRealAir_doc.vi

0.2 Zip files for 64-bit LabVIEW™

In order to install FluidVIEW on a computer running a 64-bit version of LabVIEW™ the zip file **CD_FluidVIEW_LibRealAir_x64.zip** is delivered. The directory structure of the archive is corresponding to the default directory of LabVIEW™.

The effects of the fifteen files, which are stored in the different directories of the zip archive, are shown in the Tables 0.5, 0.6, 0.7, 0.8 and 0.9.

Table 0.5 Effects of the files located in the archive directory **CD_FluidVIEW_LibRealAir_x64\vi.lib \FluidVIEW\LibRealAir**

Filename	Effects
LibRealAir.llb	LabVIEW™ library file, containing every function of the LibRealAir property library in the form of subprograms (SubVIs)

Table 0.6 Effects of the files located in the archive directory **CD_FluidVIEW_LibRealAir_x64\menus \Categories\FluidVIEW**

Filename	Effects
dir.mnu	The palette view of LabVIEW™ is based on the palette files (*.mnu). They include the palette data (e. g. the display name, the palette icon, the palette description, the help information, the synchronize information and the items)

Table 0.7 Effects of the files located in the archive directory **CD_FluidVIEW_LibRealAir_x64\source**

Filename	Effects
LibRealAir.dll	Dynamic-link library containing the algorithms for the calculation of the property functions of carbon dioxide
Capt_ico_big.ico	Icon file
Libmmd.dll	Runtime library
Libifcoremd.dll	Runtime library
LC.dll	Auxiliary library
Libiomp5md.dll	Runtime library

Table 0.8 Effects of the files located in the archive directory **CD_FluidVIEW_LibRealAir_x64\help \FluidVIEW-help**

Filename	Effects
FluidVIEW_LibRealAir.pdf	User's guide of the LibRealAir property library for the LabVIEW™ Add-On FluidVIEW
LibRealAir.chm	Help file with descriptions for each function
OpenLibRealAir_doc.vi	LabVIEW™ instrument to open the user's guide via the help menu
LibRealAir.txt	Text file to change the name of the menu item of the help file
OpenLibRealAir_doc.txt	Text file to change the name of the menu item of the file OpenLibRealAir_doc.vi

Table 0.9 Effects of the files located in the archive directory **CD_FluidVIEW_LibRealAir_x64 \vcredist_x64**

Filename	Effects
vcredist_x64.exe	Executable file to install the Microsoft Visual C++ 2008 Redistributable Package (x64). Within runtime components of Visual C++ Libraries required to run 64-bit applications developed with Visual C++ on a computer that does not have Visual C++ 2010 installed.

1 Property Functions

1.1 Range of Validity

The LibRealAir property library uses the thermodynamic property formulation for standard dry air released by *LEMMON* et al. [1], [2]. Whereas the atmospheric air is a mixture of fluids including nitrogen, oxygen, argon, carbon dioxide, steam, and other trace elements. The standard air this formulation is based on is dry and contains no carbon dioxide or trace elements. Due to the fact that the caused change is less than the experimental error in the measurements, this assumption has been made [1]. The composition is given in Table 1.1.

Table 1.1: Composition of air with N2, O2 and Ar as constituents

Component name	Chemical symbol	Mole fraction
Nitrogen	N_2	0.7812
Oxygen	O_2	0.2096
Argon	Ar	0.0092

The LibRealAir property library is valid for liquid, steam and supercritical air. This includes temperatures from 59.75 K (-213.4 °C) at the solidification point on the saturated liquid line to 2000 K (1726.85 °C) and pressures from 0.00001 bar to 20000 bar. The range of validity of the LibRealAir property library is shown in Figure 1.1 and Figure 1.3. Values for the points marked on these Figures are listed in Table 1.2 and Table 1.3.

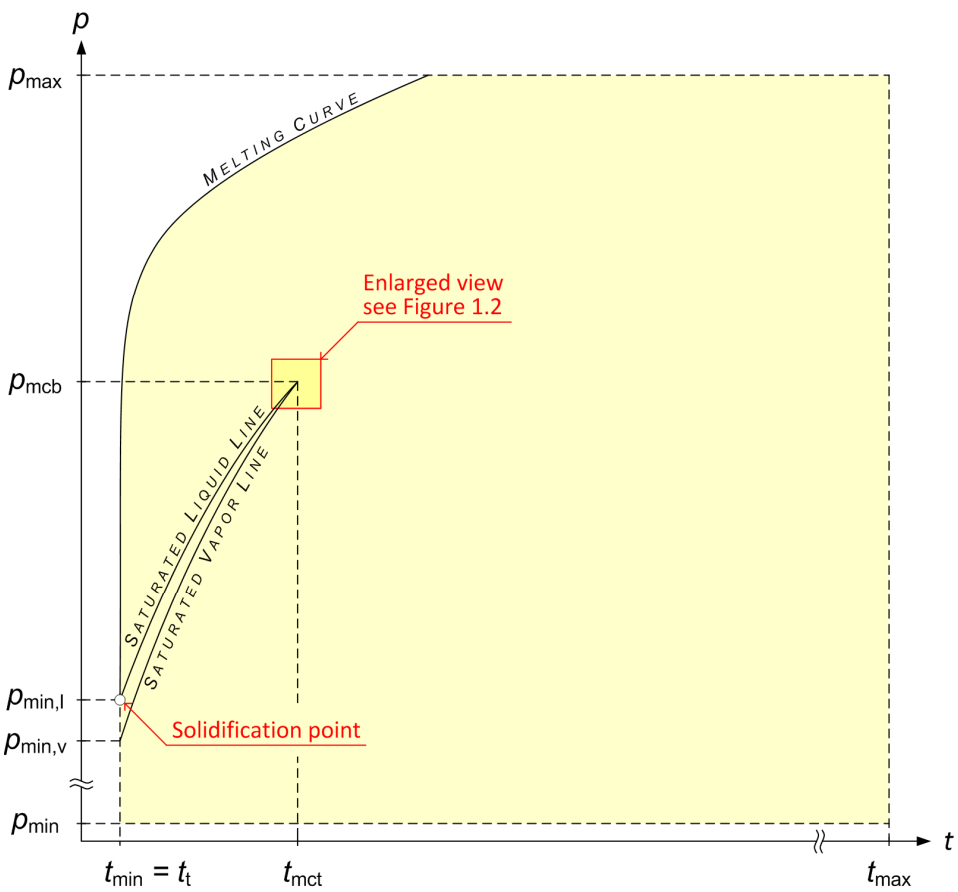

Figure 1.1: Entire range of validity in an lg *p*, lg *t* – diagram
(see Figure 1.2 for an enlarged view of the critical region phase boundaries)

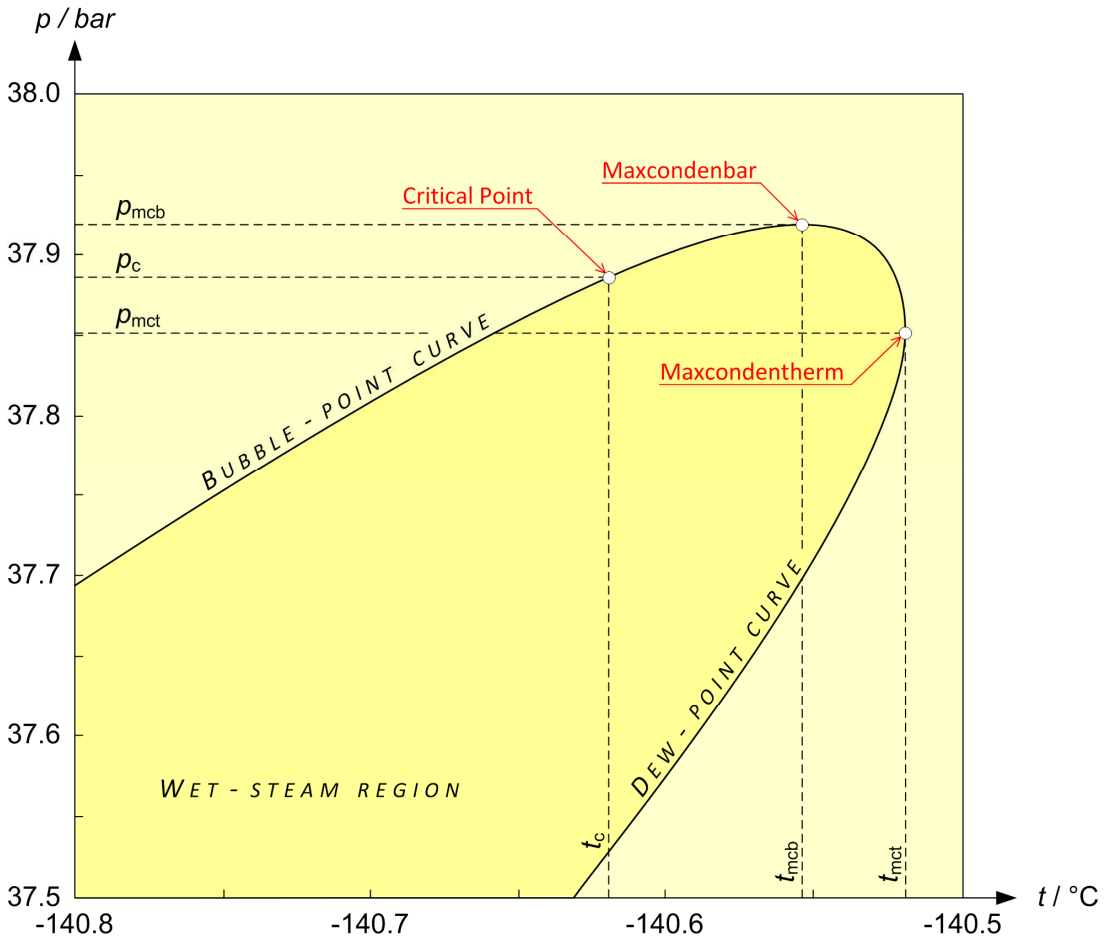

Figure 1.2: Enlarged view of the critical region phase boundaries in an *p*,*t*-diagram

Owing to the different boiling point temperatures of the mixture components in the *p*,*T*-diagram the saturation lines (liquid and vapor) of air do not overlap. In addition to the critical point a state point of maximum temperature (maxcondentherm) and a state point of maximum pressure (maxcondenbar) were determined on the saturation line. The maxcondentherm, maxcondenbar and critical point properties of air are shown in Table 1.3.

Table 1.2: Range of validity

Pressure	**Abbreviations**	**Values in bar**
Minimum pressure	p_{min}	$1 \cdot 10^{-5}$
Minimum pressure on the dew-point curve	$p_{min,l}$	0.024316
Minimum pressure on the bubble-point curve	$p_{min,v}$	0.052646
Maximum pressure	p_{max}	20000
Temperature	**Abbreviations**	**Values in °C**
Minimum temperature eq. triple point temperature	$t_{min} = t_t$	-213.4
Maximum temperature	t_{max}	1726.85
Specific Volume	**Abbreviations**	**Values in m³/kg**
Minimum specific volume	v_{min}	0.00071991
Minimum specific volume on the bubble point curve	$v_{min,l}$	0.00104112
Maximum specific volume on the dew-point curve	$v_{max,v}$	7.037519
Maximum specific volume	v_{max}	574234.252

Table 1.3: Maxcondentherm, maxcondenbar and critical point of air (calculated with the formulation by *LEMMON* et al.)

Condition	Pressure in bar	Temperature in °C	Spec. volume in m³/kg
Maxcondentherm (mct)	37.8502	-140.5188	0.003323
Maxcondenbar (mcb)	37.9195	-140.5539	0.003018
Critical point (c)	37.8869	-140.6194	0.002853

Figure 1.3 shows the entire range of validity for the equation in an *p,v*-diagram. An enlarged view of the critical region phase boundaries in an *p,v*-diagram is shown in Figure 1.4.

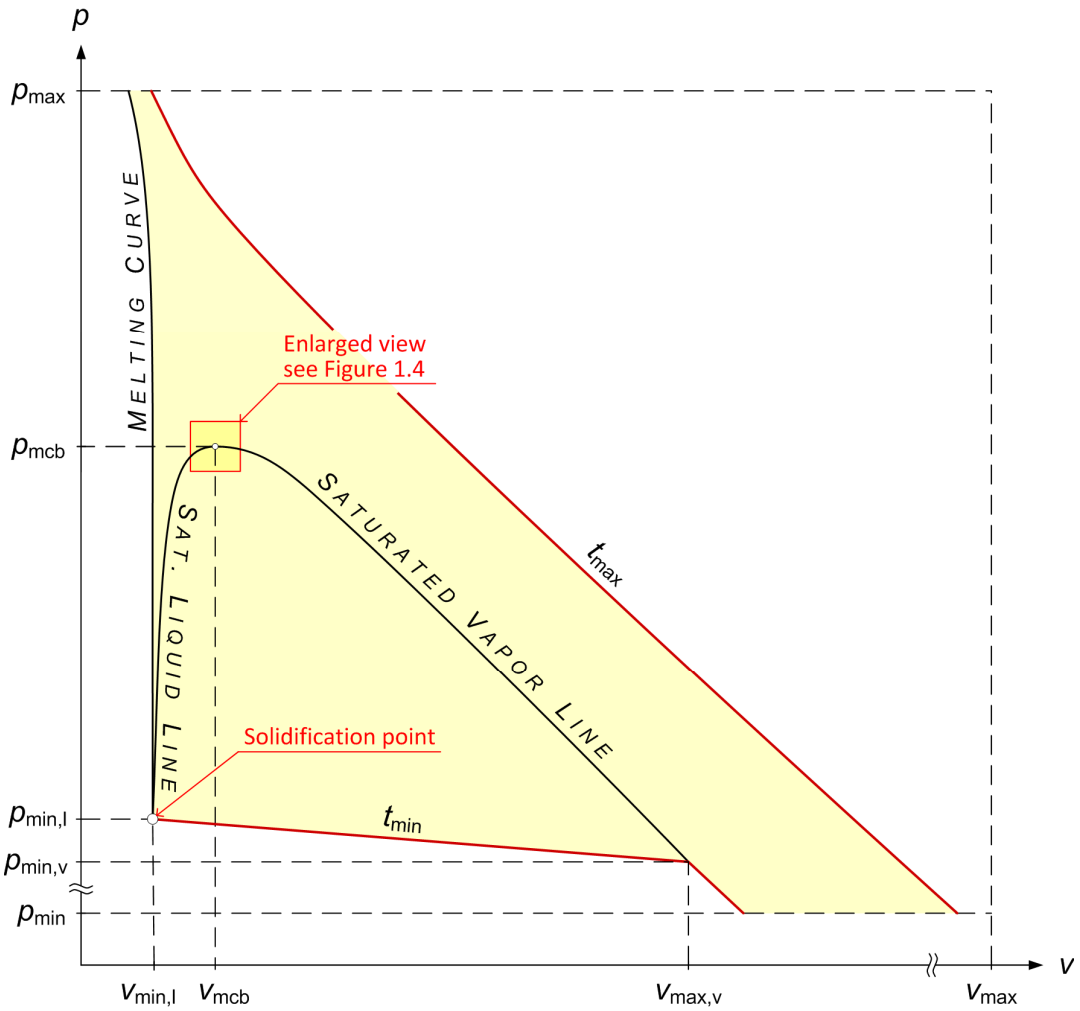

Figure 1.3: Entire range of validity in an lg *p*, lg *v* - diagram

All sub-programs and functions can be applied in the entire range of validity of the LibRealAir. The call of the equation of state for each calculation region will be carried out within the program. The sub-programs of the LibRealAir DLL and the functions of the Add-In are listed in the following section.

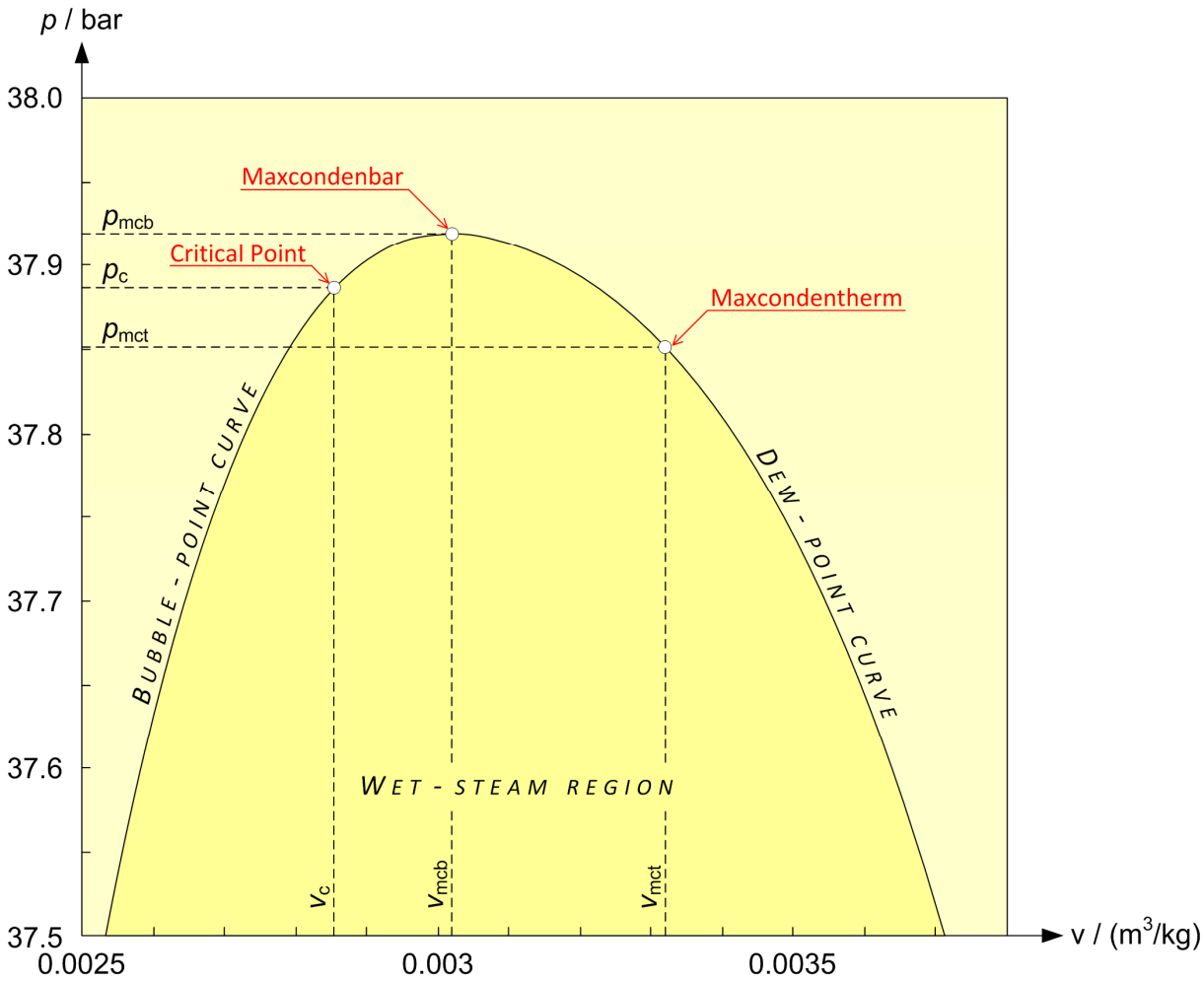

Figure 1.4: Enlarged view of the critical region phase boundaries in an *p*,*v*-diagram

1.2 Functions

Functional dependence	Function Name	Call from DLL LibRealAir, Result as Parameter	Property or Function	Unit of the Result
$a = f(p,t,x)$	a_ptx_air	= APTXAIR(P,T,X)	Thermal diffusivity	m^2/s
$\alpha_p = f(p,t,x)$	alphap_ptx_air	= ALPHAPPTXAIR(P,T,X)	Relative pressure coefficient	1/K
$\alpha_v = f(p,t,x)$	alphav_ptx_air	= ALPHAVPTXAIR(P,T,X)	Isobaric cubic expansion coefficient	1/K
$\beta_p = f(p,t,x)$	betap_ptx_air	= BETAPPTXAIR(P,T,X)	Isothermal stress coefficient	kg/m^3
$c_p = f(p,t,x)$	cp_ptx_air	= CPPTXAIR(P,T,X)	Specific isobaric heat capacity	kJ/(kg·K)
$c_v = f(p,t,x)$	cv_ptx_air	= CVPTXAIR(P,T,X)	Specific isochoric heat capacity	kJ/(kg·K)
$\eta = f(p,t,x)$	eta_ptx_air	= ETAPTXAIR(P,T,X)	Dynamic viscosity	Pa·s
$h = f(p,t,x)$	h_ptx_air	= HPTXAIR(P,T,X)	Specific enthalpy	kJ/kg
$\kappa = f(p,t,x)$	kappa_ptx_air	= KAPPAPTXAIR(P,T,X)	Isentropic exponent	-
$\kappa_T = f(p,t,x)$	kappat_ptx_air	= KAPPATPTXAIR(P,T,X)	Isothermal compressibility	1/kPa
$\lambda = f(p,t,x)$	lambda_ptx_air	= LAMBDAPTXAIR(P,T,X)	Thermal conductivity	W/(m·K)
$\nu = f(p,t,x)$	nu_ptx_air	= NUPTXAIR(P,T,X)	Kinematic viscosity	m^2/s
$p_{mel} = f(t)$	pmel_t_air	= PMELTAIR(T)	Pressure on the melting curve	bar
$Pr = f(p,t,x)$	prandtl_ptx_air	= PRANDTLPTXAIR(P,T,X)	Prandtl number	-
$p_{sl} = f(t)$	psl_t_air	= PSLTAIR(T)	Pressure on the saturated liquid line	bar
$p_{sv} = f(t)$	psv_t_air	= PSVTAIR(T)	Pressure on the saturated vapor line	bar
$\rho = f(p,t,x)$	rho_ptx_air	= RHOPTXAIR(P,T,X)	Density	kg/m^3
$s = f(p,t,x)$	s_ptx_air	= SPTXAIR(P,T,X)	Specific entropy	kJ/(kg·K)
$t_{mel} = f(p)$	tmel_p_air	= TMELPAIR(P)	Temperature on the melting curve	°C
$t = f(p,h)$	t_ph_air	= TPHAIR(P,H)	Backward function: Temperature from pressure and enthalpy	°C
$t = f(p,s)$	t_ps_air	= TPSAIR(P,S)	Backward function: Temperature from pressure and entropy	°C
$t_{sl} = f(p)$	tsl_p_air	= TSLPAIR(P)	Temperature on the saturated liquid line	°C
$t_{sv} = f(p)$	tsv_p_air	= TSVPAIR(P)	Temperature on the saturated vapor line	°C
$u = f(p,t,x)$	u_ptx_air	= UPTXAIR(P,T,X)	Specific internal energy	kJ/kg
$v = f(p,t,x)$	v_ptx_air	= VPTXAIR(P,T,X)	Specific volume	m^3/kg
$w = f(p,t,x)$	w_ptx_air	= WPTXAIR(P,T,X)	Speed of sound	m/s
$x = f(p,h)$	x_ph_air	= XPHAIR(P,H)	Backward function: Vapor fraction from pressure and enthalpy	kg/kg
$x = f(p,s)$	x_ps_air	= XPSAIR(P,S)	Backward function: Vapor fraction from pressure and entropy	kg/kg

Units:

Temperature	t in °C
Pressure	p in bar
Vapor fraction	x in kg saturated steam/kg wet steam

Range of validity of LibRealAir:

Temperature:	from -213.4 C (59.75 K) to 1726.85 °C (2000 K)
Pressure:	from 0.00001 bar to 20000 bar

Details on the vapor fraction *x* and on the calculation of wet steam:

The wet steam region is calculated automatically by the subprograms. For this purpose the following fixed details on the vapor fraction x are to be considered:

Single phase region

If the state point to be calculated is located in the single-phase region (liquid or superheated steam) $x = -1$ must be entered as a pro-forma value.

Wet steam region

When calculating wet steam, a value between 0 and 1 ($x = 0$ for saturated liquid, $x = 1$ for saturated steam) must be entered. It is adequate to enter either the given value for t and $p = -1000$, or the given value for p and $t = -1000$, plus the value for x between 0 and 1. When p and t and x are entered as given values, the program will consider whether p and t fit together. If it is not the case the calculation for the property of the chosen function to be calculated results in –1000. In this case, the backward functions result in the appropriate value between 0 and 1 for x.

Boundaries for wet steam region

The boundaries for the wet steam region are

t_t = -213.4 °C; $p_{min,l}$ = 0.052646 bar; $p_{min,v}$ =0.024316 bar

t_{mct} =-140.5188 °C; p_{mcb} = 37.9195 bar.

They are illustrated in Figure 1.1 and Figure 1.2 and listed in Table 1.2 and Table 1.3.

Note:

If the calculation results in –1000, the values entered represent a state point beyond the range of validity. For further information on each function and its range of validity see Chapter 3. The same information may also be accessed via the online help pages.

1.3 Thermodynamic Diagrams

The next pages provide the following thermodynamic diagrams showing the properties of standard dry air.

- **lg *p*,*h*-diagram** from
  p = 0.01 bar to p = 5000 bar,
  t = -213.4 °C to t = 0 °C and
  Δh = 450 kJ/kg
- ***T*,*s*-diagram** from
  t = -213.4 °C to t = 60 °C,
  p = 0.01 bar to p = 1000 bar and
  Δs = 4.8 kJ/(kg·K)
- ***T*,*s*-diagram** from
  t = -50 °C to t = 1000 °C,
  p = 0.01 bar to p = 1000 bar and
  Δs = 3.6 kJ/(kg·K)
- ***h*,*s*-diagram** from
  t = -40 °C to t = 1000 °C,
  p = 0.01 bar to p = 1000 bar and
  Δs = 3.6 kJ/(kg·K)

2 Application of FluidVIEW in LabVIEW™

The FluidVIEW Add-on has been developed to calculate thermodynamic properties in LabVIEW™ more conveniently. Within LabVIEW™, it enables the direct call of functions relating to standard dry air from the LibRealAir property library.

2.1 Installing FluidVIEW

If a FluidVIEW property library has not yet been installed, please complete the initial installation procedure described below.

If a FluidVIEW property library has already been installed, you only need to copy several files which belong to the LibRealAir library. In this case, follow the subsection "Adding the LibRealAir Library" on page 2/3.

In both cases folders and files from the zip archive

CD_FluidVIEW_LibRealAir.zip (for 32-bit version of Windows®)

CD_FluidVIEW_LibRealAir_x64.zip (for 64-bit version of Windows®)

have to be copied into the default directory of the LabVIEW™ development environment. In the following text these zipped directories for the 32-bit or 64-bit operating system will be symbolised with the term **<CD>**.

You can see the current default directory of LabVIEW™ in the paths page (options dialog box). To display this page please select *Tools* and click on *Options* to open the options dialog box and then select *Paths* from the category list.

By choosing *Default Directory* from the drop-down list the absolute pathname to the default directory, where LabVIEW™ automatically stores information, is displayed. In the following sections the pathname of the default directory will be symbolised by the term **<LV>**.

Additional Requirement When Using the 64-bit Operating System

If you want to use FluidVIEW on a 64-bit computer that does not have Visual C++ installed, please make sure the Microsoft Visual C++ 2010 x64 Redistributable Package is installed.

If it is not the case, please install it by double clicking the file

vcredist_x64.exe

which you find in the folder **\vcredist_x64** in the **64-bit** CD folder "CD_FluidVIEW_LibRealAir_x64."

In the following window you are required to accept the Microsoft® license terms to install the Microsoft Visual C++ 2010 runtime libraries by ticking the box next to "I have read and accept the license terms" (see Figure 2.1).

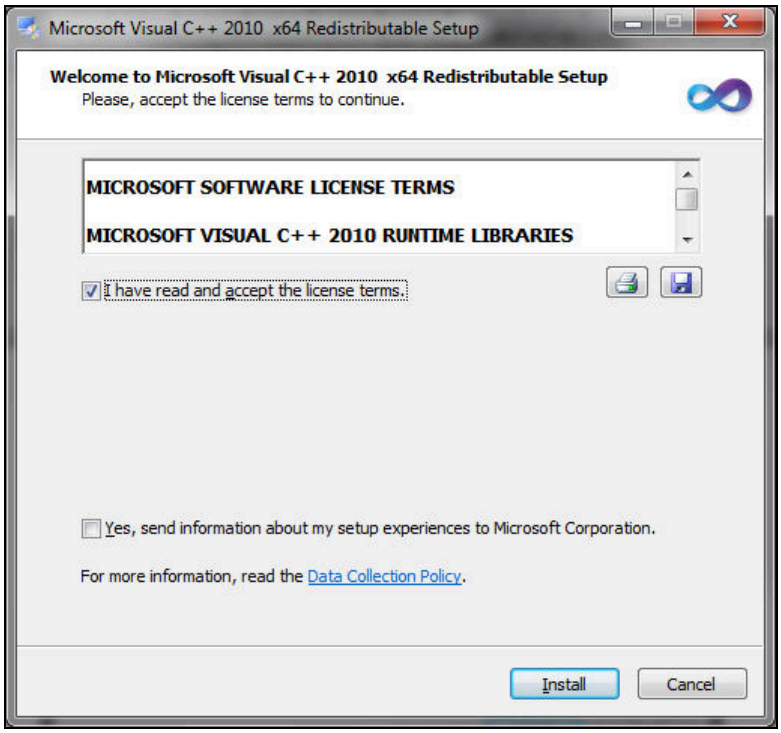

Figure 2.1 Accepting the license terms to install the Microsoft Visual C++ 2010 x64 Redistributable Package

Now click on "Install" to continue installation.

After the "Microsoft Visual C++ 2010 x64 Redistributable Pack" has been installed, you will see the sentence "Microsoft Visual C++ 2010 x64 Redistributable has been installed." Confirm this by clicking "Finish."

Now you can use the FluidVIEW Add-On on your 64-bit operating system. Please follow the instructions below to install FluidVIEW.

Initial Installation of FluidVIEW

The initial installation of FluidVIEW is carried out by copying three directories with its contents from the zip archive to the standard directory of LabVIEW™.

The directories that have to be copied, their paths in the zip archive and their target paths are listed in Table 2.1.

The installation is complete after copying the files and restarting LabVIEW™.

Due to the fact, that the functions of the DLL are called with a variable pathname, the source files you will find in the directory **<CD>\source** can be stored in a random directory. The pathname has to be indicated in order to calculate the property functions.

All source files have to be stored in the same directory to make the property functions of the LibRealAir library work. These files are for the

- **32-bit system**: LibRealAir.dll, advapi32.dll, Dformd.dll, Dforrt.dll, LC.dll, msvcp60.dll, and msvcrt.dll

and for the

- **64-bit system**: LibRealAir.dll, capt_ico_big.ico, LC.dll, libifcoremd.dll, libiomp5md.dll, and libmmd.dll.

Table 2.1 Directories which have to be copied from the zip archive in the default directory of LabVIEW™ (<LV>) for the initial installation of FluidVIEW

Name of the directory	Pathname in the zip archive	Target path in the default directory of LabVIEW (<LV>)
FluidVIEW	<CD>\vi.lib	<LV>\vi.lib
FluidVIEW	<CD>\menus\Categories	<LV>\menus\Categories
FluidVIEW-Help	<CD>\help	<LV>\help

Adding the LibRealAir Library

In order to add the LibRealAir property library to an existing FluidVIEW installation, one folder with its contents and five files have to be copied from the zip archive to the standard directory of LabVIEW™. This directory, the files plus their pathnames in the zip archive and their target paths are listed in Table 2.2.

The installation is complete after copying the files and restarting LabVIEW™.
Due to the fact, that the functions of the DLL are called with a variable pathname, the source files you will find in the directory **<CD>\source** can be stored in a random directory. The pathname has to be indicated in order to calculate the property functions.

All source files have to be stored in the same directory to make the property functions of the LibRealAir library work. These files are for the

- **32-bit system**: LibRealAir.dll, advapi32.dll, Dformd.dll, Dforrt.dll, LC.dll, msvcp60.dll, and msvcrt.dll

and for the

- **64-bit system**: LibRealAir.dll, capt_ico_big.ico, LC.dll, libifcoremd.dll, libiomp5md.dll, and libmmd.dll

Table 2.2 Data which have to be copied from the zip archive in the default directory of LabVIEW™ (<LV>) for adding the LibRealAir property library to an existing installation of FluidVIEW

File name with file extension or name of the directory	Pathname in the zip archive	Target path in the default directory of LabVIEW (<LV>)
LibRealAir.llb	<CD>\vi.lib\FluidVIEW	<LV>\vi.lib\FluidVIEW
LibRealAir	<CD>\menus\Categories \FluidVIEW	<LV>\menus\Categories \FluidVIEW
LibRealAir.hlp	<CD>\\help\FluidVIEW-Help	<LV>\help\FluidVIEW-Help
LibRealAir.txt	<CD>\\help\FluidVIEW-Help	<LV>\help\FluidVIEW-Help
FluidVIEW_LibRealAir.pdf	<CD>\\help\FluidVIEW-Help	<LV>\help\FluidVIEW-Help
Open_LibRealAir_doc.vi	<CD>\\help\FluidVIEW-Help	<LV>\help\FluidVIEW-Help
Open_LibRealAir_doc.txt	<CD>\\help\FluidVIEW-Help	<LV>\help\FluidVIEW-Help

After you have restarted LabVIEW™ you will find the functions of the LibRealAir property library in the functions palette under the sub palette FluidVIEW. An example calculation of the specific enthalpy *h* and the specific entropy *s* is shown in section 2.4.

2.2 The FluidVIEW Help System

FluidVIEW provides detailed online help functions.

General Information

The FluidVIEW Help System consists of the Microsoft WinHelp file **LibRealAir.chm** and this user's guide as PDF document **FluidVIEW_LibRealAir_Docu_Eng.pdf**. Both files can be opened via the help menu. To do this please click *Help* in the menu bar. In the submenu *FluidVIEW-Help* you will find the commands *LibRealAir Help File* and *LibRealAir User's Guide* to open an appropriate file.

Context-Sensitive Help

If you have activated the context help function in LabVIEW™ (Ctrl-H) and move the cursor over a FluidVIEW object basic information is displayed in the context help window. The in- and output parameters plus a short information text are displayed for a property function. By clicking the **Detailed help** button in the **Context help** window the online help will be opened. The context help window of the function v_ptx_air.vi is shown in Figure 2.2.

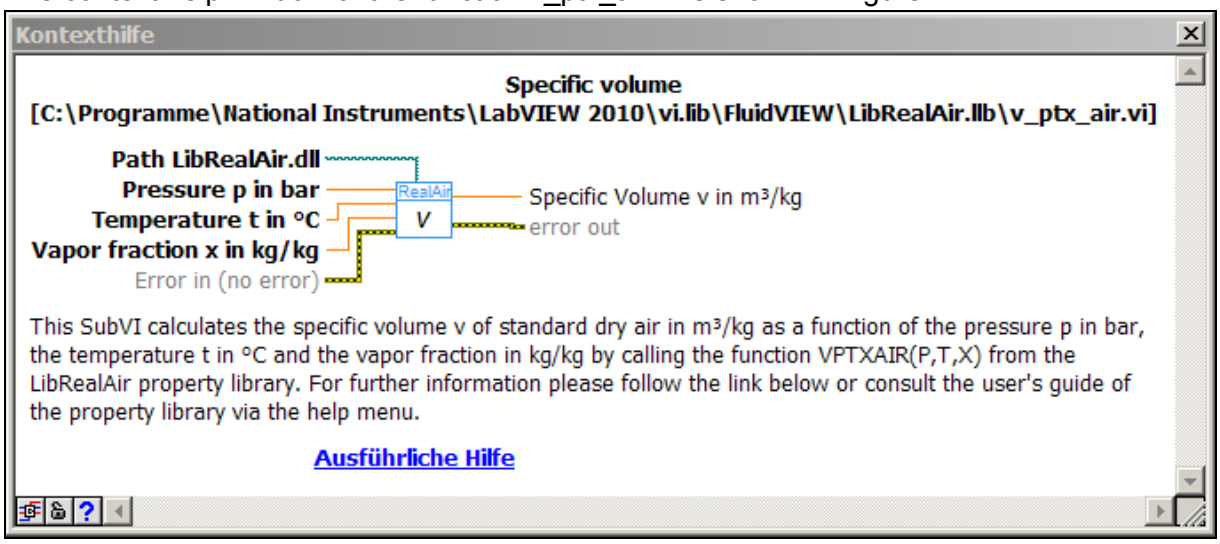

Figure 2.2 Context help window of the function v_ptx_air.vi

2.3 Licensing the LibRealAir Property Library

The licensing procedure has to be carried out when calculating a LibRealAir function and a FluidVIEW prompt message appears. In this case, you will see the "License Information" window (see figure below).

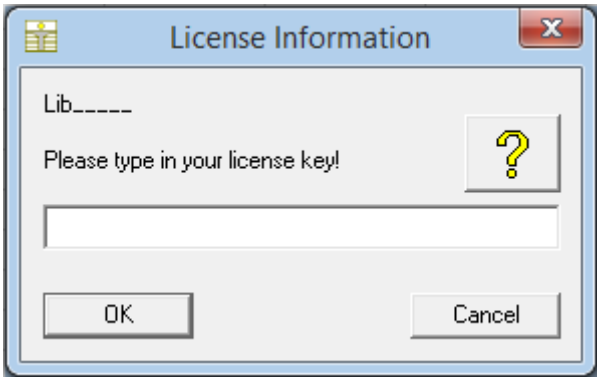

Figure 2.3 "License Information" window

Here you will have to type in the license key. You can find contact information on the "Content" page of this User's Guide or by clicking the yellow question mark in the "License Information" window. Then the following window will appear:

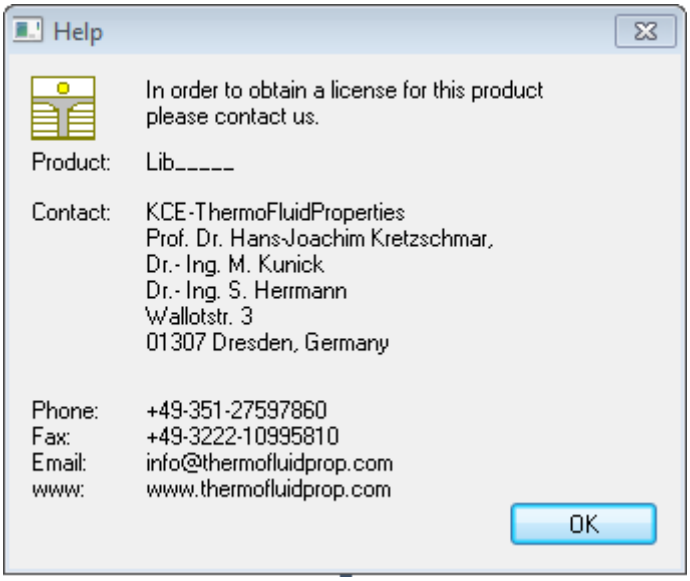

Figure 2.4 "Help" window

If you do not enter a valid license it is still possible to start Excel by clicking "Cancel". In this case, the LibRealAir property library will display the result "-1.11111E+7" for every calculation.
The "License Information" window will appear every time you start LabVIEW unless you uninstall FluidVIEW.
Should you not wish to license the LibRealAir property library, you have to uninstall FluidVIEW according to the description in section 2.5 of this User's Guide.

Note:

The product name "Lib_ _ _ _ _ in the Figures above stands for the Library you are installing.

2.4 Example: Calculation of *h* = f(*p*,*t*,*x*) and *s* = f(*p*,*t*,*x*)

After the delivered files have been copied in the appropriate folders of the default directory LabVIEW™ (described in section 2.1), the LibRealAir property library is ready to use. The function nodes of the LibRealAir property library can be used by dragging them from the functions palette into the block diagram and connecting them with the wires representing the required input parameters.

Now we will calculate, step by step, the specific enthalpy *h* as a function of pressure *p*, temperature *t*, and vapor fraction *x*, using FluidVIEW.

- Start LabVIEW™ and wait for the *Getting Started* window to be displayed. Then select *Blank VI*. The *Blank VI* will be displayed in two windows, the front panel and the block diagram.
- Open the functions palette in the block diagram **via view / Functions Palette** (or by clicking the right mouse button anywhere in the free area of the block diagram) if not yet displayed.
- In addition to the default LabVIEW™ palettes the functions palette contains the sub palette *FluidVIEW* (see Figure 2.5) with the sub palette *LibRealAir* (see Figure 2.6).

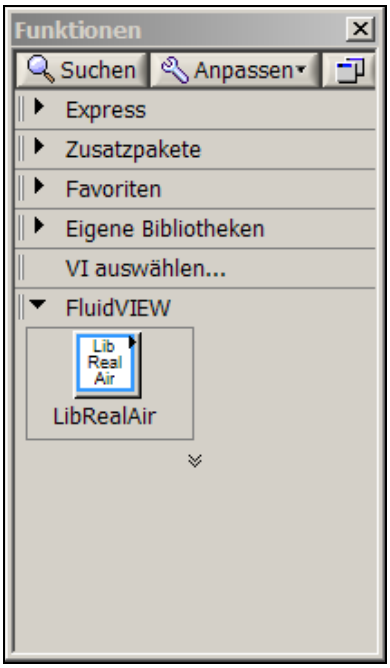

Figure 2.5
Functions palette with the sub palettes FluidVIEW and LibRealAir

Figure 2.6
Functions palette with the property functions of the LibRealAir library

In order to calculate the specific enthalpy *h*, drag the function (SubVI) whose symbol shows the *h* from the functions palette into the block diagram.
While the short names of the SubVIs behind the symbols will be shown in the control tip, the full names and brief descriptions of the property functions are displayed in the *Context Help* window (see Figure 2.2). To use the context help press <Ctrl>+<H> on your keyboard.

- After placing the node of the SubVI **h_ptx_air.vi** on your block diagram the required input parameters have to be defined.
  The input parameters which are set as required appear in bold type in the Context Help window. In this case these input parameters are **Path LibRealAir.dll** (LabVIEW™ data

type: Path), **Pressure p in bar** (LabVIEW™ data type: Double precision, floating-point), **Temperature t in °C** (LabVIEW™ data type: Double precision, floating-point) and **Vapor fraction x in kg/kg** (LabVIEW™ data type: Double precision, floating-point).

- To define these variables wire their input terminals with input elements on the front panel. You can accomplish this in one step by choosing **Create / Control** in the context menu of all required input terminals. In order to wire the output terminal of the function node with an output element on the front panel, choose **Create / Indicator** in the context menu of the output terminal **Specific enthalpy h in kJ/kg** (LabVIEW™ data type: Double precision, floating-point). After cleaning up the block diagram by pressing <Ctrl>+<U> it has the appearance illustrated in Figure 2.7. The same input and output elements are available on the appropriate front panel (see Figure 2.8).

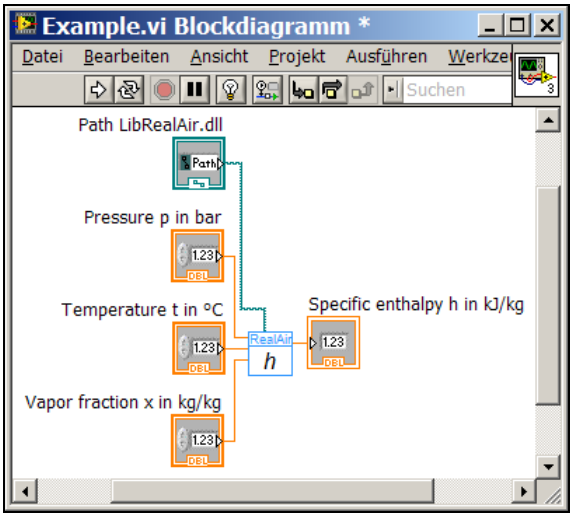

Figure 2.7
Block diagram of the example calculation

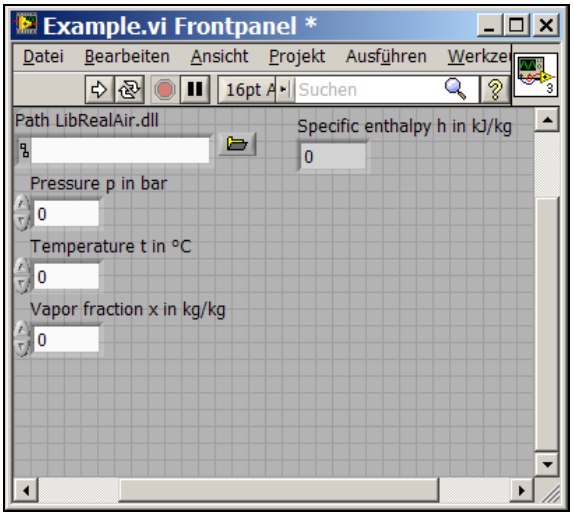

Figure 2.8
Front panel of the example calculation

- Enter a value in the input element *Pressure p in bar* on the front panel
  (Range of validity corresponding to *LEMMON*: p = 0.00001 … 20000 bar)

  ⇒ e. g.: Enter the value 10.

- Enter a value in the input element *Temperature t in °C* on the front panel
  (Range of validity corresponding to *LEMMON*: t = -213.4 … 1726.85 bar)

  ⇒ e. g.: Enter the value 20.

- Enter a value in the input element *Vapor fraction x in kg/kg* on the front panel.
  Since the wet steam region is calculated automatically by the subprograms, the following fixed details on the vapor fraction x are to be considered when the value for x is entered:

  <u>Single-phase region</u>
  If the state point to be calculated is located in the single-phase region (liquid or superheated steam) x = –1 must be entered as a pro-forma value.

  <u>Wet-steam region</u>
  When calculating wet steam, a value between 0 and 1 (x = 0 for saturated liquid, x = 1 for saturated steam) must be entered. In this case, the backward functions result in the appropriate value between 0 and 1 for x. It is adequate to enter either the given value for t <u>and</u> p = –1, or the given value for p <u>and</u> t = –1, plus the value for x between 0 and 1. When p <u>and</u> t <u>and</u> x are entered as given values, the program will consider p and t to be appropriate to represent the saturation-pressure curve. If it is not the case the calculation

for the property of the chosen function to be calculated results in –1000.
⇒ e. g.: Enter the value -1.

- Enter the path of the LibRealAir.dll in the input element *Path LibRealAir.dll* on the front panel (as explained in section 2.1 the LibRealAir.dll and the other library files from the directory **<CD>\source** have to be stored in the same directory which is arbitrary). To do this you can use the *File Open Dialog* which appears by clicking the yellow folder symbol on the right of the input element.
- To run the calculation of the specific enthalpy click on the *Run* button or press <Ctrl>+<R>. The result for *h* in kJ/kg appears in the output element (see Figure 2.9).

  ⇒ The result for *h* in our sample calculation is 18.004689125 in kJ/kg.

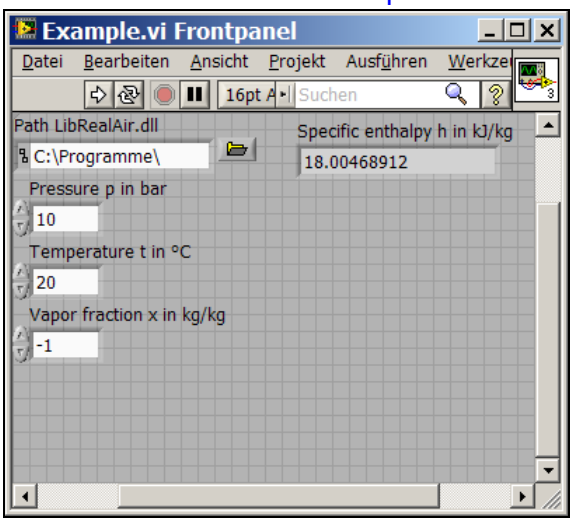

Figure 2.9 Result of the example calculation of *h*

The calculation of *h* = f(*p*,*t*,*x*) has thus been completed. Correspondingly, the specific entropy *s* = f(*p*,*t*,*x*) can be calculated with the same values for *p*, *t*, and *x*. The following changes need to be implemented.

- Open the context menu of the function node *Specific enthalpy* on the block diagram. Under **Replace / Palette LibRealAir** you will find the function **Specific entropy** symbolized with *s*. The node on the block diagram changes to **Specific entropy** by clicking on this symbol. Since the input parameters are the same as before their labels need not be changed. Only the label of the output parameter can be changed from *Specific enthalpy h in kJ/kg* to *Specific entropy s in kJ/(kg·K)* by double clicking on it and typing the new name.
- On the front panel you can see that the new label for the output element *Specific entropy s in kJ/(kg·K)* was taken automatically. Since the values in the input elements are still present the calculation can be started now by pressing <Ctrl>+<R> or clicking the *Run* button. The result for *s* in kJ/(kg·K) appears in the output element.

  ⇒ The result for *s* in our sample calculation is -0.430733041 in kJ/(kg·K).

The calculation of *s* = f(*p*,*T*,*x*) has been carried out. You can now arbitrarily change the values for *p*, *t*, or *x* in the appropriate input elements.
Note:
If the calculation results in –1000, this indicates that the values entered are located outside the range of validity of *LEMMON*. More detailed information on each function and its range of validity is available in chapter 3. For further property functions calculable with FluidVIEW,

see the function table in chapter 1.

2.5 Removing FluidVIEW

Should you wish to remove the LibRealAir library or the complete FluidVIEW Add-on you merely have to delete the files that have been copied in the default directory of the LabVIEW™ development environment **<LV>**.

Removing the FluidVIEW Add-on

To remove the FluidVIEW Add-on please delete the folders listed in Table 2.3 from the default directory of LabVIEW™.

Table 2.3 Directories that have to be deleted from the default directory of LabVIEW™ to remove the FluidVIEW Add-on

Name of the directory	Path in the default directory of LabVIEW™ (<LV>)
FluidVIEW	<LV>\vi.lib
FluidVIEW	<LV>\menus\Categories
FluidVIEW-Help	<LV>\help

Removing only the LibRealAir library

To remove only the LibRealAir library please delete the folders or files listed in Table 2.4 from the default directory of LabVIEW™.

Table 2.4 Data that have to be deleted from the default directory of LabVIEW™ (<LV>) to remove only the LibRealAir library.

File name with file extension or name of the directory	Path in the default directory of LabVIEW (<LV>)
LibRealAir.llb	<LV>\vi.lib\FluidVIEW
LibRealAir	<LV>\menus\Categories\FluidVIEW
LibRealAir.hlp	<LV>\help\FluidVIEW-Help
LibRealAir.txt	<LV>\help\FluidVIEW-Help
FluidVIEW_LibRealAir.pdf	<LV>\help\FluidVIEW-Help
Open_LibRealAir_doc.vi	<LV>\help\FluidVIEW-Help
Open_LibRealAir_doc.txt	<LV>\help\FluidVIEW-Help

The changes will take effect after restarting LabVIEW™.

3. Program Documentation

Thermal Diffusivity *a* = f(*p*,*t*,*x*)

Function Name: **a_ptx_air**
Subroutine with function value: **REAL*8 FUNCTION APTXAIR(P,T,X)**
Variable Types: REAL*8 P,T,X

Input values

P - Pressure *p* in bar
T - Temperature *t* in °C
X - Vapor fraction *x* in (kg saturated steam)/(kg wet steam)

Result

a_ptx_air or APTXAIR - Thermal diffusivity $a = \frac{\lambda}{\rho \cdot c_p} = \frac{\lambda \cdot v}{c_p}$

Range of validity

Temperature range: from -213.4 °C (59.75 K) to 1726.85 °C (2000 K)
Pressure range: from 0.00001 bar to 20000 bar

Details on the vapor fraction *x*

The wet steam region is calculated automatically by the subprograms. For this purpose the following fixed details on the vapor fraction *x* are to be considered:

Single phase region
If the state point to be calculated is located in the single phase region (liquid or superheated steam) $x = -1$ must be entered as a pro-forma value.

Saturation lines
If the state point to be calculated is located on the saturated liquid line, the value 0 has to be entered for *x*. When calculating saturated steam (saturated vapor line) $x = 1$ has to be entered. The calculation for *x* values between 0 and 1 is not possible. It is adequate to enter either the given value for *t* and $p = -1000$, or the given value for *p* and $t = -1000$, plus the value for *x* (0 or 1). When *p* and *t* and *x* are entered as given values, the program will consider whether *p* and *t* fit together. If it is not the case the calculation of the function *a* will result in –1000.

Boundaries for wet steam region
The boundaries for the wet steam region are illustrated in Figure 1.1 and Figure 1.2.

Results for wrong input values

The result is **a_ptx_air = –1000** or **APTXAIR = –1000** for the following input values:

Single phase region: $p > p_{max} = 20000$ or $p < p_{min} = 0.00001$ bar or
($x = -1$) $t > t_{max} = 1726.85$ °C or $t < t_{min} = -213.4$ °C or $t < t_{mel}(p)$

Saturated liquid line: at $p = -1$ and $t > t_{mct} = -140.5188$ °C or $t < t_{min} = -213.4$ °C or
($x = 0$) at $t = -1$ and $p > p_{mcb} = 37.9195$ bar or $p < p_{min,l} = 0.052646$ bar or

	at $p < p_{mcb}$ = 37.9195 bar and $p > p_{min,l}$ = 0.052646 bar and $\lvert t - t_{sl}(p) \rvert > 0.1\,\mathrm{K}$
Saturated vapor line: (x = 1)	at $p = -1$ and $t > t_{mct}$ = -140.5188 °C or $t < t_{min}$ = -213.4 °C or at $t = -1$ and $p > p_{mcb}$ = 37.9195 bar or $p < p_{min,v}$ = 0.024316 bar or at $p < p_{mcb}$ = 37.9195 bar and $p > p_{min,v}$ = 0.024316 bar and $\lvert t - t_{sv}(p) \rvert > 0.1\,\mathrm{K}$

References

[1], [2]

Relative Pressure Coefficient α_p = f(p,t,x)

Function Name: **alphap_ptx_air**
Subroutine with function value: **REAL*8 FUNCTION ALPHAPPTXAIR(P,T,X)**
Variable Types: REAL*8 P,T,X

Input values

P - Pressure p in bar
T - Temperature t in °C
X - Vapor fraction x in (kg saturated steam)/(kg wet steam)

Result

alphap_ptx_air or **ALPHAPPTXAIR** – Relative pressure coefficient $\alpha_p = -\frac{1}{p}\left(\frac{\partial p}{\partial T}\right)_v$ in 1/K

Range of validity

Temperature range: from -213.4 °C (59.75 K) to 1726.85 °C (2000 K)
Pressure range: from 0.00001 bar to 20000 bar

Details on the vapor fraction *x*

The wet steam region is calculated automatically by the subprograms. For this purpose the following fixed details on the vapor fraction x are to be considered:

Single phase region
If the state point to be calculated is located in the single phase region (liquid or superheated steam) x = –1 must be entered as a pro-forma value.

Saturation lines
If the state point to be calculated is located on the saturated liquid line, the value 0 has to be entered for x. When calculating saturated steam (saturated vapor line) x = 1 has to be entered. The calculation for x values between 0 and 1 is not possible. It is adequate to enter either the given value for t and p = -1000, or the given value for p and t = –1000, plus the value for x (0 or 1). When p and t and x are entered as given values, the program will consider whether p and t fit together. If it is not the case the calculation of the function α_p will result in –1000.

Boundaries for wet steam region
The boundaries for the wet steam region are illustrated in Figure 1.1 and Figure 1.2.

Results for wrong input values

Result **alphap_ptx_air = –1000** or **ALPHAPPTXAIR = –1000** for the following input values:

Single phase region: $p > p_{max}$ = 20000 or $p < p_{min}$ = 0.00001 bar or
(x = –1) $t > t_{max}$ = 1726.85 °C or $t < t_{min}$ = -213.4 °C or $t < t_{mel}(p)$

Saturated liquid line: at p = –1 and $t > t_{mct}$ = -140.5188 °C or $t < t_{min}$ = -213.4 °C or
(x = 0) at t = –1 and $p > p_{mcb}$ = 37.9195 bar or $p < p_{min,l}$ = 0.052646 bar or
at $p < p_{mcb}$ = 37.9195 bar and $p > p_{min,l}$ = 0.052646 bar and
$|t - t_{sl}(p)| > 0.1$K

Saturated vapor line:	at $p = -1$ and $t > t_{mct}$ = -140.5188 °C or $t < t_{min}$ = -213.4 °C or
(x = 1)	at $t = -1$ and $p > p_{mcb}$ = 37.9195 bar or $p < p_{min,v}$ = 0.024316 bar or
	at $p < p_{mcb}$ = 37.9195 bar and $p > p_{min,v}$ = 0.024316 bar and
	$\lvert t - t_{sv}(p) \rvert > 0.1\,\mathrm{K}$

Reference

[1]

Isobaric Cubic Expansion Coefficient α_v = f(*p*,*t*,*x*)

Function Name: **alphav_ptx_air**
Subroutine with function value: **REAL*8 FUNCTION ALPHAVPTXAIR(P,T,X)**
Variable Types: REAL*8 P,T,X

Input values

P - Pressure *p* in bar
T - Temperature *t* in °C
X - Vapor fraction *x* in (kg saturated steam)/(kg wet steam)

Result

alphav_ptx_air or **ALPHAVPTXAIR**

Isobaric cubic expansion coefficient $\alpha_v = \frac{1}{\rho}\left(\frac{\partial \rho}{\partial p}\right)_T \left(\frac{\partial p}{\partial T}\right)_\rho$ in 1/K

Range of validity

Temperature range: from -213.4 °C (59.75 K) to 1726.85 °C (2000 K)
Pressure range: from 0.00001 bar to 20000 bar

Details on the vapor fraction *x*

The wet steam region is calculated automatically by the subprograms. For this purpose the following fixed details on the vapor fraction *x* are to be considered:

Single phase region
If the state point to be calculated is located in the single phase region (liquid or superheated steam) $x = -1$ must be entered as a pro-forma value.

Saturation lines
If the state point to be calculated is located on the saturated liquid line, the value 0 has to be entered for *x*. When calculating saturated steam (saturated vapor line) $x = 1$ has to be entered. The calculation for *x* values between 0 and 1 is not possible. It is adequate to enter either the given value for *t* and $p = -1000$, or the given value for *p* and $t = -1000$, plus the value for *x* (0 or 1). When *p* and *t* and *x* are entered as given values, the program will consider whether *p* and *t* fit together. If it is not the case the calculation of the function α_v will result in –1000.

Boundaries for wet steam region
The boundaries for the wet steam region are illustrated in Figure 1.1 and Figure 1.2.

Results for wrong input values

Result **alphav_ptx_air = –1000** or **ALPHAVPTXAIR = –1000** for the following input values:

Single phase region: $p > p_{max} = 20000$ or $p < p_{min} = 0.00001$ bar or
($x = -1$) $t > t_{max} = 1726.85$ °C or $t < t_{min} = -213.4$ °C or $t < t_{mel}(p)$

Saturated liquid line: at $p = -1$ and $t > t_{mct} = -140.5188$ °C or $t < t_{min} = -213.4$ °C or
($x = 0$) at $t = -1$ and $p > p_{mcb} = 37.9195$ bar or $p < p_{min,l} = 0.052646$ bar or

	at $p < p_{mcb}$ = 37.9195 bar and $p > p_{min,l}$ = 0.052646 bar and $\lvert t - t_{sl}(p) \rvert > 0.1\,\mathrm{K}$
Saturated vapor line: (x = 1)	at $p = -1$ and $t > t_{mct}$ = -140.5188 °C or $t < t_{min}$ = -213.4 °C or at $t = -1$ and $p > p_{mcb}$ = 37.9195 bar or $p < p_{min,v}$ = 0.024316 bar or at $p < p_{mcb}$ = 37.9195 bar and $p > p_{min,v}$ = 0.024316 bar and $\lvert t - t_{sv}(p) \rvert > 0.1\,\mathrm{K}$

Reference

[1]

Isothermal Stress Coefficient β_p = f(p,t,x)

Function Name: **betap_ptx_air**
Subroutine with function value: **REAL*8 FUNCTION BETAPPTXAIR(P,T,X)**
Variable Types: REAL*8 P,T,X

Input values

P - Pressure p in bar
T - Temperature t in °C
X - Vapor fraction x in (kg saturated steam)/(kg wet steam)

Result

betap_ptx_air or **BETAPPTXAIR** – Isothermal stress coefficient $\beta_p = \frac{\rho^2}{p}\left(\frac{\partial p}{\partial \rho}\right)_T$ in kg / m^3

Range of validity

Temperature range: from -213.4 °C (59.75 K) to 1726.85 °C (2000 K)
Pressure range: from 0.00001 bar to 20000 bar

Details on the vapor fraction *x*

The wet steam region is calculated automatically by the subprograms. For this purpose the following fixed details on the vapor fraction x are to be considered:

Single phase region
If the state point to be calculated is located in the single phase region (liquid or superheated steam) x = –1 must be entered as a pro-forma value.

Saturation lines
If the state point to be calculated is located on the saturated liquid line, the value 0 has to be entered for x. When calculating saturated steam (saturated vapor line) x = 1 has to be entered. The calculation for x values between 0 and 1 is not possible. It is adequate to enter either the given value for t and p = -1000, or the given value for p and t = –1000, plus the value for x (0 or 1). When p and t and x are entered as given values, the program will consider whether p and t fit together. If it is not the case the calculation of the function β_p will result in –1000.

Boundaries for wet steam region
The boundaries for the wet steam region are illustrated in Figure 1.1 and Figure 1.2.

Results for wrong input values

Result **betap_ptx_air = –1000** or **BETAPPTXAIR = –1000** for the following input values:

Single phase region: $p > p_{max}$ = 20000 or $p < p_{min}$ = 0.00001 bar or
(x = –1) $t > t_{max}$ = 1726.85 °C or $t < t_{min}$ = -213.4 °C or $t < t_{mel}(p)$

Saturated liquid line: at p = –1 and $t > t_{mct}$ = -140.5188 °C or $t < t_{min}$ = -213.4 °C or
(x = 0) at t = –1 and $p > p_{mcb}$ = 37.9195 bar or $p < p_{min,l}$ = 0.052646 bar or
at $p < p_{mcb}$ = 37.9195 bar and $p > p_{min,l}$ = 0.052646 bar and
$|t - t_{sl}(p)| > 0.1$K

Saturated vapor line:	at $p = -1$ and $t > t_{mct}$ = -140.5188 °C or $t < t_{min}$ = -213.4 °C or
(x = 1)	at $t = -1$ and $p > p_{mcb}$ = 37.9195 bar or $p < p_{min,v}$ = 0.024316 bar or
	at $p < p_{mcb}$ = 37.9195 bar and $p > p_{min,v}$ = 0.024316 bar and
	$\lvert t - t_{sv}(p) \rvert > 0.1\,\mathrm{K}$

Reference

[1]

Specific Isobaric Heat Capacity c_p = f(p,t,x)

Function Name: **cp_ptx_air**
Subroutine with function value: **REAL*8 FUNCTION CPPTXAIR(P,T,X)**
Variable Types: REAL*8 P,T,X

Input values

P - Pressure p in bar
T - Temperature t in °C
X - Vapor fraction x in (kg saturated steam)/(kg wet steam)

Result

cp_ptx_air or **CPPTXAIR** – Specific isobaric heat capacity c_p in kJ/(kg·K)

Range of validity

Temperature range: from -213.4 °C (59.75 K) to 1726.85 °C (2000 K)
Pressure range: from 0.00001 bar to 20000 bar

Details on the vapor fraction *x*

The wet steam region is calculated automatically by the subprograms. For this purpose the following fixed details on the vapor fraction x are to be considered:

Single phase region
If the state point to be calculated is located in the single phase region (liquid or superheated steam) x = –1 must be entered as a pro-forma value.

Saturation lines
If the state point to be calculated is located on the saturated liquid line, the value 0 has to be entered for x. When calculating saturated steam (saturated vapor line) x = 1 has to be entered. The calculation for x values between 0 and 1 is not possible. It is adequate to enter either the given value for t and p = -1000, or the given value for p and t = –1000, plus the value for x (0 or 1). When p and t and x are entered as given values, the program will consider whether p and t fit together. If it is not the case the calculation of the function c_p will result in –1000.

Boundaries for wet steam region
The boundaries for the wet steam region are illustrated in Figure 1.1 and Figure 1.2.

Results for wrong input values

Result **cp_ptx_air = –1000** or **CPPTXAIR = –1000** for the following input values:

Single phase region: $p > p_{max}$ = 20000 or $p < p_{min}$ = 0.00001 bar or
(x = –1) $t > t_{max}$ = 1726.85 °C or $t < t_{min}$ = -213.4 °C or $t < t_{mel}(p)$

Saturated liquid line: at p = –1 and $t > t_{mct}$ = -140.5188 °C or $t < t_{min}$ = -213.4 °C or
(x = 0) at t = –1 and $p > p_{mcb}$ = 37.9195 bar or $p < p_{min,l}$ = 0.052646 bar or
at $p < p_{mcb}$ = 37.9195 bar and $p > p_{min,l}$ = 0.052646 bar and
$|t - t_{sl}(p)| > 0.1\,\mathrm{K}$

Saturated vapor line:	at $p = -1$ and $t > t_{mct}$ = -140.5188 °C or $t < t_{min}$ = -213.4 °C or
(x = 1)	at $t = -1$ and $p > p_{mcb}$ = 37.9195 bar or $p < p_{min,v}$ = 0.024316 bar or
	at $p < p_{mcb}$ = 37.9195 bar and $p > p_{min,v}$ = 0.024316 bar and
	$\lvert t - t_{sv}(p) \rvert > 0.1\,\mathrm{K}$

Reference

[1]

Specific Isochoric Heat Capacity c_V = f(p,t,x)

Function Name: **cv_ptx_air**
Subroutine with function value: **REAL*8 FUNCTION CVPTXAIR(P,T,X)**
Variable Types: REAL*8 P,T,X

Input values

P - Pressure p in bar
T - Temperature t in °C
X - Vapor fraction x in (kg saturated steam)/(kg wet steam)

Result

cv_ptx_air or **CVPTXAIR** – Specific isochoric heat capacity c_V in kJ/(kg·K)

Range of validity

Temperature range: from -213.4 °C (59.75 K) to 1726.85 °C (2000 K)
Pressure range: from 0.00001 bar to 20000 bar

Details on the vapor fraction *x*

The wet steam region is calculated automatically by the subprograms. For this purpose the following fixed details on the vapor fraction x are to be considered:

Single phase region
If the state point to be calculated is located in the single phase region (liquid or superheated steam) x = –1 must be entered as a pro-forma value.

Saturation lines
If the state point to be calculated is located on the saturated liquid line, the value 0 has to be entered for x. When calculating saturated steam (saturated vapor line) x = 1 has to be entered. The calculation for x values between 0 and 1 is not possible. It is adequate to enter either the given value for t and p = -1000, or the given value for p and t = –1000, plus the value for x (0 or 1). When p and t and x are entered as given values, the program will consider whether p and t fit together. If it is not the case the calculation of the function c_V will result in –1000.

Boundaries for wet steam region
The boundaries for the wet steam region are illustrated in Figure 1.1 and Figure 1.2.

Results for wrong input values

Result **cv_ptx_air = –1000** or **CVPTXAIR = –1000** for the following input values:

Single phase region: (x = –1)
$p > p_{max}$ = 20000 or $p < p_{min}$ = 0.00001 bar or
$t > t_{max}$ = 1726.85 °C or $t < t_{min}$ = -213.4 °C or $t < t_{mel}(p)$

Saturated liquid line: (x = 0)
at p = –1 and $t > t_{mct}$ = -140.5188 °C or $t < t_{min}$ = -213.4 °C or
at t = –1 and $p > p_{mcb}$ = 37.9195 bar or $p < p_{min,l}$ = 0.052646 bar or
at $p < p_{mcb}$ = 37.9195 bar and $p > p_{min,l}$ = 0.052646 bar and
$|t - t_{sl}(p)| > 0.1\,\mathrm{K}$

Saturated vapor line:	at $p = -1$ and $t > t_{mct}$ = -140.5188 °C or $t < t_{min}$ = -213.4 °C or
(x = 1)	at $t = -1$ and $p > p_{mcb}$ = 37.9195 bar or $p < p_{min,v}$ = 0.024316 bar or
	at $p < p_{mcb}$ = 37.9195 bar and $p > p_{min,v}$ = 0.024316 bar and
	$\lvert t - t_{sv}(p) \rvert > 0.1\,\mathrm{K}$

Reference

[1]

Dynamic Viscosity η = f(p,t,x)

Function Name: **eta_ptx_air**
Subroutine with function value: **REAL*8 FUNCTION ETAPTXAIR(P,T,X)**
Variable Types: REAL*8 P,T,X

Input values

P - Pressure p in bar
T - Temperature t in °C
X - Vapor fraction x in (kg saturated steam)/(kg wet steam)

Result

eta_ptx_air or **ETAPTXAIR** – Dynamic viscosity η in Pa·s

Range of validity

Temperature range: from -213.4 °C (59.75 K) to 1726.85 °C (2000 K)
Pressure range: from 0.00001 bar to 20000 bar

Details on the vapor fraction *x*

The wet steam region is calculated automatically by the subprograms. For this purpose the following fixed details on the vapor fraction x are to be considered:

Single phase region
If the state point to be calculated is located in the single phase region (liquid or superheated steam) x = –1 must be entered as a pro-forma value.

Saturation lines
If the state point to be calculated is located on the saturated liquid line, the value 0 has to be entered for x. When calculating saturated steam (saturated vapor line) x = 1 has to be entered. The calculation for x values between 0 and 1 is not possible. It is adequate to enter either the given value for t and p = -1000, or the given value for p and t = –1000, plus the value for x (0 or 1). When p and t and x are entered as given values, the program will consider whether p and t fit together. If it is not the case the calculation of the function η will result in –1000.

Boundaries for wet steam region
The boundaries for the wet steam region are illustrated in Figure 1.1 and Figure 1.2.

Results for wrong input values

Result **eta_ptx_air = –1000** or **ETAPTXAIR = –1000** for the following input values:

Single phase region: $p > p_{max}$ = 20000 or $p < p_{min}$ = 0.00001 bar or
(x = –1) $t > t_{max}$ = 1726.85 °C or $t < t_{min}$ = -213.4 °C or $t < t_{mel}(p)$

Saturated liquid line: at p = –1 and $t > t_{mct}$ = -140.5188 °C or $t < t_{min}$ = -213.4 °C or
(x = 0) at t = –1 and $p > p_{mcb}$ = 37.9195 bar or $p < p_{min,l}$ = 0.052646 bar or
at $p < p_{mcb}$ = 37.9195 bar and $p > p_{min,l}$ = 0.052646 bar and
$|t - t_{sl}(p)| > 0.1\,\mathrm{K}$

Saturated vapor line:	at $p = -1$ and $t > t_{mct}$ = -140.5188 °C or $t < t_{min}$ = -213.4 °C or
(x = 1)	at $t = -1$ and $p > p_{mcb}$ = 37.9195 bar or $p < p_{min,v}$ = 0.024316 bar or
	at $p < p_{mcb}$ = 37.9195 bar and $p > p_{min,v}$ = 0.024316 bar and
	$\lvert t - t_{sv}(p) \rvert > 0.1\,\mathrm{K}$

References

[1], [2]

Specific Enthalpy h = f(p,t,x)

Function Name: **h_ptx_air**
Subroutine with function value: **REAL*8 FUNCTION HPTXAIR(P,T,X)**
Variable Types: REAL*8 P,T,X

Input values

P - Pressure p in bar
T - Temperature t in °C
X - Vapor fraction x in (kg saturated steam)/(kg wet steam)

Result

h_ptx_air or **HPTXAIR** – Specific enthalpy h in kJ/kg

Range of validity

Temperature range: from -213.4 °C (59.75 K) to 1726.85 °C (2000 K)
Pressure range: from 0.00001 bar to 20000 bar

Details on the vapor fraction *x* and on the calculation of wet steam

The wet steam region is calculated automatically by the subprograms. For this purpose the following fixed details on the vapor fraction x are to be considered:

Single phase region
If the state point to be calculated is located in the single phase region (liquid or superheated steam) x = –1 must be entered as a pro-forma value.

Wet steam region
When calculating wet steam, a value between 0 and 1 (x = 0 for saturated liquid, x = 1 for saturated steam) must be entered. It is adequate to enter either the given value for t and p = –1000, or the given value for p and t = –1000, plus the value for x between 0 and 1. When p and t and x are entered as given values, the program will consider whether p and t fit together. If it is not the case the calculation of the function h will result in –1000.

Boundaries for wet steam region
The boundaries for the wet steam region are illustrated in Figure 1.1 and Figure 1.2.

Results for wrong input values

Result **h_ptx_air = –1000** or **HPTXAIR = –1000** for the following input values:

Single phase region: $p > p_{max}$ = 20000 or $p < p_{min}$ = 0.00001 bar or
(x = –1) $t > t_{max}$ = 1726.85 °C or $t < t_{min}$ = -213.4 °C or $t < t_{mel}(p)$

Saturated liquid line: at p = –1 and $t > t_{mct}$ = -140.5188 °C or $t < t_{min}$ = -213.4 °C or
(x = 0) at t = –1 and $p > p_{mcb}$ = 37.9195 bar or $p < p_{min,l}$ = 0.052646 bar or
at $p < p_{mcb}$ = 37.9195 bar and $p > p_{min,l}$ = 0.052646 bar and
$|t - t_{sl}(p)| > 0.1\,\mathrm{K}$

Saturated vapor line: at p = –1 and $t > t_{mct}$ = -140.5188 °C or $t < t_{min}$ = -213.4 °C or
(x = 1) at t = –1 and $p > p_{mcb}$ = 37.9195 bar or $p < p_{min,v}$ = 0.024316 bar or

at $p < p_{\mathrm{mcb}}$ = 37.9195 bar and $p > p_{\mathrm{min,v}}$ = 0.024316 bar and $|t - t_{\mathrm{sv}}(p)| > 0.1\mathrm{K}$

Reference

[1]

Isentropic Exponent κ = f(p,t,x)

Function Name: **kappa_ptx_air**
Subroutine with function value: **REAL*8 FUNCTION KAPPTXAIR(P,T,X)**
Variable Types: REAL*8 P,T,X

Input values

P - Pressure p in bar
T - Temperature t in °C
X - Vapor fraction x in (kg saturated steam)/(kg wet steam)

Result

kappa_ptx_air or **KAPPAPTXAIR** – Isentropic exponent $\kappa = -\frac{v}{p}\left(\frac{\partial p}{\partial v}\right)_s = \frac{w^2}{p \cdot v}$

Range of validity

Temperature range: from -213.4 °C (59.75 K) to 1726.85 °C (2000 K)
Pressure range: from 0.00001 bar to 20000 bar

Details on the vapor fraction *x*

The wet steam region is calculated automatically by the subprograms. For this purpose the following fixed details on the vapor fraction x are to be considered:

Single phase region
If the state point to be calculated is located in the single phase region (liquid or superheated steam) x = –1 must be entered as a pro-forma value.

Saturation lines
If the state point to be calculated is located on the saturated liquid line, the value 0 has to be entered for x. When calculating saturated steam (saturated vapor line) x = 1 has to be entered. The calculation for x values between 0 and 1 is not possible. It is adequate to enter either the given value for t and p = -1000, or the given value for p and t = –1000, plus the value for x (0 or 1). When p and t and x are entered as given values, the program will consider whether p and t fit together. If it is not the case the calculation of the function κ will result in –1000.

Boundaries for wet steam region
The boundaries for the wet steam region are illustrated in Figure 1.1 and Figure 1.2.

Results for wrong input values

Result **kappa_ptx_air = –1000** or **KAPPAPTXAIR = –1000** for the following input values:

Single phase region:	$p > p_{max}$ = 20000 or $p < p_{min}$ = 0.00001 bar or
(x = –1)	$t > t_{max}$ = 1726.85 °C or $t < t_{min}$ = -213.4 °C or $t < t_{mel}(p)$
Saturated liquid line:	at p = –1 and $t > t_{mct}$ = -140.5188 °C or $t < t_{min}$ = -213.4 °C or
(x = 0)	at t = –1 and $p > p_{mcb}$ = 37.9195 bar or $p < p_{min,l}$ = 0.052646 bar or
	at $p < p_{mcb}$ = 37.9195 bar and $p > p_{min,l}$ = 0.052646 bar and
	$\lvert t - t_{sl}(p) \rvert > 0.1\,\mathrm{K}$

Saturated vapor line:	at $p = -1$ and $t > t_{mct}$ = -140.5188 °C or $t < t_{min}$ = -213.4 °C or
(x = 1)	at $t = -1$ and $p > p_{mcb}$ = 37.9195 bar or $p < p_{min,v}$ = 0.024316 bar or
	at $p < p_{mcb}$ = 37.9195 bar and $p > p_{min,v}$ = 0.024316 bar and
	$\lvert t - t_{sv}(p) \rvert > 0.1\,\mathrm{K}$

Reference

[1]

Isothermal Compressibility κ_T = f(p,t,x)

Function Name: **kappat_ptx_air**
Subroutine with function value: **REAL*8 FUNCTION KAPPATPTXAIR(P,T,X)**
Variable Types: REAL*8 P,T,X

Input values

P - Pressure p in bar
T - Temperature t in °C
X - Vapor fraction x in (kg saturated steam)/(kg wet steam)

Result

kappat_ptx_air or **KAPPATPXAIR** - Isothermal compressibility $\kappa_T = -\frac{1}{v}\left(\frac{\partial v}{\partial p}\right)_T = v\left(\frac{\partial p}{\partial \rho}\right)_T^{-1}$

Range of validity

Temperature range: from -213.4 °C (59.75 K) to 1726.85 °C (2000 K)
Pressure range: from 0.00001 bar to 20000 bar

Details on the vapor fraction *x*

The wet steam region is calculated automatically by the subprograms. For this purpose the following fixed details on the vapor fraction x are to be considered:

Single phase region
If the state point to be calculated is located in the single phase region (liquid or superheated steam) x = –1 must be entered as a pro-forma value.

Saturation lines
If the state point to be calculated is located on the saturated liquid line, the value 0 has to be entered for x. When calculating saturated steam (saturated vapor line) x = 1 has to be entered. The calculation for x values between 0 and 1 is not possible. It is adequate to enter either the given value for t and p = -1000, or the given value for p and t = –1000, plus the value for x (0 or 1). When p and t and x are entered as given values, the program will consider whether p and t fit together. If it is not the case the calculation of the function κ_T will result in –1000.

Boundaries for wet steam region
The boundaries for the wet steam region are illustrated in Figure 1.1 and Figure 1.2.

Results for wrong input values

Result **kappat_ptx_air = –1000** or **KAPPATPTXAIR = –1000** for the following input values:

Single phase region: $p > p_{max}$ = 20000 or $p < p_{min}$ = 0.00001 bar or
(x = –1) $t > t_{max}$ = 1726.85 °C or $t < t_{min}$ = -213.4 °C or $t < t_{mel}(p)$

Saturated liquid line:	at $p = -1$ and $t > t_{mct}$ = -140.5188 °C or $t < t_{min}$ = -213.4 °C or
(x = 0)	at $t = -1$ and $p > p_{mcb}$ = 37.9195 bar or $p < p_{min,l}$ = 0.052646 bar or
	at $p < p_{mcb}$ = 37.9195 bar and $p > p_{min,l}$ = 0.052646 bar and
	$\lvert t - t_{sl}(p) \rvert > 0.1\,\mathrm{K}$
Saturated vapor line:	at $p = -1$ and $t > t_{mct}$ = -140.5188 °C or $t < t_{min}$ = -213.4 °C or
(x = 1)	at $t = -1$ and $p > p_{mcb}$ = 37.9195 bar or $p < p_{min,v}$ = 0.024316 bar or
	at $p < p_{mcb}$ = 37.9195 bar and $p > p_{min,v}$ = 0.024316 bar and
	$\lvert t - t_{sv}(p) \rvert > 0.1\,\mathrm{K}$

Reference

[1]

Thermal Conductivity λ = f(p,t,x)

Function Name: **lambda_ptx_air**
Subroutine with function value: **REAL*8 FUNCTION LAMBDAPTXAIR(P,T,X)**
Variable Types: REAL*8 P,T,X

Input values

P - Pressure p in bar
T - Temperature t in °C
X - Vapor fraction x in (kg saturated steam)/(kg wet steam)

Result

lambda_ptx_air or **LAMBDAPTXAIR** – Thermal conductivity λ in W/(m·K)

Range of validity

Temperature range: from -213.4 °C (59.75 K) to 1726.85 °C (2000 K)
Pressure range: from 0.00001 bar to 20000 bar

Details on the vapor fraction *x*

The wet steam region is calculated automatically by the subprograms. For this purpose the following fixed details on the vapor fraction x are to be considered:

Single phase region
If the state point to be calculated is located in the single phase region (liquid or superheated steam) x = –1 must be entered as a pro-forma value.

Saturation lines
If the state point to be calculated is located on the saturated liquid line, the value 0 has to be entered for x. When calculating saturated steam (saturated vapor line) x = 1 has to be entered. The calculation for x values between 0 and 1 is not possible. It is adequate to enter either the given value for t and p = -1000, or the given value for p and t = –1000, plus the value for x (0 or 1). When p and t and x are entered as given values, the program will consider whether p and t fit together. If it is not the case the calculation of the function λ will result in –1000.

Boundaries for wet steam region
The boundaries for the wet steam region are illustrated in Figure 1.1 and Figure 1.2.

Results for wrong input values

Result **lambda_ptx_air = –1000** or **LAMBDAPTXAIR = –1000** for the following input values:

Single phase region: $p > p_{max}$ = 20000 or $p < p_{min}$ = 0.00001 bar or
(x = –1) $t > t_{max}$ = 1726.85 °C or $t < t_{min}$ = -213.4 °C or $t < t_{mel}(p)$

Saturated liquid line: at p = –1 and $t > t_{mct}$ = -140.5188 °C or $t < t_{min}$ = -213.4 °C or
(x = 0) at t = –1 and $p > p_{mcb}$ = 37.9195 bar or $p < p_{min,l}$ = 0.052646 bar or
at $p < p_{mcb}$ = 37.9195 bar and $p > p_{min,l}$ = 0.052646 bar and
$|t - t_{sl}(p)| > 0.1\,\mathrm{K}$

Saturated vapor line:	at $p = -1$ and $t > t_{mct}$ = -140.5188 °C or $t < t_{min}$ = -213.4 °C or
(x = 1)	at $t = -1$ and $p > p_{mcb}$ = 37.9195 bar or $p < p_{min,v}$ = 0.024316 bar or
	at $p < p_{mcb}$ = 37.9195 bar and $p > p_{min,v}$ = 0.024316 bar and
	$\lvert t - t_{sv}(p) \rvert > 0.1\,\mathrm{K}$

References

[1], [2]

Kinematic Viscosity ν = f(p,t,x)

Function Name: **nu_ptx_air**
Subroutine with function value: **REAL*8 FUNCTION NUPTXAIR(P,T,X)**
Variable Types: REAL*8 P,T,X

Input values

P - Pressure p in bar
T - Temperature t in °C
X - Vapor fraction x in (kg saturated steam)/(kg wet steam)

Result

nu_ptx_air or **NUPTXAIR** – Kinematic viscosity $\nu = \frac{\eta}{\rho} = \eta \cdot \mathrm{v}$ in m²/s

Range of validity

Temperature range: from -213.4 °C (59.75 K) to 1726.85 °C (2000 K)
Pressure range: from 0.00001 bar to 20000 bar

Details on the vapor fraction *x*

The wet steam region is calculated automatically by the subprograms. For this purpose the following fixed details on the vapor fraction x are to be considered:

Single phase region
If the state point to be calculated is located in the single phase region (liquid or superheated steam) x = –1 must be entered as a pro-forma value.

Saturation lines
If the state point to be calculated is located on the saturated liquid line, the value 0 has to be entered for x. When calculating saturated steam (saturated vapor line) x = 1 has to be entered. The calculation for x values between 0 and 1 is not possible. It is adequate to enter either the given value for t and p = -1000, or the given value for p and t = –1000, plus the value for x (0 or 1). When p and t and x are entered as given values, the program will consider whether p and t fit together. If it is not the case the calculation of the function ν will result in –1000.

Boundaries for wet steam region
The boundaries for the wet steam region are illustrated in Figure 1.1 and Figure 1.2.

Results for wrong input values

Result **nu_ptx_air = –1000** or **NUPTXAIR = –1000** for the following input values:

Single phase region: $p > p_{max}$ = 20000 or $p < p_{min}$ = 0.00001 bar or
(x = –1) $t > t_{max}$ = 1726.85 °C or $t < t_{min}$ = -213.4 °C or $t < t_{mel}(p)$

Saturated liquid line: at p = –1 and $t > t_{mct}$ = -140.5188 °C or $t < t_{min}$ = -213.4 °C or
(x = 0) at t = –1 and $p > p_{mcb}$ = 37.9195 bar or $p < p_{min,l}$ = 0.052646 bar or
at $p < p_{mcb}$ = 37.9195 bar and $p > p_{min,l}$ = 0.052646 bar and
$|t - t_{sl}(p)| > 0.1\,\mathrm{K}$

Saturated vapor line:	at $p = -1$ and $t > t_{mct}$ = -140.5188 °C or $t < t_{min}$ = -213.4 °C or
(x = 1)	at $t = -1$ and $p > p_{mcb}$ = 37.9195 bar or $p < p_{min,v}$ = 0.024316 bar or
	at $p < p_{mcb}$ = 37.9195 bar and $p > p_{min,v}$ = 0.024316 bar and
	$\lvert t - t_{sv}(p) \rvert > 0.1\,\mathrm{K}$

References

[1], [2]

Pressure on the Melting Curve p_{mel} = f(t)

Function Name: **pmel_t_air**
Subroutine with function value: **REAL*8 FUNCTION PMELTAIR(T)**
Variable Types: REAL*8 T

Input values

T - Temperature t in °C

Result

pmel_t_air or **PMELTAIR** – Pressure on the melting curve p_{mel} in bar

Range of validity

Temperature range: from $t_t = t_{min}$ = -213.4 °C to t_{mel} (20000 bar) = -36.9508 °C

Results for wrong input values

Result **pmel_t_air = –1000** or **PMELTAIR = –1000** for the following input values:

$t > t_{mel}$ (20000 bar) = -36.9508 °C or $t < t_{min}$ = -213.4 °C or

Reference

[1]

Prandtl-Number Pr = f(*p*,*t*,*x*)

Function Name: **prandtl_ptx_air**
Subroutine with function value: **REAL*8 FUNCTION PRANDTLPTXAIR(P,T,X)**
Variable Types: REAL*8 P,T,X

Input values

P - Pressure *p* in bar
T - Temperature *t* in °C
X - Vapor fraction *x* in (kg saturated steam)/(kg wet steam)

Result

prandtl_ptx_air or **PRANDTLPTXAIR** – Prandtl-number $\mathrm{Pr} = \frac{\nu}{a} = \frac{\eta \cdot c_p}{\lambda}$

Range of validity

Temperature range: from -213.4 °C (59.75 K) to 1726.85 °C (2000 K)
Pressure range: from 0.00001 bar to 20000 bar

Details on the vapor fraction *x*

The wet steam region is calculated automatically by the subprograms. For this purpose the following fixed details on the vapor fraction *x* are to be considered:

Single phase region
If the state point to be calculated is located in the single phase region (liquid or superheated steam) *x* = –1 must be entered as a pro-forma value.

Saturation lines
If the state point to be calculated is located on the saturated liquid line, the value 0 has to be entered for *x*. When calculating saturated steam (saturated vapor line) *x* = 1 has to be entered. The calculation for *x* values between 0 and 1 is not possible. It is adequate to enter either the given value for *t* and *p* = -1000, or the given value for *p* and *t* = –1000, plus the value for *x* (0 or 1). When *p* and *t* and *x* are entered as given values, the program will consider whether *p* and *t* fit together. If it is not the case the calculation of the function Pr will result in –1000.

Boundaries for wet steam region
The boundaries for the wet steam region are illustrated in Figure 1.1 and Figure 1.2.

Results for wrong input values

Result **prandtl_ptx_air = –1000** or **PRANDTLPTXAIR = –1000** for the following input values:

Single phase region:	$p > p_{max}$ = 20000 or $p < p_{min}$ = 0.00001 bar or
(*x* = –1)	$t > t_{max}$ = 1726.85 °C or $t < t_{min}$ = -213.4 °C or $t < t_{mel}(p)$
Saturated liquid line:	at p = –1 and $t > t_{mct}$ = -140.5188 °C or $t < t_{min}$ = -213.4 °C or
(*x* = 0)	at t = –1 and $p > p_{mcb}$ = 37.9195 bar or $p < p_{min,l}$ = 0.052646 bar or
	at $p < p_{mcb}$ = 37.9195 bar and $p > p_{min,l}$ = 0.052646 bar and
	$\lvert t - t_{sl}(p) \rvert > 0.1\,\mathrm{K}$

Saturated vapor line:	at $p = -1$ and $t > t_{mct}$ = -140.5188 °C or $t < t_{min}$ = -213.4 °C or
(x = 1)	at $t = -1$ and $p > p_{mcb}$ = 37.9195 bar or $p < p_{min,v}$ = 0.024316 bar or
	at $p < p_{mcb}$ = 37.9195 bar and $p > p_{min,v}$ = 0.024316 bar and
	$\lvert t - t_{sv}(p) \rvert > 0.1\,\mathrm{K}$

References

[1], [2]

Pressure on the Saturated Liquid Line p_{sl} = f(t)

Function Name: **psl_t_air**
Subroutine with function value: **REAL*8 FUNCTION PSLTAIR(T)**
Variable Types: REAL*8 T

Input values

T - Temperature t in °C

Result

psl_t_air or **PSLTAIR** – Pressure on the saturated liquid line p_{sl} in bar

Range of validity

Temperature range: from t_{min} = -213.4 °C to t_{mct} = -140.5188 °C

Details on the saturation lines

The boundaries for the wet steam region are illustrated in Figure 1.1 and Figure 1.2. In order that the function p_{sv} = f(t) will not be double-valued in the critical region, the saturated vapor line (x = 1) is partially represented by the function p_{sl} = f(t) calculating pressures on the saturated liquid line (x = 0). This concerns the segment between the critical point and the maxcondentherm point.

Results for wrong input values

Result **psl_t_air = –1000** or **PSLTAIR = –1000** for the following input values:

$t > t_{mct}$ = -140.5188 °C or $t < t_{min}$ = -213.4 °C

Reference

[1]

Pressure on the Saturated Vapor Line p_{sv} = f(t)

Function Name: **psv_t_air**
Subroutine with function value: **REAL*8 FUNCTION PSVTAIR(T)**
Variable Types: REAL*8 T

Input values

T - Temperature t in °C

Result

psv_t_air or **PSVTAIR** – Pressure on the saturated vapor line p_{sv} in bar

Range of validity

Temperature range: from t_{min} = -213.4 °C to t_{mct} = -140.5188 °C

Details on the saturation lines

The boundaries for the wet steam region are illustrated in Figure 1.1 and Figure 1.2. In order that the function p_{sv} = f(t) will not be double-valued in the critical region, the saturated vapor line (x = 1) is partially represented by the function p_{sl} = f(t) calculating pressures on the saturated liquid line (x = 0). This concerns the segment between the critical point and the maxcondentherm point.

Results for wrong input values

Result **psv_t_air = –1000** or **PSVTAIR = –1000** for the following input values:

$t > t_{mct}$ = -140.5188 °C or $t < t_{min}$ = -213.4 °C

Reference

[1]

Density ρ = f(p,t, x)

Function Name: **rho_ptx_air**
Subroutine with function value: **REAL*8 FUNCTION RHOPTXAIR(P,T,X)**
Variable Types: REAL*8 P,T,X

Input values

P - Pressure p in bar
T - Temperature t in °C
X - Vapor fraction x in (kg saturated steam)/(kg wet steam)

Result

rho_ptx_air or **RHOPTXAIR** – Density $\rho = \frac{1}{v}$ in kg/m^3

Range of validity

Temperature range: from -213.4 °C (59.75 K) to 1726.85 °C (2000 K)
Pressure range: from 0.00001 bar to 20000 bar

Details on the vapor fraction *x* and on the calculation of wet steam

The wet steam region is calculated automatically by the subprograms. For this purpose the following fixed details on the vapor fraction x are to be considered:

Single phase region
If the state point to be calculated is located in the single phase region (liquid or superheated steam) x = –1 must be entered as a pro-forma value.

Wet steam region
When calculating wet steam, a value between 0 and 1 (x = 0 for saturated liquid, x = 1 for saturated steam) must be entered. It is adequate to enter either the given value for t and p = –1000, or the given value for p and t = –1000, plus the value for x between 0 and 1. When p and t and x are entered as given values, the program will consider whether p and t fit together. If it is not the case the calculation of the function ρ will result in –1000.

Boundaries for wet steam region
The boundaries for the wet steam region are illustrated in Figure 1.1 and Figure 1.2.

Results for wrong input values

Result **rho_ptx_air = –1000** or **RHOPTXAIR = –1000** for the following input values:

Single phase region: (x = –1)
$p > p_{max}$ = 20000 or $p < p_{min}$ = 0.00001 bar or
$t > t_{max}$ = 1726.85 °C or $t < t_{min}$ = -213.4 °C or $t < t_{mel}(p)$

Saturated liquid line: (x = 0)
at p = –1 and $t > t_{mct}$ = -140.5188 °C or $t < t_{min}$ = -213.4 °C or
at t = –1 and $p > p_{mcb}$ = 37.9195 bar or $p < p_{min,l}$ = 0.052646 bar or
at $p < p_{mcb}$ = 37.9195 bar and $p > p_{min,l}$ = 0.052646 bar and
$|t - t_{sl}(p)| > 0.1\,\mathrm{K}$

Saturated vapor line: (x = 1)
at p = –1 and $t > t_{mct}$ = -140.5188 °C or $t < t_{min}$ = -213.4 °C or
at t = –1 and $p > p_{mcb}$ = 37.9195 bar or $p < p_{min,v}$ = 0.024316 bar or

at $p < p_{\mathrm{mcb}}$ = 37.9195 bar and $p > p_{\mathrm{min,v}}$ = 0.024316 bar and $|t - t_{\mathrm{sv}}(p)| > 0.1\mathrm{K}$

Reference

[1]

Specific Entropy $s = f(p,t,x)$

Function Name: **s_ptx_air**
Subroutine with function value: **REAL*8 FUNCTION SPTXAIR(P,T,X)**
Variable Types: REAL*8 P,T,X

Input values

P - Pressure p in bar
T - Temperature t in °C
X - Vapor fraction x in (kg saturated steam)/(kg wet steam)

Result

s_ptx_air or **SPTXAIR** – Specific entropy s in kJ/kg

Range of validity

Temperature range: from -213.4 °C (59.75 K) to 1726.85 °C (2000 K)
Pressure range: from 0.00001 bar to 20000 bar

Details on the vapor fraction *x* and on the calculation of wet steam

The wet steam region is calculated automatically by the subprograms. For this purpose the following fixed details on the vapor fraction x are to be considered:

Single phase region
If the state point to be calculated is located in the single phase region (liquid or superheated steam) $x = -1$ must be entered as a pro-forma value.

Wet steam region
When calculating wet steam, a value between 0 and 1 ($x = 0$ for saturated liquid, $x = 1$ for saturated steam) must be entered. It is adequate to enter either the given value for t and $p = -1000$, or the given value for p and $t = -1000$, plus the value for x between 0 and 1. When p and t and x are entered as given values, the program will consider whether p and t fit together. If it is not the case the calculation of the function s will result in –1000.

Boundaries for wet steam region
The boundaries for the wet steam region are illustrated in Figure 1.1 and Figure 1.2.

Results for wrong input values

Result **s_ptx_air = –1000** or **SPTXAIR = –1000** for the following input values:

Single phase region: $p > p_{max}$ = 20000 or $p < p_{min}$ = 0.00001 bar or
($x = -1$) $t > t_{max}$ = 1726.85 °C or $t < t_{min}$ = -213.4 °C or $t < t_{mel}(p)$

Saturated liquid line: at $p = -1$ and $t > t_{mct}$ = -140.5188 °C or $t < t_{min}$ = -213.4 °C or
($x = 0$) at $t = -1$ and $p > p_{mcb}$ = 37.9195 bar or $p < p_{min,l}$ = 0.052646 bar or
at $p < p_{mcb}$ = 37.9195 bar and $p > p_{min,l}$ = 0.052646 bar and
$|t - t_{sl}(p)| > 0.1\,\mathrm{K}$

Saturated vapor line: at $p = -1$ and $t > t_{mct}$ = -140.5188 °C or $t < t_{min}$ = -213.4 °C or
($x = 1$) at $t = -1$ and $p > p_{mcb}$ = 37.9195 bar or $p < p_{min,v}$ = 0.024316 bar or

at $p < p_{\mathrm{mcb}}$ = 37.9195 bar and $p > p_{\mathrm{min,v}}$ = 0.024316 bar and $|t - t_{\mathrm{sv}}(p)| > 0.1\mathrm{K}$

Reference

[1]

Temperature on the Melting Curve t_{mel} = f(p)

Function Name: **tmel_p_air**
Subroutine with function value: **REAL*8 FUNCTION TMELPAIR(P)**
Variable Types: REAL*8 P

Input values

P – Pressure p in bar

Result

tmel_p_air or **TMELPAIR** – Temperature on the melting curve t_{mel} in °C

Range of validity

Pressure range: from $p_t = p_{min,l}$ = 0.052646 bar to p_{max} = 20000 bar

Results for wrong input values

Result **tmel_t_air = –1000** or **TMELPAIR = –1000** for the following input values:

$p > p_{max}$ = 20000 bar or $p < p_{min,l}$ = 0.052646 bar

Reference

[1]

Backward Function: Temperature t = f(p,h)

Function Name: **t_ph_air**
Subroutine with function value: **REAL*8 FUNCTION TPHAIR(P,H)**
Variable Types: REAL*8 P,H

Input values

P - Pressure p in bar
H - Specific enthalpy h in kJ/kg

Result

t_ph_air or **TPHAIR** – Temperature t in °C

Range of validity

Temperature range: from -213.4 °C (59.75 K) to 1726.85 °C (2000 K)
Pressure range: from 0.00001 bar to 20000 bar

Details on the calculation of wet steam

The wet steam region is calculated automatically by the subprograms. Using the given values for p and h the program determines whether the state point to be calculated is located within the single phase region (liquid or superheated steam) or the wet steam region. After that, the calculation is carried out for the specific region.

The boundaries for the wet steam region are illustrated in Figure 1.1 and Figure 1.2.

Results for wrong input values

Result **t_ph_air = –1000** or **TPHAIR =–1000** for the following input values:

Single phase region: $p > p_{max}$ = 20000 or $p < p_{min}$ = 0.00001 bar or
$t > t_{max}$ = 1726.85 °C or $t < t_{min}$ = -213.4 °C or $t < t_{mel}(p)$

Saturated liquid line: at $p > p_{mcb}$ = 37.9195 bar or $p < p_{min,l}$ = 0.052646 bar or
at result $t > t_{mcb}$ = -140.5539 °C or $t < t_{min}$ = -213.4 °C

Saturated vapor line: at $p > p_{mcb}$ = 37.9195 bar or $p < p_{min,v}$ = 0.024316 bar or
at result $t > t_{mcb}$ = -140.5539 °C or $t < t_{min}$ = -213.4 °C or

Reference

[1]

Backward Function: Temperature t = f(p, s)

Function Name: **t_ps_air**
Subroutine with function value: **REAL*8 FUNCTION TPSAIR(P,S)**
Variable Types: REAL*8 P,S

Input values

P - Pressure p in bar
S - Specific entropy s in kJ/(kg·K)

Result

t_ps_air or **TPSAIR** – Temperature t in °C

Range of validity

Temperature range: from -213.4 °C (59.75 K) to 1726.85 °C (2000 K)
Pressure range: from 0.00001 bar to 20000 bar

Details on the calculation of wet steam

The wet steam region is calculated automatically by the subprograms. Using the given values for p and s the program determines whether the state point to be calculated is located within the single phase region (liquid or superheated steam) or the wet steam region. After that, the calculation is carried out for the specific region.

The boundaries for the wet steam region are illustrated in Figure 1.1 and Figure 1.2.

Results for wrong input values

Result **t_ps_air = –1000** or **TPSAIR =–1000** for the following input values:

Single phase region: $p > p_{max}$ = 20000 or $p < p_{min}$ = 0.00001 bar or
$t > t_{max}$ = 1726.85 °C or $t < t_{min}$ = -213.4 °C or $t < t_{mel}(p)$

Saturated liquid line: at $p > p_{mcb}$ = 37.9195 bar or = 0.052646 bar or
at result $t > t_{mcb}$ = -140.5539 °C or $t < t_{min}$ = -213.4 °C

Saturated vapor line: at $p > p_{mcb}$ = 37.9195 bar or $p < p_{min,v}$ = 0.024316 bar or
at result $t > t_{mcb}$ = -140.5539 °C or $t < t_{min}$ = -213.4 °C or

Reference

[1]

Temperature on the Saturated Liquid Line t_{sl} = f(p)

Function Name: **tsl_p_air**
Subroutine with function value: **REAL*8 FUNCTION TSLPAIR(P)**
Variable Types: REAL*8 P

Input values

P - Pressure p in bar

Result

tsl_p_air or **TSLPAIR** – Temperature on the saturated liquid line t_{sl} in °C

Range of validity

Pressure range: from $p_{min,l}$ = 0.052646 bar to p_{mcb} = 37.9195 bar

Details on the saturation lines

The boundaries for the wet steam region are illustrated in Figure 1.1 and Figure 1.2. In order that the function t_{sv} = f(p) will not be double-valued in the critical region, the saturated vapor line (x = 1) is partially represented by the function t_{sl} = f(p) calculating temperatures on the saturated liquid line (x = 0). This concerns the segment between the critical point and the maxcondenbar point.

Results for wrong input values

Result **tsl_p_air = –1000** or **TSLPAIR = –1000** for the following input values:

$p > p_{mcb}$ = 37.9195 bar or $p < p_{min,l}$ = 0.052646 bar

Reference

[1]

Temperature on the Saturated Vapor Line t_{sv} = f(p)

Function Name: **tsv_p_air**
Subroutine with function value: **REAL*8 FUNCTION TSVPAIR(P)**
Variable Types: REAL*8 P

Input values

P - Pressure p in bar

Result

tsv_p_air or **TSVPAIR** – Temperature on the saturated vapor line t_{sv} in °C

Range of validity

Pressure range: from $p_{min,v}$ = 0.024316 bar to p_{mcb} = 37.9195 bar

Details on the saturation lines

The boundaries for the wet steam region are illustrated in Figure 1.1 and Figure 1.2. In order that the function t_{sv} = f(p) will not be double-valued in the critical region, the saturated vapor line (x = 1) is partially represented by the function t_{sl} = f(p) calculating temperatures on the saturated liquid line (x = 0). This concerns the segment between the critical point and the maxcondenbar point.

Results for wrong input values

Result **tsv_p_air = –1000** or **TSVPAIR = –1000** for the following input values:

$p > p_{mcb}$ = 37.9195 bar or $p < p_{min,v}$ = 0.024316 bar

Reference

[1]

Specific Internal Energy u = f(p,t,x)

Function Name: **u_ptx_air**
Subroutine with function value: **REAL*8 FUNCTION UPTXAIR(P,T,X)**
Variable Types: REAL*8 P,T,X

Input values

P - Pressure p in bar
T - Temperature t in °C
X - Vapor fraction x in (kg saturated steam)/(kg wet steam)

Result

u_ptx_air or **UPTXAIR** – Specific internal energy u in kJ/kg

Range of validity

Temperature range: from -213.4 °C (59.75 K) to 1726.85 °C (2000 K)
Pressure range: from 0.00001 bar to 20000 bar

Details on the vapor fraction *x* and on the calculation of wet steam

The wet steam region is calculated automatically by the subprograms. For this purpose the following fixed details on the vapor fraction x are to be considered:

Single phase region
If the state point to be calculated is located in the single phase region (liquid or superheated steam) $x = -1$ must be entered as a pro-forma value.

Wet steam region
When calculating wet steam, a value between 0 and 1 ($x = 0$ for saturated liquid, $x = 1$ for saturated steam) must be entered. It is adequate to enter either the given value for t and $p = -1000$, or the given value for p and $t = -1000$, plus the value for x between 0 and 1. When p and t and x are entered as given values, the program will consider whether p and t fit together. If it is not the case the calculation of the function u will result in –1000.

Boundaries for wet steam region
The boundaries for the wet steam region are illustrated in Figure 1.1 and Figure 1.2.

Results for wrong input values

Result **u_ptx_air = –1000** or **UPTXAIR = –1000** for the following input values:

Single phase region: $p > p_{max}$ = 20000 or $p < p_{min}$ = 0.00001 bar or
($x = -1$) $t > t_{max}$ = 1726.85 °C or $t < t_{min}$ = -213.4 °C or $t < t_{mel}(p)$

Saturated liquid line: at $p = -1$ and $t > t_{mct}$ = -140.5188 °C or $t < t_{min}$ = -213.4 °C or
($x = 0$) at $t = -1$ and $p > p_{mcb}$ = 37.9195 bar or $p < p_{min,l}$ = 0.052646 bar or
at $p < p_{mcb}$ = 37.9195 bar and $p > p_{min,l}$ = 0.052646 bar and
$|t - t_{sl}(p)| > 0.1\,\mathrm{K}$

Saturated vapor line: at $p = -1$ and $t > t_{mct}$ = -140.5188 °C or $t < t_{min}$ = -213.4 °C or
($x = 1$) at $t = -1$ and $p > p_{mcb}$ = 37.9195 bar or $p < p_{min,v}$ = 0.024316 bar or

at $p < p_{\mathrm{mcb}}$ = 37.9195 bar and $p > p_{\mathrm{min,v}}$ = 0.024316 bar and $|t - t_{\mathrm{sv}}(p)| > 0.1\mathrm{K}$

Reference

[1]

Specific Volume v = f(p,t,x)

Function Name: **v_ptx_air**
Subroutine with function value: **REAL*8 FUNCTION VPTXAIR(P,T,X)**
Variable Types: REAL*8 P,T,X

Input values

P - Pressure p in bar
T - Temperature t in °C
X - Vapor fraction x in (kg saturated steam)/(kg wet steam)

Result

v_ptx_air or **VPTXAIR** – Specific volume v in m^3/kg

Range of validity

Temperature range: from -213.4 °C (59.75 K) to 1726.85 °C (2000 K)
Pressure range: from 0.00001 bar to 20000 bar

Details on the vapor fraction *x* and on the calculation of wet steam

The wet steam region is calculated automatically by the subprograms. For this purpose the following fixed details on the vapor fraction x are to be considered:

Single phase region
If the state point to be calculated is located in the single phase region (liquid or superheated steam) $x = -1$ must be entered as a pro-forma value.

Wet steam region
When calculating wet steam, a value between 0 and 1 ($x = 0$ for saturated liquid, $x = 1$ for saturated steam) must be entered. It is adequate to enter either the given value for t and $p = -1000$, or the given value for p and $t = -1000$, plus the value for x between 0 and 1. When p and t and x are entered as given values, the program will consider whether p and t fit together. If it is not the case the calculation of the function v will result in –1000.

Boundaries for wet steam region
The boundaries for the wet steam region are illustrated in Figure 1.1 and Figure 1.2.

Results for wrong input values

Result **v_ptx_air = –1000** or **VPTXAIR = –1000** for the following input values:

Single phase region: $p > p_{max}$ = 20000 or $p < p_{min}$ = 0.00001 bar or
($x = -1$) $t > t_{max}$ = 1726.85 °C or $t < t_{min}$ = -213.4 °C or $t < t_{mel}(p)$

Saturated liquid line: at $p = -1$ and $t > t_{mct}$ = -140.5188 °C or $t < t_{min}$ = -213.4 °C or
($x = 0$) at $t = -1$ and $p > p_{mcb}$ = 37.9195 bar or $p < p_{min,l}$ = 0.052646 bar or
at $p < p_{mcb}$ = 37.9195 bar and $p > p_{min,l}$ = 0.052646 bar and
$|t - t_{sl}(p)| > 0.1\,\mathrm{K}$

Saturated vapor line: at $p = -1$ and $t > t_{mct}$ = -140.5188 °C or $t < t_{min}$ = -213.4 °C or
($x = 1$) at $t = -1$ and $p > p_{mcb}$ = 37.9195 bar or $p < p_{min,v}$ = 0.024316 bar or

at $p < p_{\mathrm{mcb}}$ = 37.9195 bar and $p > p_{\mathrm{min,v}}$ = 0.024316 bar and $|t - t_{\mathrm{sv}}(p)| > 0.1\mathrm{K}$

Reference

[1]

Isentropic Speed of Sound $w = f(p,t,x)$

Function Name: **w_ptx_air**
Subroutine with function value: **REAL*8 FUNCTION WPTXAIR(P,T,X)**
Variable Types: REAL*8 P,T,X

Input values

P - Pressure p in bar
T - Temperature t in °C
X - Vapor fraction x in (kg saturated steam)/(kg wet steam)

Result

w_ptx_air or **WPTXAIR** – Isentropic speed of sound w in m/s

Range of validity

Temperature range: from -213.4 °C (59.75 K) to 1726.85 °C (2000 K)
Pressure range: from 0.00001 bar to 20000 bar

Details on the vapor fraction *x*

The wet steam region is calculated automatically by the subprograms. For this purpose the following fixed details on the vapor fraction x are to be considered:

Single phase region
If the state point to be calculated is located in the single phase region (liquid or superheated steam) $x = -1$ must be entered as a pro-forma value.

Saturation lines
If the state point to be calculated is located on the saturated liquid line, the value 0 has to be entered for x. When calculating saturated steam (saturated vapor line) $x = 1$ has to be entered. The calculation for x values between 0 and 1 is not possible. It is adequate to enter either the given value for t and $p = -1000$, or the given value for p and $t = -1000$, plus the value for x (0 or 1). When p and t and x are entered as given values, the program will consider whether p and t fit together. If it is not the case the calculation of the function w will result in –1000.

Boundaries for wet steam region
The boundaries for the wet steam region are illustrated in Figure 1.1 and Figure 1.2.

Results for wrong input values

Result **w_ptx_air = –1000** or **WPTXAIR = –1000** for the following input values:

Single phase region:	$p > p_{max} = 20000$ or $p < p_{min} = 0.00001$ bar or
($x = -1$)	$t > t_{max} = 1726.85$ °C or $t < t_{min} = -213.4$ °C or $t < t_{mel}(p)$
Saturated liquid line:	at $p = -1$ and $t > t_{mct} = -140.5188$ °C or $t < t_{min} = -213.4$ °C or
($x = 0$)	at $t = -1$ and $p > p_{mcb} = 37.9195$ bar or $p < p_{min,l} = 0.052646$ bar or
	at $p < p_{mcb} = 37.9195$ bar and $p > p_{min,l} = 0.052646$ bar and
	$\lvert t - t_{sl}(p) \rvert > 0.1\,\mathrm{K}$

Saturated vapor line:	at $p = -1$ and $t > t_{mct}$ = -140.5188 °C or $t < t_{min}$ = -213.4 °C or
(x = 1)	at $t = -1$ and $p > p_{mcb}$ = 37.9195 bar or $p < p_{min,v}$ = 0.024316 bar or
	at $p < p_{mcb}$ = 37.9195 bar and $p > p_{min,v}$ = 0.024316 bar and
	$\lvert t - t_{sv}(p) \rvert > 0.1\,\mathrm{K}$

References

[1], [2]

Backward Function: Vapor Fraction *x* = f(*p*,*h*)

Function Name: **x_ph_air**
Subroutine with function value: **REAL*8 FUNCTION XPHAIR(P,H)**
Variable Types: REAL*8 P,H

Input values

P - Pressure *p* in bar
H - Specific enthalpy *h* in kJ/kg

Result

x_ph_air or **XPHAIR** – Vapor fraction *x* in (kg saturated steam)/(kg wet steam)

Range of validity

Temperature range: from -213.4 °C (59.75 K) to 1726.85 °C (2000 K)
Pressure range: from 0.00001 bar to 20000 bar

Details on the calculation of wet steam

The wet steam region is calculated automatically by the subprograms. Using the given values of *p* and *h*, the program determines whether the state point to be calculated is located within the single phase region (liquid or superheated steam) or the wet steam region. When the given state point is located in the wet steam region, *x* will be calculated, otherwise the result is set to *x* = -1

Results for wrong input values

Result **x_ph_air = –1** or **XPHAIR = -1** for the following input values:

$p > p_{mcb}$ = 37.9195 bar or $p < p_{min,v}$ = 0.024316 bar

Reference:

[1]

Backward Function: Vapor Fraction *x* = f(*p*,*s*)

Function Name: **x_ps_air**
Subroutine with function value: **REAL*8 FUNCTION XPSAIR(P,S)**
Variable Types: REAL*8 P,S

Input values

P - Pressure *p* in bar
S - Specific entropy *s* in kJ/(kg·K)

Result

x_ps_air or **XPSAIR** – Vapor fraction *x* in (kg saturated steam)/(kg wet steam)

Range of validity

Temperature range: from -213.4 °C (59.75 K) to 1726.85 °C (2000 K)
Pressure range: from 0.00001 bar to 20000 bar

Details on the calculation of wet steam

The wet steam region is calculated automatically by the subprograms. Using the given values of *p* and *s*, the program determines whether the state point to be calculated is located within the single phase region (liquid or superheated steam) or the wet steam region. When the given state point is located in the wet steam region, *x* will be calculated, otherwise the result is set to *x* = -1

Results for wrong input values

Result **x_ps_air = –1** or **XPSAIR = -1** for the following input values:

$p > p_{mcb}$ = 37.9195 bar or $p < p_{min,v}$ = 0.024316 bar

Reference:

[1]

KCE ThermoFluidProperties

KCE-ThermoFluidProperties
www.thermofluidprop.com

Hochschule Zittau/Görlitz
UNIVERSITY OF APPLIED SCIENCES

Property Libraries for Calculating Heat Cycles, Boilers, Turbines and Refrigerators

Water and Steam

Library LibIF97

- Industrial Formulation IAPWS-IF97 (Revision 2007)
- Supplementary Standards IAPWS-IF97-S01, -S03rev, -S04, and -S05
- IAPWS Revised Advisory Note No. 3 on Thermo-dynamic Derivatives (2008)

Library LibIF97_META

- Industrial Formulation IAPWS-IF97 (Revision 2007) for metastable steam

Humid Combustion Gas Mixtures

Library LibHuGas

Model: Ideal mixture of the real fluids:

CO_2 - Span, Wagner H_2O - IAPWS-95
O_2 - Schmidt, Wagner N_2 - Span et al.
Ar - Tegeler et al.

and of the ideal gases:
SO_2, CO, Ne
(Scientific Formulation of Bücker et al.)

Consideration of:

- Dissociation from VDI 4670
- Poynting effect

Humid Air

Library LibHuAir

Model: Ideal mixture of the real fluids:

- Dry air from Lemmon et al.
- Steam, water and ice from IAPWS-IF97 and IAPWS-06

Consideration of:

- Condensation and freezing of steam
- Dissociation from VDI 4670
- Poynting effect from ASHRAE RP-1485

Extremely Fast Property Calculations

Spline-Based Table Look-up Method (SBTL)

Library LibSBTL_IF97
Library LibSBTL_95
Library LibSBTL_HuAir

For steam, water, humid air, carbon dioxide and other fluids and mixtures according IAPWS Guideline 2015 for Computational Fluid Dynamics (CFD), real-time and non-stationary simulations

Carbon Dioxide Including Dry Ice

Library LibCO2

Formulation of Span and Wagner (1996)

Seawater

Library LibSeaWa

IAPWS Industrial Formulation 2013

Ice

Library LibICE

Ice from IAPWS-06, Melting and sublimation pressures from IAPWS-08, Water from IAPWS-IF97, Steam from IAPWS-95 and -IF97

Ideal Gas Mixtures

Library LibIdGasMix

Model: Ideal mixture of the ideal gases:

Ar	NO	He	Propylene
Ne	H_2O	F_2	Propane
N_2	SO_2	NH_3	Iso-Butane
O_2	H_2	Methane	n-Butane
CO	H_2S	Ethane	Benzene
CO_2	OH	Ethylene	Methanol
Air			

Consideration of:

- Dissociation from the VDI Guideline 4670

Library LibIDGAS

Model: Ideal gas mixture from VDI Guideline 4670

Consideration of:

- Dissociation from the VDI Guideline 4670

Humid Air

Library ASHRAE LibHuAirProp

Model: Virial equation from ASHRAE Report RP-1485 for real mixture of the real fluids:
- Dry air
- Steam

Consideration of:

- Enhancement of the partial saturation pressure of water vapor at elevated total pressures

www.ashrae.org/bookstore

Dry Air Including Liquid Air

Library LibRealAir

Formulation of Lemmon et al. (2000)

Refrigerants

Ammonia

Library LibNH3

Formulation of Tillner-Roth et al. (1993)

R134a

Library LibR134a

Formulation of Tillner-Roth and Baehr (1994)

Iso-Butane

Library LibButane_Iso

Formulation of Bücker and Wagner (2006)

n-Butane

Library LibButane_n

Formulation of Bücker and Wagner (2006)

Mixtures for Absorption Processes

Ammonia/Water Mixtures

Library LibAmWa

IAPWS Guideline 2001 of Tillner-Roth and Friend (1998)

Helmholtz energy equation for the mixing term

(also useable for calculating the Kalina Cycle)

Water/Lithium Bromide Mixtures

Library LibWaLi

Formulation of Kim and Infante Ferreira (2004)

Gibbs energy equation for the mixing term

Liquid Coolants

Liquid Secondary Refrigerants

Library LibSecRef

Liquid solutions of water with

$C_2H_6O_2$	Ethylene glycol
$C_3H_8O_2$	Propylene glycol
C_2H_5OH	Ethanol
CH_3OH	Methanol
$C_3H_8O_3$	Glycerol
K_2CO_3	Potassium carbonate
$CaCl_2$	Calcium chloride
$MgCl_2$	Magnesium chloride
NaCl	Sodium chloride
$C_2H_3KO_2$	Potassium acetate
$CHKO_2$	Potassium formate
LiCl	Lithium chloride
NH_3	Ammonia

Formulation of the International Institute of Refrigeration (IIR 2010)

Ethanol

Library LibC2H5OH

Formulation of
Schroeder et al. (2014)

Methanol

Library LibCH3OH

Formulation of
de Reuck and Craven (1993)

Propane

Library LibPropane

Formulation of
Lemmon et al. (2009)

Siloxanes as ORC Working Fluids

Octamethylcyclotetrasiloxane $C_8H_{24}O_4Si_4$ **Library LibD4**

Decamethylcyclopentasiloxane $C_{10}H_{30}O_5Si_5$ **Library LibD5**

Tetradecamethylhexasiloxane $C_{14}H_{42}O_5Si_6$ **Library LibMD4M**

Hexamethyldisiloxane $C_6H_{18}OSi_2$ **Library LibMM**

Formulation of Colonna et al. (2006)

Dodecamethylcyclohexasiloxane $C_{12}H_{36}O_6Si_6$ **Library LibD6**

Decamethyltetrasiloxane $C_{10}H_{30}O_3Si_4$ **Library LibMD2M**

Dodecamethylpentasiloxane $C_{12}H_{36}O_4Si_5$ **Library LibMD3M**

Octamethyltrisiloxane $C_8H_{24}O_2Si_3$ **Library LibMDM**

Formulation of Colonna et al. (2008)

Nitrogen and Oxygen

Libraries LibN2 and LibO2

Formulations of Span et al. (2000)
and Schmidt and Wagner (1985)

Hydrogen

Library LibH2

Formulation of
Leachman et al. (2009)

Helium

Library LibHe

Formulation of
Arp et al. (1998)

Hydrocarbons

Decane $C_{10}H_{22}$ **Library LibC10H22**

Isopentane C_5H_{12} **Library LibC5H12_Iso**

Neopentane C_5H_{12} **Library LibC5H12_Neo**

Isohexane C_6H_{14} **Library LibC6H14**

Toluene C_7H_8 **Library LibC7H8**

Formulation of Lemmon and Span (2006)

Further Fluids

Carbon monoxide **CO** **Library LibCO**

Carbonyl sulfide **COS** **Library LibCOS**

Hydrogen sulfide H_2S **Library LibH2S**

Nitrous oxide N_2O **Library LibN2O**

Sulfur dioxide SO_2 **Library LibSO2**

Acetone C_3H_6O **Library LibC3H6O**

Formulation of Lemmon and Span (2006)

KCE ThermoFluidProperties

For more information please contact:

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01307 Dresden, Germany

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Mobile: +49-172-7914607
Fax: +49-3222-1095810

The following thermodynamic and transport properties can be calculated[a]:

Thermodynamic Properties

- Vapor pressure p_s
- Saturation temperature T_s
- Density ρ
- Specific volume v
- Enthalpy h
- Internal energy u
- Entropy s
- Exergy e
- Isobaric heat capacity c_p
- Isochoric heat capacity c_v
- Isentropic exponent κ
- Speed of sound w
- Surface tension σ

Transport Properties

- Dynamic viscosity η
- Kinematic viscosity ν
- Thermal conductivity λ
- Prandtl number Pr
- Thermal diffusivity a

Backward Functions

- T, v, s (p,h)
- T, v, h (p,s)
- p, T, v (h,s)
- p, T (v,h)
- p, T (v,u)

Thermodynamic Derivatives

- Partial derivatives used in process modeling can be calculated.

[a] Not all of these property functions are available in all property libraries.

www.thermofluidprop.com

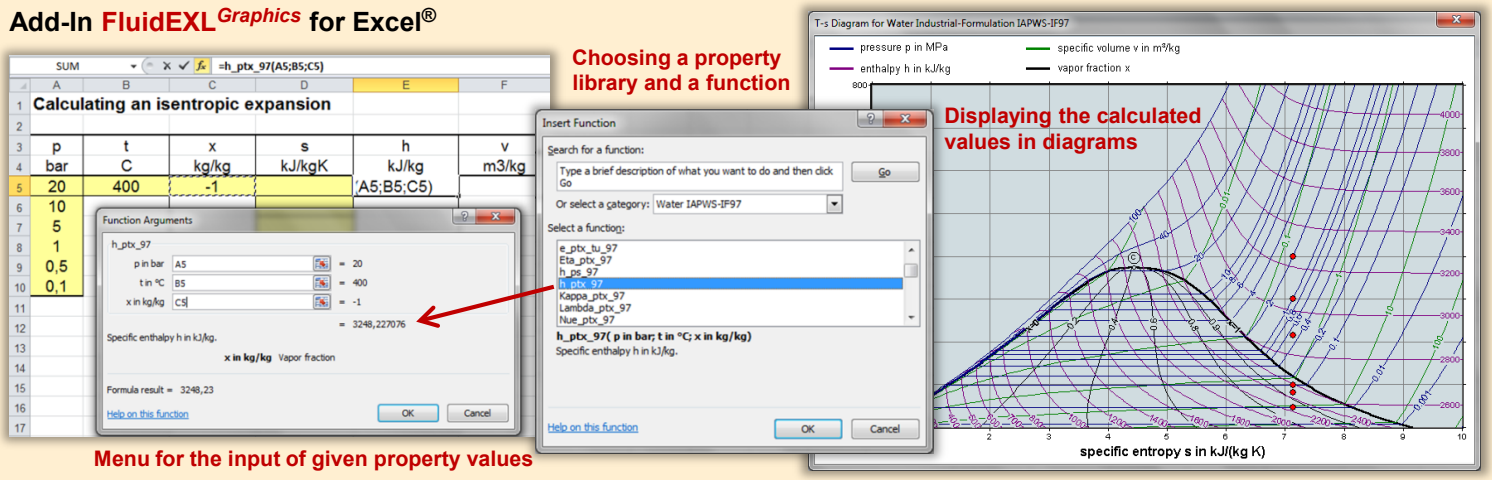
KCE-ThermoFluidProperties
www.thermofluidprop.com

KCE ThermoFluidProperties

Hochschule Zittau/Görlitz
UNIVERSITY OF APPLIED SCIENCES

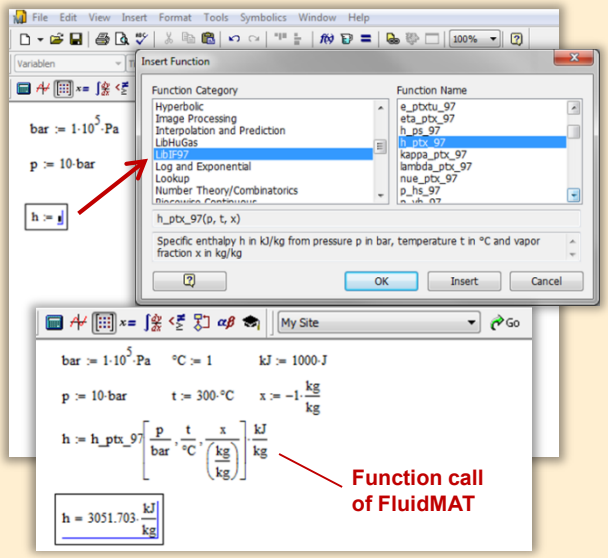
Property Software for Calculating Heat Cycles, Boilers, Turbines and Refrigerators

Add-In FluidEXL*Graphics* for Excel®



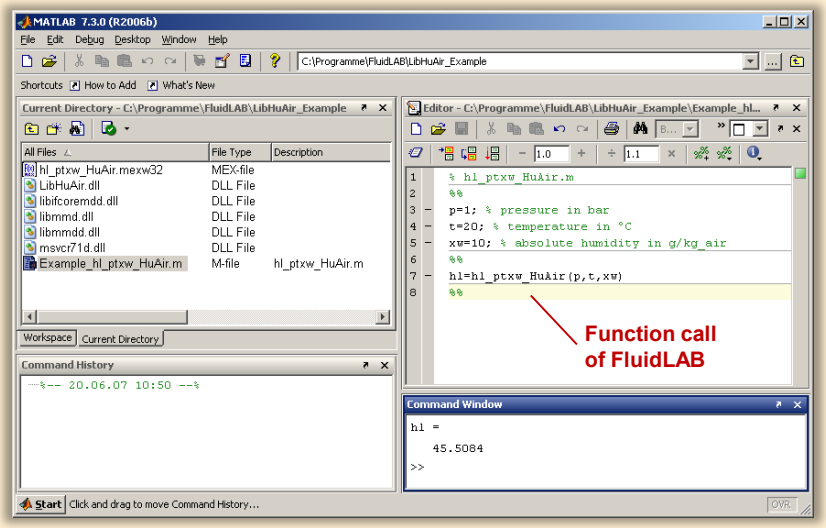
Add-On FluidMAT for Mathcad®
Add-On FluidPRIME for Mathcad Prime®

The property libraries can be used in Mathcad® and Mathcad Prime®.



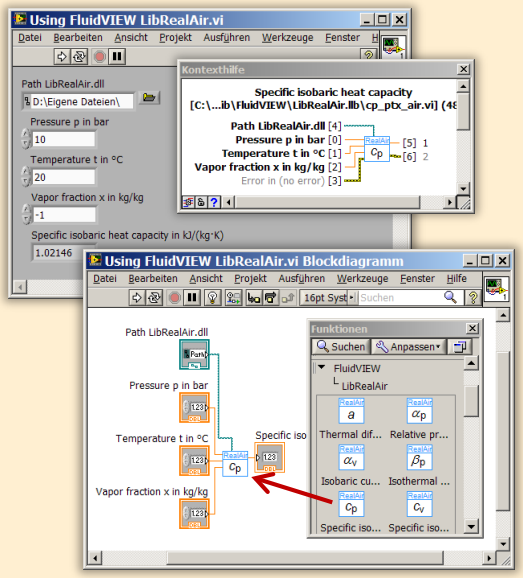
Add-On FluidLAB for MATLAB® and SIMULINK®

Using the Add-In FluidLAB the property functions can be called in MATLAB® and SIMULINK®.



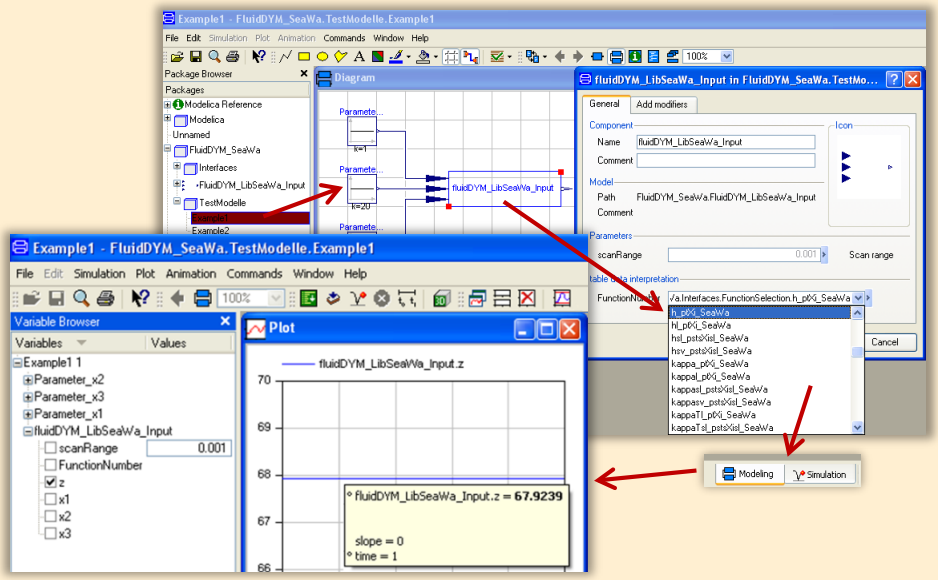
Add-On FluidVIEW for LabVIEW™

The property functions can be calculated in LabVIEW™.

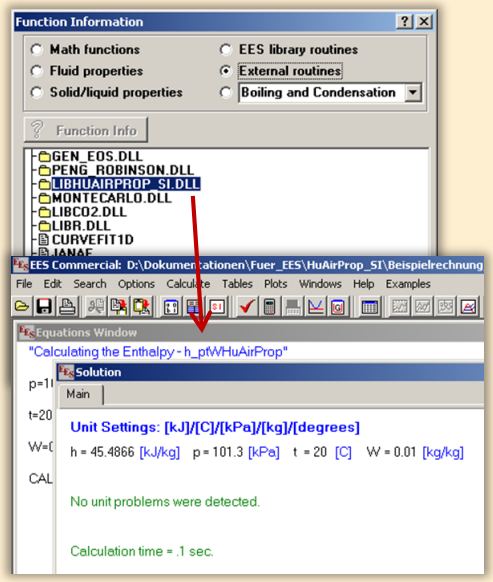


Add-On FluidDYM for DYMOLA® (Modelica) and SimulationX®

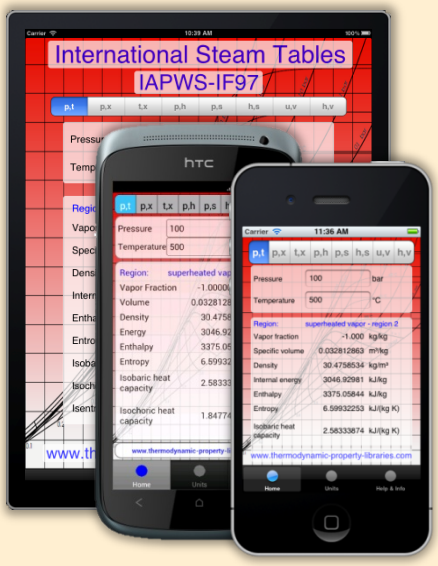
The property functions can be called in DYMOLA® and SimulationX®.



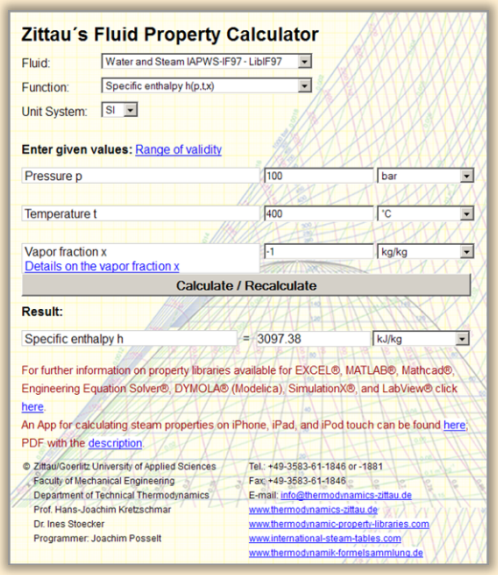
Add-On FluidEES for Engineering Equation Solver®



App International Steam Tables for iPhone, iPad, iPod touch, Android Smartphones and Tablets



Online Property Calculator at www.thermofluidprop.com



Property Software for Pocket Calculators

FluidCasio

fx 9750 G II | CFX 9850 fx-GG20 | CFX 9860 G Graph 85 | ALGEBRA FX 2.0

FluidHP

HP 48 | HP 49

FluidTI

TI Nspire CX CAS
TI Nspire CAS

TI 83
TI 84
TI 89

TI Voyage 200

TI 92

For more information please contact:

KCE ThermoFluidProperties

KCE-ThermoFluidProperties UG & Co. KG
Prof. Dr. Hans-Joachim Kretzschmar
Wallotstr. 3
01307 Dresden, Germany

Internet: www.thermofluidprop.com
Email: info@thermofluidprop.com
Phone: +49-351-27597860
Mobile: +49-172-7914607
Fax: +49-3222-1095810

The following thermodynamic and transport properties[a] can be calculated in Excel®, MATLAB®, Mathcad®, Engineering Equation Solver® (EES), DYMOLA® (Modelica), SimulationX® and LabVIEW™:

Thermodynamic Properties

- Vapor pressure p_s
- Saturation temperature T_s
- Density ρ
- Specific volume v
- Enthalpy h
- Internal energy u
- Entropy s
- Exergy e
- Isobaric heat capacity c_p
- Isochoric heat capacity c_v
- Isentropic exponent κ
- Speed of sound w
- Surface tension σ

Transport Properties

- Dynamic viscosity η
- Kinematic viscosity ν
- Thermal conductivity λ
- Prandtl number Pr
- Thermal diffusivity a

Backward Functions

- $T, v, s\ (p,h)$
- $T, v, h\ (p,s)$
- $p, T, v\ (h,s)$
- $p, T\ (v,h)$
- $p, T\ (v,u)$

Thermodynamic Derivatives

- Partial derivatives used in process modeling can be calculated.

[a] Not all of these property functions are available in all property libraries.

www.thermofluidprop.com

5. References

[1] Lemmon, E. W.; Jacobsen, R. T; Friend D. G.: *Thermodynamic Properties of Air and Mixtures of Nitrogen, Argon, and Oxygen From 60 to 2000 K at Pressures to 2000 MPa*. Journal of Physical and Chemical Reference Data, Volume 29, No. 3, 2000.

[2] Lemmon, E. W.; Jacobsen, R, T.: *Viscosity and Thermal Conductivity Equations for Nitrogen, Oxygen, Argon, and Air*. International Journal of Thermophysics, Volume 25, No. 1, 2004.

6. Satisfied Customers

Date: 07/2019

The following companies and institutions use the property libraries:

- FluidEXL*Graphics* for Excel®
- FluidLAB for MATLAB® and Simulink
- FluidMAT for Mathcad®
- FluidPRIME for Mathcad Prime®
- FluidEES for Engineering Equation Solver® EES
- FluidDYM for Dymola® (Modelica) and SimulationX®
- FluidVIEW for LabVIEW™
- DLLs for Windows™
- Shared Objects for Linux®.

2019

WARNICA, Waterloo, Canada	07/2019
MIBRAG, Zeitz	06/2019
Pöyry, Zürich, Switzerland	06/2019
RWTH Aachen, Inst. Strahlantriebe und Turbomaschinen	06/2019
Midiplan, Bietigheim-Bissingen	06/2019
GKS Schweinfurt	06/2019
HS Zittau/Görlitz, Wirtschaftswissenschaften und Wirtschaftsingenieurwesen	06/2019
ILK Dresden	06/2019
HZDR Helmholtz Zentrum Dresden-Rossendorf	06/2019
TH Köln, TGA	05/2019
IB Knittel, Braunschweig	05/2019
Norsk Energi, Oslo, Norway	05/2019
STEAG Essen	05/2019
Stora Enso, Eilenburg	05/2019
IB Lücke, Paderborn	05/2019
Haarslev, Sonderso, Denmark	05/2019
MAN Augsburg	05/2019
Wieland Werke, Ulm	04/2019
Fels-Werke, Elbingerode	04/2019
Univ. Luxembourg Luxembourg	04/2019
BTU Cottbus, Power Engineering	03/2009
Eins-Energie Sachsen, Schwarzenberg	03/2019
TU Dresden, Kälte- und Kryotechnik	03/2019
ITER, St. Paul Lez Durance Cedex, France	03/2019
Fraunhofer UMSICHT, Oberhausen	03/2019
Comparex Leipzig for Spedition Thiele HEMMERSBACH	03/2019
Rückert NaturGas, Lauf/Pegnitz	03/2019
BASF, Basel, Switzerland	02/2019
Stadtwerke Leipzig	02/2019

Maerz Ofenbau Zürich, Switzerland	02/2019
Hanon Systems Germany, Kerpen	02/2019
Thermofin, Heinsdorfergrund	01/2019
BSH Berlin	01/2019

2018

Jaguar Energy, Guatemala	12/2018
WEBASTO, Gilching	12/2018
Smurfit Kappa, Oosterhout, Netherlands	12/2018
Univ. BW München	12/2018
RAIV, Liberec for VALEO, Prague, Czech Republic	11/2018
VPC Group Vetschau	11/2018
SEITZ, Wetzikon, Switzerland	11/2018
MVV, Mannheim	10/2018
IB Troche	10/2018
KANIS Turbinen, Nürnberg	10/2018
TH Ingolstadt, Institut für neue Energiesysteme	10/2018
IB Kristl & Seibt, Graz, Austria	09/2018
INEOS, Köln	09/2018
IB Lücke, Paderborn	09/2018
Südzucker, Ochsenfurt	08/2018
K&K Turbinenservice, Bielefeld	07/2018
OTH Regensburg, Elektrotechnik	07/2018
Comparex Leipzig for LEAG, Berlin	06/2018
Münstermann, Telgte	05/2018
TH Nürnberg, Verfahrenstechnik	05/2018
Universität Madrid, Madrid, Spanien	05/2018
HS Zittau/Görlitz, Wirtschaftswissenschaften und Wirtschaftsingenieurwesen	05/2018
HS Niederrhein, Krefeld	05/2018
Wilhelm-Büchner HS, Pfungstadt	03/2018
GRS, Köln	03/2018
WIB, Dennheritz	03/2018
RONAL AG, Härklingen, Schweiz	02/2018
Ingenieurbüro Leipert, Riegelsberg	02/2018
AIXPROCESS, Aachen	02/2018
KRONES, Neutraubling	02/2018
Doosan Lentjes, Ratingen	01/2018

2017

Compact Kältetechnik, Dresden	12/2017
Endress + Hauser Messtechnik GmbH +Co. KG, Hannover	12/2017
TH Mittelhessen, Gießen	11/2017
Haarslev Industries, Søndersø, Denmark	11/2017
Hochschule Zittau/Görlitz, Fachgebiet Energiesystemtechnik	11/2017
ATESTEO, Alsdorf	10/2017
Wijbenga, PC Geldermalsen, Netherlands	10/2017
Fels-Werke GmbH, Elbingerode	10/2017

KIT Karlsruhe, Institute für Neutronenphysik und Reaktortechnik	09/2017
Air-Consult, Jena	09/2017
Papierfabrik Koehler, Oberkirch	09/2017
ZWILAG, Würenlingen, Switzerland	09/2017
TLK-Thermo Universität Braunschweig, Braunschweig	08/2017
Fichtner IT Consulting AG, Stuttgart	07/2017
Hochschule Ansbach, Ansbach	06/2017
RONAL, Härkingen, Switzerland	06/2017
BORSIG Service, Berlin	06/2017
BOGE Kompressoren, Bielefeld	06/2017
STEAG Energy Services, Zwingenberg	06/2017
CES clean energy solutions, Wien, Austria	04/2017
Princeton University, Princeton, USA	04/2017
B2P Bio-to-Power, Wadersloh	04/2017
TU Dresden, Institute for Energy Engineering, Dresden	04/2017
SAINT-GOBAIN, Vaujours, France	03/2017
TU Bergakademie Freiberg, Chair of Thermodynamics, Freiberg	03/2017
SCHMIDT + PARTNER, Therwil, Switzerland	03/2017
KAESER Kompressoren, Gera	03/2017
F&R, Praha, Czech Republic	03/2017
ULT Umwelt-Lufttechnik, Löbau	02/2017
JS Energie & Beratung, Erding	02/2017
Kelvion Brazed PHE, Nobitz-Wilchwitz	02/2017
MTU Aero Engines, München	02/2017
Hochschule Zittau/Görlitz, IPM	01/2017
CombTec ProCE, Zittau	01/2017
SHELL Deutschland Oil, Wesseling	01/2017
MARTEC Education Center, Frederikshaven, Denmark	01/2017
SynErgy Thermal Management, Krefeld	01/2017

2016

BOGE Druckluftsysteme, Bielefeld	12/2016
BFT Planung, Aachen	11/2016
Midiplan, Bietigheim-Bissingen	11/2016
BBE Barnich IB	11/2016
Wenisch IB,	11/2016
INL, Idaho Falls	11/2016
TU Kältetechnik, Dresden	11/2016
Kopf SynGas, Sulz	11/2016
INTVEN, Bellevne (USA)	11/2016
DREWAG Dresden, Dresden	10/2016
AGO AG Energie+Anlagen, Kulmbach	10/2016
Universität Stuttgart, ITW, Stuttgart	09/2016
Pöyry Deutschland GmbH, Dresden	09/2016
Siemens AG, Erlangen	09/2016
BASF über Fichtner IT Consulting AG	09/2016
B+B Engineering GmbH, Magdeburg	09/2016
Wilhelm Büchner Hochschule, Pfungstadt	08/2016

Webasto Thermo & Comfort SE, Gliching	08/2016
TU Dresden, Dresden	08/2016
Endress+Hauser Messtechnik GmbH+Co. KG, Hannover	08/2016
D + B Kältetechnik, Althausen	07/2016
Fichtner IT Consulting AG, Stuttgart	07/2016
AB Electrolux, Krakow, Poland	07/2016
ENEXIO Germany GmbH, Herne	07/2016
VPC GmbH, Vetschau/Spreewald	07/2016
INWAT, Lodz, Poland	07/2016
E.ON SE, Düsseldorf	07/2016
Planungsbüro Waidhas GmbH, Chemnitz	07/2016
EEB Enerko, Aldershoven	07/2016
IHEBA Naturenergie GmbH & Co. KG, Pfaffenhofen	07/2016
SSP Kälteplaner AG, Wolfertschwenden	07/2016
EEB ENERKO Energiewirtschaftliche Beratung GmbH, Berlin	07/2016
BOGE Kompressoren Otto BOGE GmbH & Co KG, Bielefeld	06/2016
Universidad Carlos III de Madrid, Madrid, Spain	04/2016
INWAT, Lodzi, Poland	04/2016
Planungsbüro WAIDHAS GmbH, Chemnitz	04/2016
STEAG Energy Services GmbH, Laszlo Küppers, Zwingenberg	03/2016
WULFF & UMAG Energy Solutions GmbH, Husum	03/2016
FH Bielefeld, Bielefeld	03/2016
EWT Eckert Wassertechnik GmbH, Celle	03/2016
ILK Institut für Luft- und Kältetechnik GmbH, Dresden	02/2016, 06/2016
IEV KEMA - DNV GV – Energie, Dresden	02/2016
Allborg University, Department of Energie, Aalborg, Denmark	02/2016
G.A.M. Heat GmbH, Gräfenhainichen	02/2016
Institut für Luft- und Kältetechnik, Dresden	02/2016, 05/2016, 06/2016
Bosch, Stuttgart	02/2016
INL Idaho National Laboratory, Idaho, USA	11/2016, 01/2016
Friedl ID, Wien, Austria	01/2016
Technical University of Dresden, Dresden	01/2016

2015

EES Enerko, Aachen	12/2015
Ruldolf IB, Strau, Austria	12/2015
Allborg University, Department of Energie, Aalborg, Denmark	12/2015
University of Lyubljana, Slovenia	12/2015
Steinbrecht IB, Berlin	11/2015
Universidad Carlos III de Madrid, Madrid, Spain	11/2015
STEAK, Essen	11/2015
Bosch, Lohmar	10/2015
Team Turbo Machines, Rouen, France	09/2015
BTC – Business Technology Consulting AG, Oldenburg	07/2015
KIT Karlsruhe Institute of Technology, Eggenstein-Leopoldshafen	07/2015
ILK, Dresden	07/2015
Schniewindt GmbH & Co. KG, Neuenwalde	08/2015

2014

PROJEKTPLAN, Dohna	04/2014
Technical University of Vienna, Austria	04/2014
MTU Aero Engines AG, Munich	04/2014
GKS, Schweinfurt	03/2014
Technical University of Nuremberg	03/2014
EP-E, Niederstetten	03/2014
Rückert NatUrgas GmbH, Lauf	03/2014
YESS-World, South Korea	03/2014
ZAB, Dessau	02/2014
KIT-TVT, Karlsruhe	02/2014
Stadtwerke Neuburg	02/2014
COMPAREX, Leipzig for RWE Essen	02/2014
Technical University of Prague, Czech Republic	02/2014
HS Augsburg	02/2014
Envi-con, Nuremberg	01/2014
DLR, Stuttgart	01/2014
Doosan Lentjes, Ratingen	01/2014
Technical University of Berlin	01/2014
Technical University of Munich	01/2014
Technical University of Braunschweig	01/2014
M&M Turbinentechnik, Bielefeld	01/2014

2013

TRANTER-GmbH, Artern	12/2013
SATAKE, Shanghai, China	12/2013
VOITH, Kunshan, China	12/2013
ULT, Löbau	12/2013
MAN, Copenhagen, Dänemark	11/2013
DREWAG, Dresden	11/2013
Haarslev Industries, Herlev, Dänemark	11/2013
STEAG, Herne	11/2013, 12/2013
Ingersoll-Rand, Oberhausen	11/2013
Wilhelm-Büchner HS, Darmstadt	10/2013
IAV, Chemnitz	10/2013
Technical University of Regensburg	10/2013
PD-Energy, Bitterfeld	09/2013
Thermofin, Heinsdorfergrund	09/2013
SHI, New Jersey, USA	09/2013
M&M Turbinentechnik, Bielefeld	08/2013
BEG-BHV, Bremerhaven	08/2013
TIG-Group, Husum	08/2013
COMPAREX, Leipzig for RWE Essen	08/2013, 11/2013 12/2013
University of Budapest, Hungary	08/2013
Siemens, Frankenthal	08/2013, 10/2013

	11/2013
VGB, Essen	07/2013, 11/2013
Brunner Energieberatung, Zurich, Switzerland	07/2013
Technical University of Deggendorf	07/2013
University of Maryland, USA	07/2013, 08/2013
University of Princeton, USA	07/2013
NIST, Boulder, USA	06/2013
IGUS GmbH, Dresden	06/2013
BHR Bilfinger, Essen	06/2013
SÜDSALZ, Bad Friedrichshall	06/2013, 12/2013
Technician School of Berlin	05/2013
KIER, Gajeong-ro, Südkorea	05/2013
Schwing/Stetter GmbH, Memmingen	05/2013
Vattenfall, Berlin	05/2013
AUTARK, Kleinmachnow	05/2013
STEAG, Zwingenberg	05/2013
Hochtief, Düsseldorf	05/2013
University of Stuttgart	04/2013
Technical University -Bundeswehr, Munich	04/2013
Rerum Cognitio Forschungszentrum, Frankfurt	04/2013
Kältetechnik Dresen + Bremen, Alfhausen	04/2013
University Auckland, New Zealand	04/2013
MASDAR Institut, Abu Dhabi, United Arab Emirates	03/2013
Simpelkamp, Dresden	02/2013
VEO, Eisenhüttenstadt	02/2013
ENTEC, Auerbach	02/2013
Caterpillar, Kiel	02/2013
Technical University of Wismar	02/2013
Technical University of Dusseldorf	02/2013
ILK, Dresden	01/2013, 08/2013
Fichtner IT, Stuttgart	01/2013, 11/2013
Schnepf Ingeniuerbüro, Nagold	01/2013
Schütz Engineering, Wadgassen	01/2013
Endress & Hauser, Reinach, Switzerland	01/2013
Oschatz GmbH, Essen	01/2013
frischli Milchwerke, Rehburg-Loccum	01/2013

2012

Voith, Bayreuth	12/2012
Technical University of Munich	12/2012
Dillinger Huette	12/2012
University of Stuttgart	11/2012
Siemens, Muehlheim	11/2012
Sennheiser, Hannover	11/2012
Oschatz GmbH, Essen	10/2012
Fichtner IT, Stuttgart	10/2012, 11/2012
Helbling Technik AG, Zurich, Switzerland	10/2012
University of Duisburg	10/2012

Rerum Cognitio Forschungszentrum, Frankfurt	09/2012
Pöyry Deutschland GmbH, Dresden	08/2012
Extracciones, Guatemala	08/2012
RWE, Essen	08/2012
Weghaus Consulting Engineers, Wuerzburg	08/2012
GKS, Schweinfurt	07/2012
COMPAREX, Leipzig for RWE Essen	07/2012
GEA, Nobitz	07/2012
Meyer Werft, Papenburg	07/2012
STEAG, Herne	07/2012
GRS, Cologne	06/2012
Fichtner IT Consult, Chennai, India	06/2012
Siemens, Freiburg	06/2012
Nikon Research of America, Belmont, USA	06/2012
Niederrhein University of Applied Sciences, Krefeld	06/2012
STEAG, Zwingenberg	06/2012
Mainova, Frankfurt on Main via Fichtner IT Consult	05/2012
Endress & Hauser	05/2012
PEU, Espenheim	05/2012
Luzern University of Applied Sciences, Switzerland	05/2012
BASF, Ludwigshafen (general license) via Fichtner IT Consult	05/2012
SPX Balcke-Dürr, Ratingen	05/2012, 07/2012
Gruber-Schmidt, Wien, Austria	04/2012
Vattenfall, Berlin	04/2012
ALSTOM, Baden	04/2012
SKW, Piesteritz	04/2012
TERA Ingegneria, Trento, Italy	04/2012
Siemens, Erlangen	04/2012, 05/2012
LAWI Power, Dresden	04/2012
Stadtwerke Leipzig	04/2012
SEITZ, Wetzikon, Switzerland	03/2012, 07/2012
M & M, Bielefeld	03/2012
Sennheiser, Wedemark	03/2012
SPG, Montreuil Cedex, France	02/2012
German Destilation, Sprendlingen	02/2012
Lopez, Munguia, Spain	02/2012
Endress & Hauser, Hannover	02/2012
Palo Alto Research Center, USA	02/2012
WIPAK, Walsrode	02/2012
Freudenberg, Weinheim	01/2012
Fichtner, Stuttgart	01/2012
airinotec, Bayreuth	01/2012, 07/2012
University Auckland, New Zealand	01/2012
VPC, Vetschau	01/2012
Franken Guss, Kitzingen	01/2012

2011

XRG-Simulation, Hamburg	12/2011
Smurfit Kappa PPT, AX Roermond, Netherlands	12/2011
AWTEC, Zurich, Switzerland	12/2011
eins-energie, Bad Elster	12/2011
BeNow, Rodenbach	11/2011
Luzern University of Applied Sciences, Switzerland	11/2011
GMVA, Oberhausen	11/2011
CCI, Karlsruhe	10/2011
W.-Büchner University of Applied Sciences, Pfungstadt	10/2011
PLANAIR, La Sagne, Switzerland	10/2011
LAWI, Dresden	10/2011
Lopez, Munguia, Spain	10/2011
University of KwaZulu-Natal, Westville, South Africa	10/2011
Voith, Heidenheim	09/2011
SpgBe Montreal, Canada	09/2011
SPG TECH, Montreuil Cedex, France	09/2011
Voith, Heidenheim-Mergelstetten	09/2011
MTU Aero Engines, Munich	08/2011
MIBRAG, Zeitz	08/2011
RWE, Essen	07/2011
Fels, Elingerode	07/2011
Weihenstephan University of Applied Sciences	07/2011, 09/2011 10/2011
Forschungszentrum Juelich	07/2011
RWTH Aachen University	07/2011, 08/2011
INNEO Solutions, Ellwangen	06/2011
Caliqua, Basel, Switzerland	06/2011
Technical University of Freiberg	06/2011
Fichtner IT Consulting, Stuttgart	05/2011, 06/2011, 08/2011
Salzgitter Flachstahl, Salzgitter	05/2011
Helbling Beratung & Bauplanung, Zurich, Switzerland	05/2011
INEOS, Cologne	04/2011
Enseleit Consulting Engineers, Siebigerode	04/2011
Witt Consulting Engineers, Stade	03/2011
Helbling, Zurich, Switzerland	03/2011
MAN Diesel, Copenhagen, Denmark	03/2011
AGO, Kulmbach	03/2011
University of Duisburg	03/2011, 06/2011
CCP, Marburg	03/2011
BASF, Ludwigshafen	02/2011
ALSTOM Power, Baden, Switzerland	02/2011
Universität der Bundeswehr, Munich	02/2011
Calorifer, Elgg, Switzerland	01/2011
STRABAG, Vienna, Austria	01/2011
TUEV Sued, Munich	01/2011

ILK Dresden	01/2011
Technical University of Dresden	01/2011, 05/2011 06/2011, 08/2011

2010

Umweltinstitut Neumarkt	12/2010
YIT Austria, Vienna, Austria	12/2010
MCI Innsbruck, Austria	12/2010
University of Stuttgart	12/2010
HS Cooler, Wittenburg	12/2010
Visteon, Novi Jicin, Czech Republic	12/2010
CompuWave, Brunntal	12/2010
Stadtwerke Leipzig	12/2010
MCI Innsbruck, Austria	12/2010
EVONIK Energy Services, Zwingenberg	12/2010
Caliqua, Basel, Switzerland	11/2010
Shanghai New Energy Resources Science & Technology, China	11/2010
Energieversorgung Halle	11/2010
Hochschule für Technik Stuttgart, University of Applied Sciences	11/2010
Steinmueller, Berlin	11/2010
Amberg-Weiden University of Applied Sciences	11/2010
AREVA NP, Erlangen	10/2010
MAN Diesel, Augsburg	10/2010
KRONES, Neutraubling	10/2010
Vaillant, Remscheid	10/2010
PC Ware, Leipzig	10/2010
Schubert Consulting Engineers, Weißenberg	10/2010
Fraunhofer Institut UMSICHT, Oberhausen	10/2010
Behringer Consulting Engineers, Tagmersheim	09/2010
Saacke, Bremen	09/2010
WEBASTO, Neubrandenburg	09/2010
Concordia University, Montreal, Canada	09/2010
Compañía Eléctrica de Sochagota, Bogota, Colombia	08/2010
Hannover University of Applied Sciences	08/2010
ERGION, Mannheim	07/2010
Fichtner IT Consulting, Stuttgart	07/2010
TF Design, Matieland, South Africa	07/2010
MCE, Berlin	07/2010, 12/2010
IPM, Zittau/Goerlitz University of Applied Sciences	06/2010
TUEV Sued, Dresden	06/2010
RWE IT, Essen	06/2010
Glen Dimplex, Kulmbach	05/2010, 07/2010 10/2010
Hot Rock, Karlsruhe	05/2010
Darmstadt University of Applied Sciences	05/2010
Voith, Heidenheim	04/2010
CombTec, Zittau	04/2010
University of Glasgow, Great Britain	04/2010

Universitaet der Bundeswehr, Munich	04/2010
Technical University of Hamburg-Harburg	04/2010
Vattenfall Europe, Berlin	04/2010
HUBER Consulting Engineers, Berching	04/2010
VER, Dresden	04/2010
CCP, Marburg	03/2010
Offenburg University of Applied Sciences	03/2010
Technical University of Berlin	03/2010
NIST Boulder CO, USA	03/2010
Technical University of Dresden	02/2010
Siemens Energy, Nuremberg	02/2010
Augsburg University of Applied Sciences	02/2010
ALSTOM Power, Baden, Switzerland	02/2010, 05/2010
MIT Massachusetts Institute of Technology Cambridge MA, USA	02/2010
Wieland Werke, Ulm	01/2010
Siemens Energy, Goerlitz	01/2010, 12/2010
Technical University of Freiberg	01/2010
ILK, Dresden	01/2010, 12/2010
Fischer-Uhrig Consulting Engineers, Berlin	01/2010

2009

ALSTOM Power, Baden, Schweiz	01/2009, 03/2009 05/2009
Nordostschweizerische Kraftwerke AG, Doettingen, Switzerland	02/2009
RWE, Neurath	02/2009
Brandenburg University of Technology, Cottbus	02/2009
Hamburg University of Applied Sciences	02/2009
Kehrein, Moers	03/2009
EPP Software, Marburg	03/2009
Bernd Münstermann, Telgte	03/2009
Suedzucker, Zeitz	03/2009
CPP, Marburg	03/2009
Gelsenkirchen University of Applied Sciences	04/2009
Regensburg University of Applied Sciences	05/2009
Gatley & Associates, Atlanta, USA	05/2009
BOSCH, Stuttgart	06/2009, 07/2009
Dr. Nickolay, Consulting Engineers, Gommersheim	06/2009
Ferrostal Power, Saarlouis	06/2009
BHR Bilfinger, Essen	06/2009
Intraserv, Wiesbaden	06/2009
Lausitz University of Applied Sciences, Senftenberg	06/2009
Nuernberg University of Applied Sciences	06/2009
Technical University of Berlin	06/2009
Fraunhofer Institut UMSICHT, Oberhausen	07/2009
Bischoff, Aurich	07/2009
Fichtner IT Consulting, Stuttgart	07/2009
Techsoft, Linz, Austria	08/2009
DLR, Stuttgart	08/2009

Wienstrom, Vienna, Austria	08/2009
RWTH Aachen University	09/2009
Vattenfall, Hamburg	10/2009
AIC, Chemnitz	10/2009
Midiplan, Bietigheim-Bissingen	11/2009
Institute of Air Handling and Refrigeration ILK, Dresden	11/2009
FZD, Rossendorf	11/2009
Techgroup, Ratingen	11/2009
Robert Sack, Heidelberg	11/2009
EC, Heidelberg	11/2009
MCI, Innsbruck, Austria	12/2009
Saacke, Bremen	12/2009
ENERKO, Aldenhoven	12/2009

2008

Pink, Langenwang	01/2008
Fischer-Uhrig, Berlin	01/2008
University of Karlsruhe	01/2008
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Lentjes, Ratingen	03/2008
Siemens Power Generation, Goerlitz	04/2008
Evonik, Zwingenberg (general EBSILON program license)	04/2008
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CFC Solutions, Munich	04/2008
RWE IT, Essen	04/2008
Rerum Cognitio, Zwickau	04/2008, 05/2008
ARUP, Berlin	05/2008
Research Center, Karlsruhe	07/2008
AWECO, Neukirch	07/2008
Technical University of Dresden, Professorship of Building Services	07/2008
Technical University of Cottbus, Chair in Power Plant Engineering	07/2008, 10/2008
Ingersoll-Rand, Unicov, Czech Republic	08/2008
Technip Benelux BV, Zoetermeer, Netherlands	08/2008
Fennovoima Oy, Helsinki, Finland	08/2008
Fichtner Consulting & IT, Stuttgart	09/2008
PEU, Espenhain	09/2008
Poyry, Dresden	09/2008
WINGAS, Kassel	09/2008
TUEV Sued, Dresden	10/2008
Technical University of Dresden, Professorship of Thermic Energy Machines and Plants	10/2008, 11/2008
AWTEC, Zurich, Switzerland	11/2008
Siemens Power Generation, Erlangen	12/2008

2007

Audi, Ingolstadt	02/2007
ANO Abfallbehandlung Nord, Bremen	02/2007
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Redacom, Nidau, Switzerland	02/2007
Universität der Bundeswehr, Munich	02/2007
Maxxtec, Sinsheim	03/2007
University of Rostock, Chair in Technical Thermodynamics	03/2007
AGO, Kulmbach	03/2007
University of Stuttgart, Chair in Aviation Propulsions	03/2007
Siemens Power Generation, Duisburg	03/2007
ENTHAL Haustechnik, Rees	05/2007
AWECO, Neukirch	05/2007
ALSTOM, Rugby, Great Britain	06/2007
SAAS, Possendorf	06/2007
Grenzebach BSH, Bad Hersfeld	06/2007
Reichel Engineering, Haan	06/2007
Technical University of Cottbus, Chair in Power Plant Engineering	06/2007
Voith Paper Air Systems, Bayreuth	06/2007
Egger Holzwerkstoffe, Wismar	06/2007
Tissue Europe Technologie, Mannheim	06/2007
Dometic, Siegen	07/2007
RWTH Aachen University, Institute for Electrophysics	09/2007
National Energy Technology Laboratory, Pittsburg, USA	10/2007
Energieversorgung Halle	10/2007
AL-KO, Jettingen	10/2007
Grenzebach BSH, Bad Hersfeld	10/2007
Wiesbaden University of Applied Sciences, Department of Engineering Sciences	10/2007
Endress+Hauser Messtechnik, Hannover	11/2007
Munich University of Applied Sciences, Department of Mechanical Engineering	11/2007
Rerum Cognitio, Zwickau	12/2007
Siemens Power Generation, Erlangen	11/2007
University of Rostock, Chair in Technical Thermodynamics	11/2007, 12/2007

2006

STORA ENSO Sachsen, Eilenburg	01/2006
Technical University of Munich, Chair in Energy Systems	01/2006
NUTEC Engineering, Bisikon, Switzerland	01/2006, 04/2006
Conwel eco, Bochov, Czech Republic	01/2006
Offenburg University of Applied Sciences	01/2006
KOCH Transporttechnik, Wadgassen	01/2006
BEG Bremerhavener Entsorgungsgesellschaft	02/2006
Deggendorf University of Applied Sciences, Department of Mechanical Engineering and Mechatronics	02/2006
University of Stuttgart,	02/2006

Department of Thermal Fluid Flow Engines	
Technical University of Munich,	02/2006
Chair in Apparatus and Plant Engineering	
Energietechnik Leipzig (company license),	02/2006
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RWE Power, Essen	03/2006
WAETAS, Pobershau	04/2006
Siemens Power Generation, Goerlitz	04/2006
Technical University of Braunschweig,	04/2006
Department of Thermodynamics	
EnviCon & Plant Engineering, Nuremberg	04/2006
Brassel Engineering, Dresden	05/2006
University of Halle-Merseburg,	05/2006
Department of USET Merseburg incorporated society	
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ThyssenKrupp Marine Systems, Kiel	07/2006
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Department of Mechanical Engineering	
Siemens Power Generation, Berlin	11/2006
Zikesch Armaturentechnik, Essen	11/2006
Wismar University of Applied Sciences, Seafaring Department	11/2006
BASF, Schwarzheide	12/2006
Enertech Energie und Technik, Radebeul	12/2006

2005

TUEV Nord, Hannover	01/2005
J.H.K Plant Engineering and Service, Bremerhaven	01/2005
Electrowatt-EKONO, Zurich, Switzerland	01/2005
FCIT, Stuttgart	01/2005
Energietechnik Leipzig (company license)	02/2005, 04/2005
	07/2005
eta Energieberatung, Pfaffenhofen	02/2005
FZR Forschungszentrum, Rossendorf/Dresden	04/2005
University of Saarbruecken	04/2005
Technical University of Dresden	04/2005
Professorship of Thermic Energy Machines and Plants	
Grenzebach BSH, Bad Hersfeld	04/2005
TUEV Nord, Hamburg	04/2005

Technical University of Dresden, Waste Management	05/2005
Siemens Power Generation, Goerlitz	05/2005
Duesseldorf University of Applied Sciences,	05/2005
Department of Mechanical Engineering and Process Engineering	
Redacom, Nidau, Switzerland	06/2005
Dumas Verfahrenstechnik, Hofheim	06/2005
Alensys Engineering, Erkner	07/2005
Stadtwerke Leipzig	07/2005
SaarEnergie, Saarbruecken	07/2005
ALSTOM ITC, Rugby, Great Britain	08/2005
Technical University of Cottbus, Chair in Power Plant Engineering	08/2005
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Technical University of Berlin	10/2005
Basel University of Applied Sciences,	10/2005
Department of Mechanical Engineering, Switzerland	
Midiplan, Bietigheim-Bissingen	11/2005
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Ulm University of Applied Sciences	03/2004
Visteon, Kerpen	03/2004, 10/2004
Technical University of Dresden,	
Professorship of Thermic Energy Machines and Plants	04/2004
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University of Saarbruecken	04/2004
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HEW-Kraftwerk, Tiefstack	06/2004
h s energieanlagen, Freising	07/2004
FCIT, Stuttgart	08/2004
Physikalisch Technische Bundesanstalt (PTB), Braunschweig	08/2004
Mainova Frankfurt	08/2004
Rietschle Energieplaner, Winterthur, Switzerland	08/2004
MAN Turbo Machines, Oberhausen	09/2004
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STEAG Kraftwerk, Herne	10/2004, 12/2004
University of Weimar	10/2004
energeticals (e-concept), Munich	11/2004
SorTech, Halle	11/2004

Enertech EUT, Radebeul (company license)	11/2004
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STORA ENSO Sachsen, Eilenburg	12/2004
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Freudenberg Service, Weinheim	12/2004

2003

Paper Factory, Utzenstorf, Switzerland	01/2003
MAB Plant Engineering, Vienna, Austria	01/2003
Wulff Energy Systems, Husum	01/2003
Technip Benelux BV, Zoetermeer, Netherlands	01/2003
ALSTOM Power, Baden, Switzerland	01/2003, 07/2003
VER, Dresden	02/2003
Rietschle Energieplaner, Winterthur, Switzerland	02/2003
DLR, Leupholdhausen	04/2003
Emden University of Applied Sciences, Department of Technology	05/2003
Petterssson+Ahrends, Ober-Moerlen	05/2003
SOFBID ,Zwingenberg (general EBSILON program license)	05/2003
Ingenieurbuero Ostendorf, Gummersbach	05/2003
TUEV Nord, Hamburg	06/2003
Muenstermann GmbH, Telgte-Westbevern	06/2003
University of Cali, Colombia	07/2003
Atlas-Stord, Rodovre, Denmark	08/2003
ENERKO, Aldenhoven	08/2003
STEAG RKB, Leuna	08/2003
eta Energieberatung, Pfaffenhofen	08/2003
exergie, Dresden	09/2003
AWTEC, Zurich, Switzerland	09/2003
Energie, Timelkam, Austria	09/2003
Electrowatt-EKONO, Zurich, Switzerland	09/2003
LG, Annaberg-Buchholz	10/2003
FZR Forschungszentrum, Rossendorf/Dresden	10/2003
EnviCon & Plant Engineering, Nuremberg	11/2003
Visteon, Kerpen	11/2003
VEO Vulkan Energiewirtschaft Oderbruecke, Eisenhuettenstadt	11/2003
Stadtwerke Hannover	11/2003
SaarEnergie, Saarbruecken	11/2003
Fraunhofer-Gesellschaft, Munich	12/2003
Erfurt University of Applied Sciences, Department of Supply Engineering	12/2003
SorTech, Freiburg	12/2003
Mainova, Frankfurt	12/2003
Energieversorgung Halle	12/2003

2002

Hamilton Medical AG, Rhaezuens, Switzerland	01/2002
Bochum University of Applied Sciences, Department of Thermo- and Fluid Dynamics	01/2002

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Stadtwerke Hannover	09/2002
Siemens Power Generation, Goerlitz	10/2002
Energieversorgung Halle (company license)	10/2002
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Dillinger Huette, Dillingen	11/2002
G.U.N.T. Geraetebau, Barsbuettel	12/2002
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VEAG, Berlin (group license)	12/2002

2001

ALSTOM Power, Baden, Switzerland	01/2001, 06/2001 12/2001
KW2 B. V., Amersfoot, Netherlands	01/2001, 11/2001
Eco Design, Saitamaken, Japan	01/2001
M&M Turbine Technology, Bielefeld	01/2001, 09/2001
MVV Energie, Mannheim	02/2001
Technical University of Dresden, Department of	02/2001
Power Machinery and Plants	
PREUSSAG NOELL, Wuerzburg	03/2001
Fichtner Consulting & IT Stuttgart	04/2001
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Muenstermann GmbH, Telgte-Westbevern	05/2001
SaarEnergie, Saarbruecken	05/2001
Siemens, Karlsruhe	08/2001
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Neusiedler AG, Ulmerfeld, Austria	09/2001
h s energieanlagen, Freising	09/2001
Electrowatt-EKONO, Zurich, Switzerland	09/2001
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SOFBID, Zwingenberg	01/2000
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AG KKK - PGW Turbo, Leipzig	01/2000
PREUSSAG NOELL, Wuerzburg	01/2000
M&M Turbine Technology, Bielefeld	01/2000
IBR Engineering Reis, Nittendorf-Undorf	02/2000
GK, Hannover	03/2000
KRUPP-UHDE, Dortmund (company license)	03/2000
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Thinius Engineering, Erkrath	04/2000
SaarEnergie, Saarbruecken	05/2000, 08/2000
DVO Data Processing Service, Oberhausen	05/2000
RWTH Aachen University	06/2000
VAUP Process Automation, Landau	08/2000
Knuerr-Lommatec, Lommatzsch	09/2000
AVACON, Helmstedt	10/2000
Compania Electrica, Bogota, Colombia	10/2000
G.U.N.T. Geraetebau, Barsbuettel	11/2000
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Bayernwerk, Munich	01/1999
DREWAG, Dresden (company license)	02/1999
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Regensburg University of Applied Sciences	04/1999
Fichtner Consulting & IT, Stuttgart	07/1999
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Technical University of Graz, Department of Thermal Engineering, Austria	11/1999
Ostendorf Engineering, Gummersbach	12/1999

1998

Technical University of Cottbus, Chair in Power Plant Engineering	05/1998
Fichtner Consulting & IT (CADIS information systems) Stuttgart	05/1998
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SCA Hygiene Products, Munich	10/1998
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Gerb, Dresden	06/1997
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