KCE
ThermoFluidProperties

Property Library for Propane

FluidVIEW with LibPropan for LabVIEW™

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Property Library of Ammonia-Water Mixtures
Including DLL and Add-on for LabVIEW™
FluidVIEW
LibPropan

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0 Package Contents

0.1 Zip files for 32-bit LabVIEW™

In order to install FluidVIEW on a computer running a 32-bit version of LabVIEW™ the zip file **CD_FluidVIEW_LibPropan.zip** is delivered. The directory structure of the archive is corresponding to the default directory of LabVIEW™.

The effects of the fifteen files, which are stored in the different directories of the zip archive, are shown in the Tables 0.1, 0.2, 0.3 and 0.4.

Table 0.1 Effects of the files located in the archive directory **CD_FluidVIEW_LibPropan\vi.lib \FluidVIEW\LibPropan**

Filename	Effects
LibPropan.llb	LabVIEW™ library file, containing every function of the LibPropan property library in the form of subprograms (SubVIs)

Table 0.2 Effects of the files located in the archive directory **CD_FluidVIEW_LibPropan\menus \Categories\FluidVIEW**

Filename	Effects
dir.mnu	The palette view of LabVIEW™ is based on the palette files (*.mnu). They include the palette data (e. g. the display name, the palette icon, the palette description, the help information, the synchronize information and the items)

Table 0.3 Effects of the files located in the archive directory **CD_FluidVIEW_LibPropan\source**

Filename	Effects
LibPropan.dll	Dynamic-link library containing the algorithms for the calculation of the property functions of carbon dioxide
advapi32.dll	Runtime library
Dformd.dll	Runtime library for the Fortran DLL
Dforrt.dll	Runtime library for the Fortran DLL
LC.dll	Auxiliary library
msvcp60.dll	Runtime library
msvcrt.dll	Runtime library

Table 0.4 Effects of the files located in the archive directory **CD_FluidVIEW_LibPropan\help \FluidVIEW-help**

Filename	Effects
FluidVIEW_LibPropan.pdf	User's guide of the property library LibPropan for the LabVIEW™ Add-On FluidVIEW
LibPropan.chm	Help file with descriptions for each function
OpenLibPropan_doc.vi	LabVIEW™ instrument to open the user's guide via the help menu
LibPropan.txt	Text file to change the name of the menu item of the help file
OpenLibPropan_doc.txt	Text file to change the name of the menu item of the file OpenLibPropan_doc.vi

0.2 Zip files for 64-bit LabVIEW™

In order to install FluidVIEW on a computer running a 64-bit version of LabVIEW™ the zip file **CD_FluidVIEW_LibPropan_x64.zip** is delivered. The directory structure of the archive is corresponding to the default directory of LabVIEW™.

The effects of the fifteen files, which are stored in the different directories of the zip archive, are shown in the Tables 0.5, 0.6, 0.7, 0.8 and 0.9.

Table 0.5 Effects of the files located in the archive directory **CD_FluidVIEW_LibPropan_x64\vi.lib \FluidVIEW\LibPropan**

Filename	Effects
LibPropan.llb	LabVIEW™ library file, containing every function of the LibPropan property library in the form of subprograms (SubVIs)

Table 0.6 Effects of the files located in the archive directory **CD_FluidVIEW_LibPropan_x64\menus \Categories\FluidVIEW**

Filename	Effects
dir.mnu	The palette view of LabVIEW™ is based on the palette files (*.mnu). They include the palette data (e. g. the display name, the palette icon, the palette description, the help information, the synchronize information and the items)

Table 0.7 Effects of the files located in the archive directory **CD_FluidVIEW_LibPropan_x64\source**

Filename	Effects
LibPropan.dll	Dynamic-link library containing the algorithms for the calculation of the property functions of carbon dioxide
Capt_ico_big.ico	Icon file
Libmmd.dll	Runtime library
Libifcoremd.dll	Runtime library
LC.dll	Auxiliary library
Libiomp5md.dll	Runtime library

Table 0.8 Effects of the files located in the archive directory **CD_FluidVIEW_LibPropan_x64\help \FluidVIEW-help**

Filename	Effects
FluidVIEW_LibPropan.pdf	User's guide of the LibPropan property library for the LabVIEW™ Add-On FluidVIEW
LibPropan.chm	Help file with descriptions for each function
OpenLibPropan_doc.vi	LabVIEW™ instrument to open the user's guide via the help menu
LibPropan.txt	Text file to change the name of the menu item of the help file
OpenLibPropan_doc.txt	Text file to change the name of the menu item of the file OpenLibPropan_doc.vi

Table 0.9 Effects of the files located in the archive directory **CD_FluidVIEW_LibPropan_x64 \vcredist_x64**

Filename	Effects
vcredist_x64.exe	Executable file to install the Microsoft Visual C++ 2008 Redistributable Package (x64). Within runtime components of Visual C++ Libraries required to run 64-bit applications developed with Visual C++ on a computer that does not have Visual C++ 2010 installed.

1. Property Functions

Functional Dependence	Function Name	Call from Fortran program	Call in DLL LibPropan as parameter	Property or Function	Unit of the result
$a = f(p,t,x)$	a_ptx_PROP	APTXPROP(P,T,X)	C_APTXPROP(A,P,T,X)	Thermal diffusivity	m^2/s
$c_p = f(p,t,x)$	cp_ptx_PROP	CPPTXPROP(P,T,X)	C_CPPTXPROP(CP,P,T,X)	Specific isobaric heat capacity	kJ/(kg K)
$\eta = f(p,t,x)$	eta_ptx_PROP	ETAPTXPROP(P,T,X)	C_ETAPTXPROP(ETA,P,T,X)	Dynamic viscosity	Pa s
$h = f(p,t,x)$	h_ptx_PROP	HPTXPROP(P,T,X)	C_HPTXPROP(H,P,T,X)	Specific enthalpy	kJ/kg
$\kappa = f(p,t,x)$	kappa_ptx_PROP	KAPTXPROP(P,T,X)	C_KAPTXPROP(KAP,P,T,X)	Isentropic exponent	-
$\lambda = f(p,t,x)$	lambda_ptx_PROP	LAMPTXPROP(P,T,X)	C_LAMPTXPROP(LAM,P,T,X)	Thermal conductivity	W/(m K)
$\nu = f(p,t,x)$	ny_ptx_PROP	NYPTXPROP(P,T,X)	C_NYPTXPROP(NY,P,T,X)	Kinematic viscosity	m^2/s
$p_{mel} = f(t)$	pmel_t_PROP	PMELPROP(T)	C_PMELPROP(PMEL,T)	Melting pressure from temperature	bar
$p_s = f(t)$	ps_t_PROP	PSTPROP(T)	C_PSTPROP(PS,T)	Vapor pressure from temperature	bar
$Pr = f(p,t,x)$	Pr_ptx_PROP	PRPTXPROP(P,T,X)	C_PRPTXPROP(PR,P,T,X)	*Prandtl*-Number	-
$\rho = f(p,t,x)$	rho_ptx_PROP	ROPTXPROP(P,T,X)	C_ROPTXPROP(RHO,P,T,X)	Density	kg/m^3
$s = f(p,t,x)$	s_ptx_PROP	SPTXPROP(P,T,X)	C_SPTXPROP(S,P,T,X)	Specific entropy	kJ/(kg K)
$t = f(p,h)$	t_ph_PROP	TPHPROP(P,H)	C_TPHPROP(T,P,H)	Backward function: Temperature from pressure and enthalpy	°C
$t = f(p,s)$	t_ps_PROP	TPSPROP(P,S)	C_TPSPROP(T,P,S)	Backward function: Temperature from pressure and entropy	°C
$t_{mel} = f(p)$	tmel_p_PROP	TMELPROP(P)	C_TMELPROP(TMEL,P)	Melting temperature from pressure	°C
$t_s = f(p)$	ts_p_PROP	TSPPROP(P)	C_TSPPROP(TS,P)	Saturation temperature from pressure	°C
$u = f(p,t,x)$	u_ptx_PROP	UPTXPROP(P,T,X)	C_UPTXPROP(U,P,T,X)	Specific internal energy	kJ/kg
$v = f(p,t,x)$	v_ptx_PROP	VPTXPROP(P,T,X)	C_VPTXPROP(V,P,T,X)	Specific volume	m^3/kg
$w = f(p,t,x)$	w_ptx_PROP	WPTXPROP(P,T,X)	C_WPTXPROP(W,P,T,X)	Isentropic speed of sound	m/s
$x = f(p,h)$	x_ph_PROP	XPHPROP(P,H)	C_XPHPROP(X,P,H)	Backward function: Vapor fraction from pressure and enthalpy	kg/kg
$x = f(p,s)$	x_ps_PROP	XPSPROP(P,S)	C_XPSPROP(X,P,S)	Backward function: Vapor fraction from pressure and entropy	kg/kg

Units: t in °C
p in bar
x in (kg of saturated steam)/(kg wet steam)

Range of validity

Temperature range: from $t_{mel}(p)$ to 326.85 °C
Pressure range: from $p_s(t_t) = 1.7517 \times 10^{-9}$ bar to 1000 bar

Reference state

h = 200 kJ/kg and s = 1 kJ/(kg K) at t = 0 °C on the boiling curve (x = 0)

Details on the vapor fraction *x*

The wet steam region is calculated automatically by the subprograms. For this purpose the following fixed details on the vapor fraction x are to be considered:

Single-phase region

If the state point to be calculated is located in the single-phase region (liquid or superheated steam) x = –1 must be entered as a pro-forma value.

Wet-steam region

If the state point to be calculated is located in the wet steam region, a value for x between 0 and 1 (x = 0 for saturated liquid, x = 1 for saturated steam) must be entered. In this case, the backward functions result in the appropriate value between 0 and 1 for x. When calculating wet steam either the given value for t and p = -1000 or the given value for p and t = -1000 and in both cases the value for x between 0 and 1 must be entered.

If p and t and x are entered as given values, the program considers p and t to be appropriate to represent the vapor pressure curve. If this is not the case the calculation for the property of the chosen function results in –1000.

Wet steam region: Temperature range from t_t = –187.625 °C to t_c = 96.74 °C
Pressure range from $p_s(t_t) = 1.7517 \times 10^{-9}$ bar to p_c = 42.512 bar

Note.

If the calculation results in –1000, the values entered represent a state point beyond the range of validity of LibPropan. For further information on each function and its range of validity see Chapter 3. The same information may also be accessed via the online help pages.

2 Application of FluidVIEW in LabVIEW™

The FluidVIEW Add-on has been developed to calculate thermodynamic properties in LabVIEW™ (version 10.0 or higher) more conveniently. Within LabVIEW™, it enables the direct call of functions relating to propane from the LibPropan property library.

2.1 Installing FluidVIEW

If a FluidVIEW property library has not yet been installed, please complete the initial installation procedure described below.

If a FluidVIEW property library has already been installed, you only need to copy several files which belong to the LibPropan library. In this case, follow the subsection "Adding the LibPropan Library" on page 2/3.

In both cases folders and files from the zip archive

CD_FluidVIEW_LibPropan.zip (for 32-bit version of Windows®)

CD_FluidVIEW_LibPropan_x64.zip (for 64-bit version of Windows®)

have to be copied into the default directory of the LabVIEW™ development environment. In the following text these zipped directories for the 32-bit or 64-bit operating system will be symbolised with the term **<CD>**.

You can see the current default directory of LabVIEW™ in the paths page (options dialog box). To display this page please select *Tools* and click on *Options* to open the options dialog box and then select *Paths* from the category list.

By choosing *Default Directory* from the drop-down list the absolute pathname to the default directory, where LabVIEW™ automatically stores information, is displayed. In the following sections the pathname of the default directory will be symbolised by the term **<LV>**.

Additional Requirement When Using the 64-bit Operating System

If you want to use FluidVIEW on a 64-bit computer that does not have Visual C++ installed, please make sure the Microsoft Visual C++ 2010 x64 Redistributable Package is installed.

If it is not the case, please install it by double clicking the file

vcredist_x64.exe

which you find in the folder **\vcredist_x64** in the **64-bit** CD folder "CD_FluidVIEW_LibPropan_x64."

In the following window you are required to accept the Microsoft® license terms to install the Microsoft Visual C++ 2010 runtime libraries by ticking the box next to "I have read and accept the license terms" (see Figure 2.1).

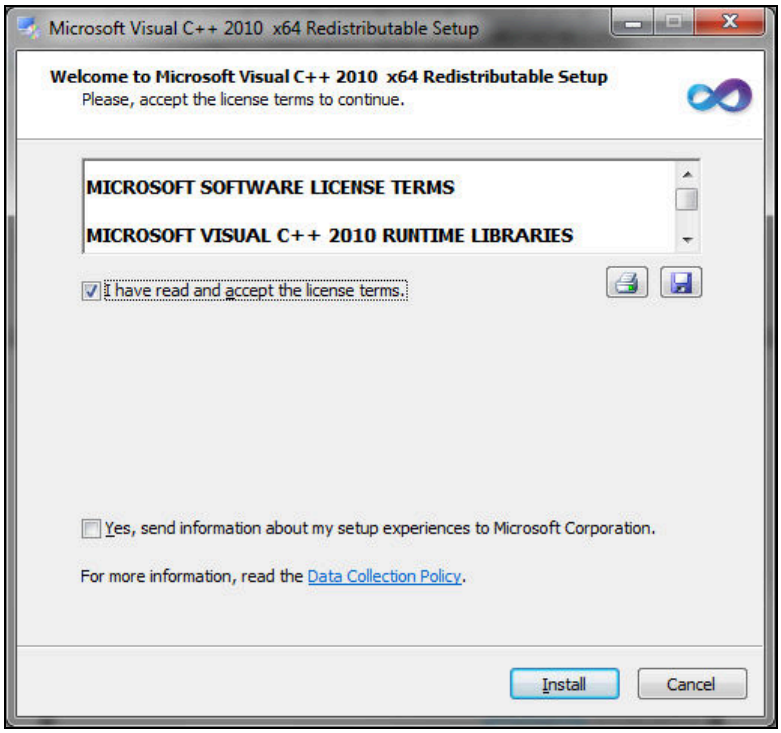


Figure 2.1 Accepting the license terms to install the Microsoft Visual C++ 2010 x64 Redistributable Package

Now click on "Install" to continue installation.

After the "Microsoft Visual C++ 2010 x64 Redistributable Pack" has been installed, you will see the sentence "Microsoft Visual C++ 2010 x64 Redistributable has been installed." Confirm this by clicking "Finish."

Now you can use the FluidVIEW Add-On on your 64-bit operating system. Please follow the instructions below to install FluidVIEW.

Initial Installation of FluidVIEW

The initial installation of FluidVIEW is carried out by copying three directories with its contents from the zip archive to the standard directory of LabVIEW™.

The directories that have to be copied, their paths in the zip archive and their target paths are listed in Table 2.1.

The installation is complete after copying the files and restarting LabVIEW™.

Due to the fact, that the functions of the DLL are called with a variable pathname, the source files you will find in the directory **<CD>\source** can be stored in a random directory on the harddisc. The pathname of LibHuAir.dll, which is located in this directory, has to be indicated in order to calculate the property functions (see example calculation in section 2.4 on page 2/9).

All source files have to be stored in the same directory to make the property functions of the LibPropan library work. These files are for the

- **32-bit system**: LibPropan.dll, advapi32.dll, Dformd.dll, Dforrt.dll, LC.dll, msvcp60.dll, and msvcrt.dll

and for the

- **64-bit system**: LibPropan.dll, capt_ico_big.ico, LC.dll, libifcoremd.dll, libiomp5md.dll, and libmmd.dll.

Table 2.1 Directories which have to be copied from the zip archive in the default directory of LabVIEW™ (<LV>) for the initial installation of FluidVIEW

Name of the directory	Parent directory in the zip archive	Target path in the default directory of LabVIEW (<LV>)
FluidVIEW	<CD>\vi.lib	<LV>\vi.lib
FluidVIEW	<CD>\menus\Categories	<LV>\menus\Categories
FluidVIEW-Help	<CD>\help	<LV>\help

Adding the LibPropan Library

In order to add the LibPropan property library to an existing FluidVIEW installation, one folder with its contents and five files have to be copied from the zip archive to the standard directory of LabVIEW™. This directory, the files plus their pathnames in the zip archive and their target paths are listed in Table 2.2.

The installation is complete after copying the files and restarting LabVIEW™.

Due to the fact, that the functions of the DLL are called with a variable pathname, the source files you will find in the directory **<CD>\source** can stored in a random directory on the harddisc. The pathname of LibHuAir.dll, which is located in this directory, has to be indicated in order to calculate the property functions (see example calculation in section 2.4 on page 2/9).

All source files have to be stored in the same directory to make the property functions of the LibPropan library work. These files are for the

- **32-bit system**: LibPropan.dll, advapi32.dll, Dformd.dll, Dforrt.dll, LC.dll, msvcp60.dll, and msvcrt.dll

and for the

- **64-bit system**: LibPropan.dll, capt_ico_big.ico, LC.dll, libifcoremd.dll, libiomp5md.dll, and libmmd.dll

Table 2.2 Data which have to be copied from the zip archive in the default directory of LabVIEW™ (<LV>) for adding the LibPropan property library to an existing installation of FluidVIEW

File name with file extension or name of the directory	Parent directory in the zip archive	Target path in the default directory of LabVIEW (<LV>)
LibPropan.llb	<CD>\vi.lib\FluidVIEW	<LV>\vi.lib\FluidVIEW
LibPropan	<CD>\menus\Categories \FluidVIEW	<LV>\menus\Categories \FluidVIEW
LibPropan.hlp	<CD>\\help\FluidVIEW-Help	<LV>\help\FluidVIEW-Help
LibPropan.txt	<CD>\\help\FluidVIEW-Help	<LV>\help\FluidVIEW-Help
FluidVIEW_LibPropan.pdf	<CD>\\help\FluidVIEW-Help	<LV>\help\FluidVIEW-Help
Open_LibPropan_doc.vi	<CD>\\help\FluidVIEW-Help	<LV>\help\FluidVIEW-Help
Open_LibPropan_doc.txt	<CD>\\help\FluidVIEW-Help	<LV>\help\FluidVIEW-Help

After you have restarted LabVIEW™ you will find the functions of the LibPropan property library in the functions palette under the sub palette FluidVIEW. An example calculation of the specific enthalpy *h* and the specific entropy *s* is shown in section 2.4.

2.2 The FluidVIEW Help System

FluidVIEW provides detailed online help functions.

General Information

The FluidVIEW Help System consists of the Microsoft WinHelp file **LibPropan.hlp** and this user's guide as PDF document **FluidVIEW_LibPropan_Docu_Eng.pdf**. Both files can be opened via the help menu. To do this please click *Help* in the menu bar. In the submenu *FluidVIEW-Help* you will find the commands *LibPropan Help File* and *LibPropan User's Guide* to open an appropriate file.

Context-Sensitive Help

If you have activated the context help function in LabVIEW™ (Ctrl-H) and move the cursor over a FluidVIEW object basic information is displayed in the context help window. The in- and output parameters plus a short information text are displayed for a property function. By clicking the **Detailed help** button in the **Context help** window the online help will be opened. The context help window of the function v_ptx_PROP.vi is shown in Figure 2.2.

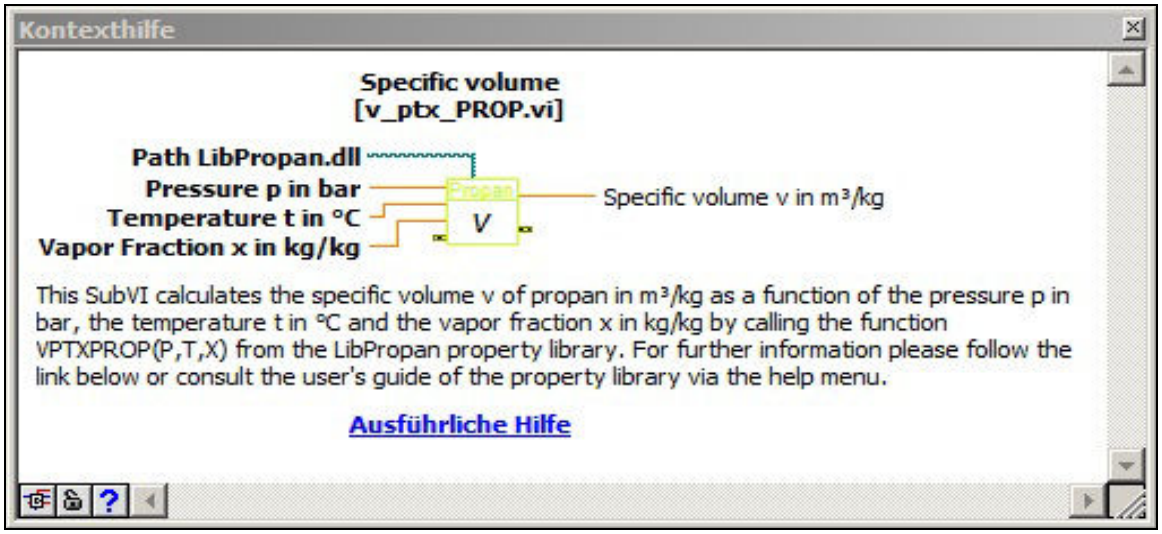


Figure 2.2 Context help window of the function v_ptx_PROP.vi

2.3 Licensing the LibPropan Property Library

The licensing procedure has to be carried out when calculating a LibPropan function and a FluidVIEW prompt message appears. In this case, you will see the "License Information" window (see figure below).

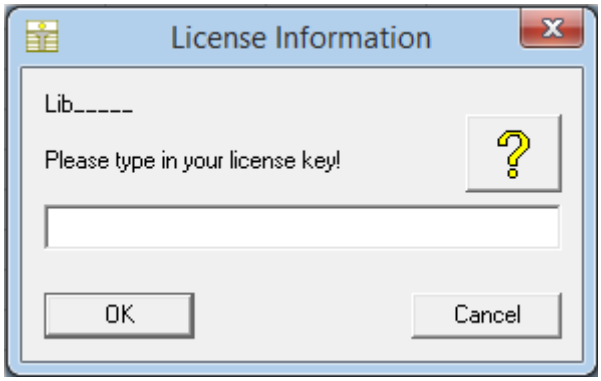


Figure 2.3 "License Information" window

Here you will have to type in the license key which you have obtained from the Zittau/Goerlitz University of Applied Sciences. You can find contact information on the "Content" page of this User's Guide or by clicking the yellow question mark in the "License Information" window. Then the following window will appear:

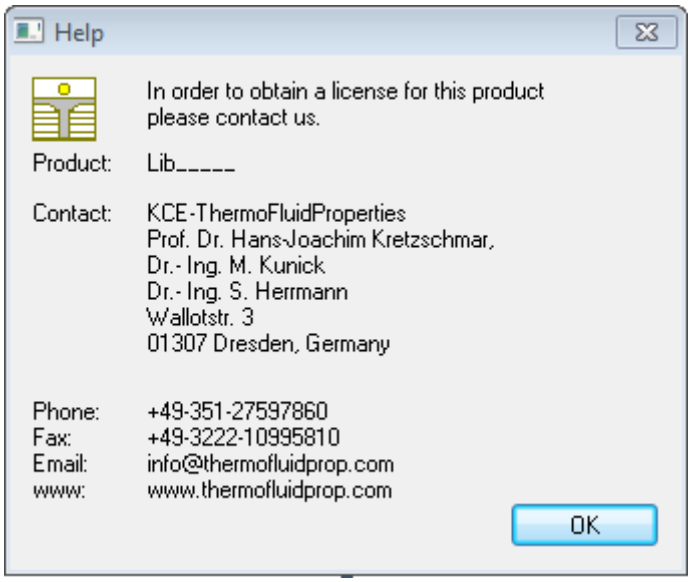


Figure 2.4 "Help" window

If you do not enter a valid license it is still possible to run your VI by clicking "Cancel". In this case, the LibPropan property library will display the result "-1.11111E+7" for every calculation.

The "License Information" window will appear every time you reopen your Virtual Instrument (VI) or reload the path of the LibPropan.dll. Should you not wish to license the LibPropan property library, you have to uninstall FluidVIEW according to the description in section 2.5 of this User's Guide.

Note:

The product name "Lib_ _ _ _ _ in the Figures above stands for the Library you are installing.

2.4 Example: Calculation of *h* = f(*p*,*t*,*x*) and *s* = f(*p*,*t*,*x*)

After the delivered files have been copied in the appropriate folders of the default directory LabVIEW™ (described in section 2.1), the LibPropan property library is ready to use. The function nodes of the LibPropan property library can be used by dragging them from the functions palette into the block diagram and connecting them with the wires representing the required input parameters.

Now we will calculate, step by step, the specific enthalpy *h* as a function of pressure *p*, temperature *t*, and vapor fraction *x*, using FluidVIEW.

- Start LabVIEW™ and wait for the *Getting Started* window to be displayed. Then select *Blank VI*. The *Blank VI* will be displayed in two windows, the front panel and the block diagram.
- Open the functions palette in the block diagram **via view / Functions Palette** (or by clicking the right mouse button anywhere in the free area of the block diagram) if not yet displayed.
- In addition to the default LabVIEW™ palettes the functions palette contains the sub palette *FluidVIEW* (see Figure 2.5) with the sub palette *LibPropan* (see Figure 2.6).

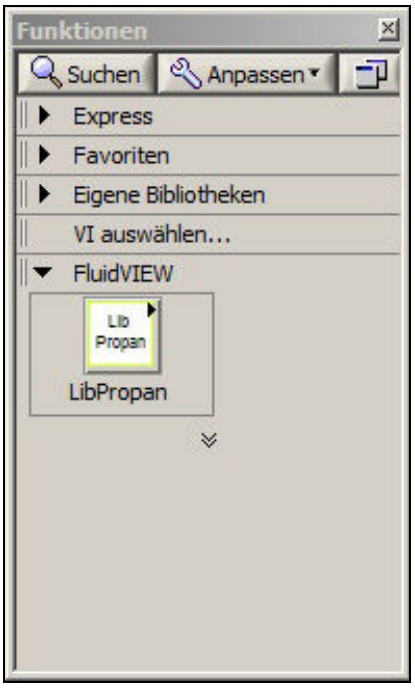


Figure 2.5
Functions palette with the sub palettes FluidVIEW and LibPropan

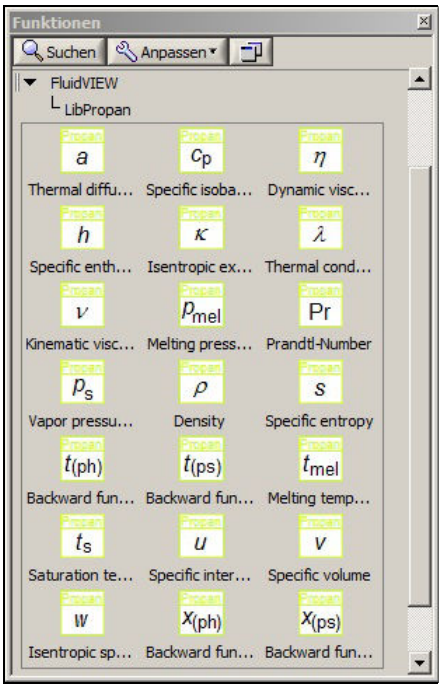


Figure 2.6
Functions palette with the property functions of the LibPropan library

In order to calculate the specific enthalpy *h*, drag the function (SubVI) whose symbol shows the *h* from the functions palette into the block diagram.
While the short names of the SubVIs behind the symbols will be shown in the control tip, the full names and brief descriptions of the property functions are displayed in the *Context Help* window (see Figure 2.2). To use the context help press <Ctrl>+<H> on your keyboard.

- After placing the node of the SubVI **h_ptx_PROP.vi** on your block diagram the required input parameters have to be defined.
  The input parameters which are set as required appear in bold type in the Context Help

window. In this case these input parameters are **Path LibPropan.dll** (LabVIEW™ data type: Path), **Pressure p in bar** (LabVIEW™ data type: Double precision, floating-point), **Temperature t in °C** (LabVIEW™ data type: Double precision, floating-point) and **Vapor fraction x in kg/kg** (LabVIEW™ data type: Double precision, floating-point).

- To define these variables wire their input terminals with input elements on the front panel. You can accomplish this in one step by choosing **Create / Control** in the context menu of all required input terminals. In order to wire the output terminal of the function node with an output element on the front panel, choose **Create / Indicator** in the context menu of the output terminal **Specific enthalpy h in kJ/kg** (LabVIEW™ data type: Double precision, floating-point). After cleaning up the block diagram by pressing <Ctrl>+<U> it has the appearance illustrated in Figure 2.7. The same input and output elements are available on the appropriate front panel (see Figure 2.8).

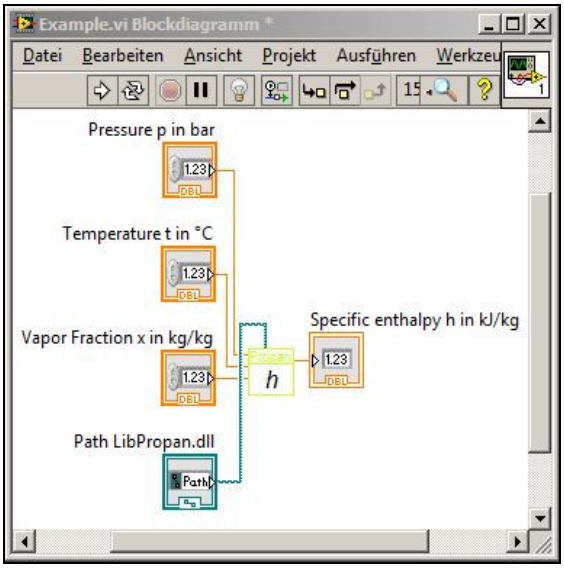


Figure 2.7
Block diagram of the example calculation

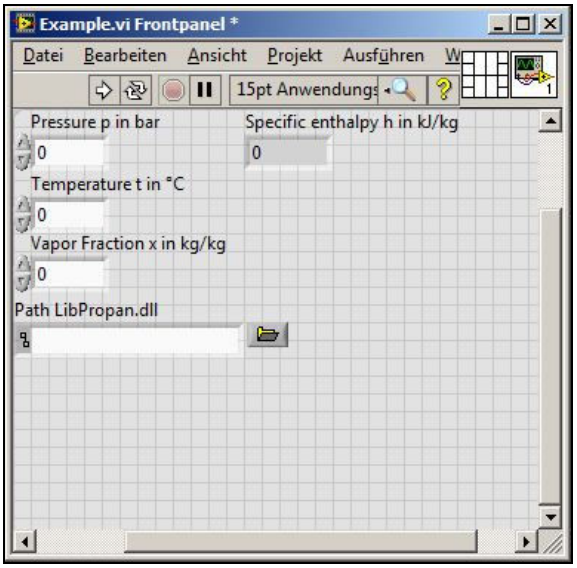


Figure 2.8
Front panel of the example calculation

- Enter a value in the input element *pressure p in bar* on the front panel
(Range of validity: from p_t = 1.43998 x 10^{-9} bar to 1000 bar)

  ⇒ e. g.: Enter the value 100.

- Enter a value in the input element *temperature t in °C* on the front panel
(Range of validity: $t = t_{mel}(p)$ … 326.85 °C)

  ⇒ e. g.: Enter the value 50.

- Enter a value in the input element *vapor fraction x in kg/kg* on the front panel.
Since the wet steam region is calculated automatically by the subprograms, the following fixed details on the vapor fraction *x* are to be considered when the value for x is entered:

  Single-phase region
  If the state point to be calculated is located in the single-phase region (liquid or superheated steam) x = –1 must be entered as a pro-forma value.

  Wet-steam region
  When calculating wet steam, a value between 0 and 1 (*x* = 0 for saturated liquid, *x* = 1 for saturated steam) must be entered. In this case, the backward functions result in the appropriate value between 0 and 1 for *x*. It is adequate to enter either the given value for *t* and *p* = –1, or the given value for *p* and *t* = –1, plus the value for *x* between 0 and 1.

When *p* and *t* and x are entered as given values, the program will consider *p* and *t* to be appropriate to represent the saturation-pressure curve. If it is not the case the calculation for the property of the chosen function to be calculated results in –1000.
(Vapor pressure curve of Propane: t_t = –187.625 °C ... t_c = 96.74 °C
$p_s(t_t)$ = 1.7517 x 10^{-9} bar … p_c = 42.512 bar)

⇒ e. g.: Enter the value -1.

- Enter the path of the LibPropan.dll in the input element *Path LibPropan.dll* on the front panel (as explained in section 2.1 the LibPropan.dll and the other library files from the directory **<CD>\source** have to be stored in the same directory which is arbitrary). To do this you can use the *File Open Dialog* which appears by clicking the yellow folder symbol on the right of the input element.
- To run the calculation of the specific enthalpy click on the *Run* button or press <Ctrl>+<R>. The result for *h* in kJ/kg appears in the output element (see Figure 2.9).

  ⇒ The result for *h* in our sample calculation is h = 333.549595 kJ/kg.

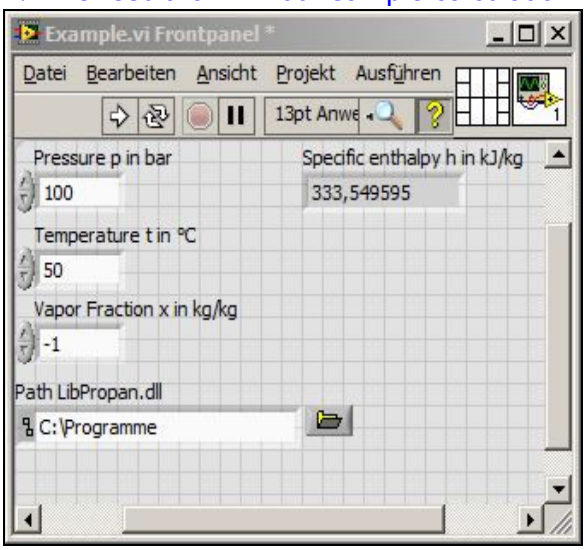


Figure 2.9 Result of the example calculation of *h*

The calculation of *h* = f(*p*,*t*,*x*) has thus been completed. Correspondingly, the specific entropy *s* = f(*p*,*t*,*x*) can be calculated with the same values for *p*, *t*, and *x*. The following changes need to be implemented.

- Open the context menu of the function node *specific enthalpy* on the block diagram. Under **Replace / Palette LibPropan** you will find the function **Specific entropy** symbolized with *s*. The node on the block diagram changes to **Specific entropy** by clicking on this symbol. Since the input parameters are the same as before their labels need not be changed. Only the label of the output parameter can be changed from *specific enthalpy h in kJ/kg* to *specific entropy s in kJ/(kg·K)* by double clicking on it and typing the new name.
- On the front panel you can see that the new label for the output element *specific entropy s in kJ/(kg·K)* was taken automatically. Since the values in the input elements are still present the calculation can be started now by pressing <Ctrl>+<R> or clicking the *Run* button. The result for *s* in kJ/(kg·K) appears in the output element.

  ⇒ The result for *s* in our sample calculation is 1.385218259 in kJ/(kg·K).

The calculation of *s* = f(*p*,*t*,*x*) has been carried out. You can now arbitrarily change the

values for *p*, *t*, or *x* in the appropriate input elements.
Note:
If the calculation results in –1000, this indicates that the values entered are located outside the range of validity. More detailed information on each function and its range of validity is available in chapter 3. For further property functions calculable with FluidVIEW, see the function table in chapter 1.

2.5 Removing FluidVIEW

Should you wish to remove the LibPropan library or the complete FluidVIEW Add-on you have to delete the files that have been copied in the default directory of the LabVIEW™ development environment **<LV>**.

Removing the FluidVIEW Add-on

To remove the FluidVIEW Add-on please delete the folders listed in Table 2.3 from the default directory of LabVIEW™.

Table 2.3 Directories that have to be deleted from the default directory of LabVIEW™ to remove the FluidVIEW Add-on

Name of the directory	Parent directory in the default directory of LabVIEW™ (<LV>)
FluidVIEW	<LV>\vi.lib
FluidVIEW	<LV>\menus\Categories
FluidVIEW-Help	<LV>\help

Removing only the LibPropan library

To remove only the LibPropan library please delete the folders or files listed in Table 2.4 from the default directory of LabVIEW™.

Table 2.4 Data that have to be deleted from the default directory of LabVIEW™ (<LV>) to remove only the LibPropan library.

File name with file extension or name of the directory	Parent directory in the default directory of LabVIEW (<LV>)
LibPropan.llb	<LV>\vi.lib\FluidVIEW
LibPropan	<LV>\menus\Categories\FluidVIEW
LibPropan.hlp	<LV>\help\FluidVIEW-Help
LibPropan.txt	<LV>\help\FluidVIEW-Help
FluidVIEW_LibPropan.pdf	<LV>\help\FluidVIEW-Help
Open_LibPropan_doc.vi	<LV>\help\FluidVIEW-Help
Open_LibPropan_doc.txt	<LV>\help\FluidVIEW-Help

The changes will take effect after restarting LabVIEW™.

3. Program Documentation

Thermal Diffusivity *a* = f(*p*,*t*,*x*)

Function Name:	**a_ptx_PROP**
Subroutine with function value: for call from Fortran	**REAL*8 FUNCTION APTXPROP(P,T,X)** REAL*8 P,T,X
Subroutine with parameter: for call from DLL	**INTEGER*4 FUNCTION C_APTXPROP(A,P,T,X)** REAL*8 A,P,T,X

Input Values:

P - Pressure *p* in bar

T - Temperature *t* in °C

X - Vapor fraction *x* (kg of saturated steam)/(kg wet steam)

Result

APTXPROP, **A** or **a_ptx_PROP** – Thermal diffusivity $a = \frac{\lambda * v}{c_p}$ in m^2 / s

Range of validity

Temperature range: from t_{mel} to 326.85 °C

Pressure range: from $p_s(t_t) = 1.7517 \cdot 10^{-9}$ bar to 1000 bar

Details on the vapor fraction *x* and on the calculation of saturated liquid and saturated steam

The wet steam region is calculated automatically by the subprograms. For this purpose the following fixed details on the vapor fraction *x* are to be considered:

If the state point to be calculated is located in the single-phase region (liquid or superheated steam) x = –1 must be entered as a pro-forma value.

If the state point to be calculated is located on the saturated liquid line, x = 0 must be entered. When calculating saturated steam (saturated vapor line) x = 1 must be entered.
The calculation for *x*-values between 0 and 1 is not possible.

When calculating saturated liquid or saturated steam, it is adequate to enter either the given value for *t* and p = -1000, or the given value for *p* and t = -1000, plus the value for *x* (x = 0 or x = 1). If *p* and *t* and *x* are entered as given values, the program will consider *p* and *t* to be appropriate to represent the vapor pressure curve.

Saturated liquid and saturated vapor line :

Temperature ranges from $t_t = -187.625$ °C to $t_c = 96.74$ °C

Pressure ranges from $p_s(t_t) = 1.7517 \cdot 10^{-9}$ bar to $p_c = 42.512$ bar

Results for wrong input values

Result **APTXPOP = -1000**, **A = -1000** or **a_ptx_PROP = -1000** for input values:

Single phase region:	$p > 1000$ bar or $p < p_s(t_t) = 1.7517 \cdot 10^{-9}$ bar or
(*x* = -1)	$t > 326.85$ °C or $t < t_{mel}$
Saturation lines:	at $p = -1000$ and $t > t_c = 96.74$ °C or $t < t_t = -187.625$ °C
	at $t = -1000$ and $p > p_c = 42.512$ bar or $p < p_s(t_t) = 1.7517 \cdot 10^{-9}$ bar or
	at $p > p_c = 42.512$ bar or $p < p_s(t_t) = 1.7517 \cdot 10^{-9}$ bar and $t > t_c = 96.74$ °C or $t < t_t = -187.625$ °C

References: [22], [25], [30]

Specific Isobaric Heat Capacity $c_p = f(p,t,x)$

Function Name:	**cp_ptx_PROP**
Subroutine with function value: for call from Fortran	**REAL*8 FUNCTION CPPTXPROP(P,T,X)** REAL*8 P,T,X
Subroutine with parameter: for call from DLL	**INTEGER*4 FUNCTION C_CPPTXPROP(CP,P,T,X)** REAL*8 CP,P,T,X

Input Values:

P - Pressure p in bar

T - Temperature t in °C

X - Vapor fraction x (kg of saturated steam)/(kg wet steam)

Result

CPPTXPROP, **CP** or **cp_ptx_PROP** – Specific isobaric heat capacity c_p in $kJ/(kg\,K)$

Range of validity

Temperature range: from t_{mel} to 326.85 °C

Pressure range: from $p_s(t_t) = 1.7517 \cdot 10^{-9}$ bar to 1000 bar

Details on the vapor fraction *x* and on the calculation of saturated liquid and saturated steam

The wet steam region is calculated automatically by the subprograms. For this purpose the following fixed details on the vapor fraction *x* are to be considered:

If the state point to be calculated is located in the single-phase region (liquid or superheated steam) x = –1 must be entered as a pro-forma value.

If the state point to be calculated is located on the saturated liquid line, x = 0 must be entered. When calculating saturated steam (saturated vapor line) x = 1 must be entered.
The calculation for *x*-values between 0 and 1 is not possible.

When calculating saturated liquid or saturated steam, it is adequate to enter either the given value for *t* and p = -1000, or the given value for *p* and t = -1000, plus the value for *x* (x = 0 or x = 1). If *p* and *t* and *x* are entered as given values, the program will consider *p* and *t* to be appropriate to represent the vapor pressure curve.

Saturated liquid and saturated vapor line:

Temperature ranges from $t_t = -187.625$ °C to $t_c = 96.74$ °C

Pressure ranges from $p_s(t_t) = 1.7517 \cdot 10^{-9}$ bar to $p_c = 42.512$ bar

Results for wrong input values

Result **CPPTXPROP = -1000**, **CP = -1000** or **cp_ptx_PROP = -1000** for input values:

Single phase region:	$p > 1000$ bar or $p < p_s(t_t) = 1.7517 \cdot 10^{-9}$ bar or
(x = -1)	$t > 326.85$ °C or $t < t_{mel}$
Saturation lines:	at $p = -1000$ and $t > t_c = 96.74$ °C or $t < t_t = -187.625$ °C
	at $t = -1000$ and $p > p_c = 42.512$ bar or $p < p_s(t_t) = 1.7517 \cdot 10^{-9}$ bar or
	at $p > p_c = 42.512$ bar or $p < p_s(t_t) = 1.7517 \cdot 10^{-9}$ bar and $t > t_c = 96.74$ °C or $t < t_t = -187.625$ °C

References: [22], [25]

Dynamic Viscosity $\eta = f(p,t,x)$

Function Name:	**eta_ptx_PROP**
Subroutine with function value:	**REAL*8 FUNCTION ETAPTXPROP(P,T,X)**
for call from Fortran	REAL*8 P,T,X
Subroutine with parameter:	**INTEGER*4 FUNCTION C_ETAPTXPROP(ETA,P,T,X)**
for call from DLL	REAL*8 ETA,P,T,X

Input Values:

P - Pressure *p* in bar

T - Temperature *t* in °C

X - Vapor fraction *x* (kg of saturated steam)/(kg wet steam)

Result

ETAPTXPROP, **ETA** or **eta_ptx_PROP** – Dynamic viscosity η in Pa s

Range of validity

Temperature range: from t_{mel} to 326.85 °C

Pressure range: from $p_s(t_t) = 1.7517 \cdot 10^{-9}$ bar to 1000 bar

Details on the vapor fraction *x* and on the calculation of saturated liquid and saturated steam

The wet steam region is calculated automatically by the subprograms. For this purpose the following fixed details on the vapor fraction *x* are to be considered:

If the state point to be calculated is located in the single-phase region (liquid or superheated steam) x = –1 must be entered as a pro-forma value.

If the state point to be calculated is located on the saturated liquid line, x = 0 must be entered. When calculating saturated steam (saturated vapor line) x = 1 must be entered.
The calculation for *x*-values between 0 and 1 is not possible.

When calculating saturated liquid or saturated steam, it is adequate to enter either the given value for *t* and p = -1000, or the given value for *p* and t = -1000, plus the value for *x* (x = 0 or x = 1). If *p* and *t* and *x* are entered as given values, the program will consider *p* and *t* to be appropriate to represent the vapor pressure curve.

Saturated liquid and saturated vapor line:

Temperature ranges from $t_t = -187.625$ °C to $t_c = 96.74$ °C

Pressure ranges from $p_s(t_t) = 1.7517 \cdot 10^{-9}$ bar to $p_c = 42.512$ bar

Results for wrong input values

Result **ETAPTXPROP = -1000**, **ETA = -1000** or **eta_ptx_PROP = -1000** for input values:

Single phase region:	$p > 1000$ bar or $p < p_s(t_t) = 1.7517 \cdot 10^{-9}$ bar or
(*x* = -1)	$t > 326.85$ °C or $t < t_{mel}$
Saturation lines:	at $p = -1000$ and $t > t_c = 96.74$ °C or $t < t_t = -187.625$ °C
	at $t = -1000$ and $p > p_c = 42.512$ bar or $p < p_s(t_t) = 1.7517 \cdot 10^{-9}$ bar or
	at $p > p_c = 42.512$ bar or $p < p_s(t_t) = 1.7517 \cdot 10^{-9}$ bar and $t > t_c = 96.74$ °C or $t < t_t = -187.625$ °C

References: [22], [25], [29]

Specific Enthalpy *h* = f(*p*,*t*,*x*)

Function Name:	**h_ptx_PROP**
Subroutine with function value:	**REAL*8 FUNCTION HPTXPROP(P,T,X)**
for call from Fortran	REAL*8 P,T,X
Subroutine with parameter:	**INTEGER*4 FUNCTION C_HPTXPROP(H,P,T,X)**
for call from DLL	REAL*8 H,P,T,X

Input Values:

P - Pressure *p* in bar

T - Temperature *t* in °C

X - Vapor fraction *x* (kg of saturated steam)/(kg wet steam)

Result

HPTXPROP, **H** or **h_ptx_PROP** - Specific enthalpy *h* in kJ/kg

Range of validity

Temperature range: from t_{mel} to 326.85 °C

Pressure range: from $p_s(t_t) = 1.7517 \cdot 10^{-9}$ bar to 1000 bar

Details on the vapor fraction *x* and on the calculation of wet steam

The wet steam region is calculated automatically by the subprograms. For this purpose the following fixed details on the vapor fraction *x* are to be considered:

If the state point to be calculated is located in the single-phase region (liquid or superheated steam) x = –1 must be entered as a pro-forma value.

If the state point to be calculated is located in the wet steam region, a value for *x* between 0 and 1 (x = 0 for saturated liquid, x = 1 for saturated steam) must be entered.

When calculating wet steam either the given value for *t* and p = -1000 or the given value for *p* and t = -1000 and in both cases the value for *x* between 0 and 1 must be entered.

If *p* and *t* and *x* are entered as given values, the program considers *p* and *t* to be appropriate to represent the vapor pressure curve.

Wet steam region: Temperature ranges from $t_t = -187.625$ °C °C to $t_c = 96.74$ °C

Pressure ranges from $p_s(t_t) = 1.7517 \cdot 10^{-9}$ bar to $p_c = 42.512$ bar

Results for wrong input values

Result **HPTXPROP = -1000**, **H = -1000** or **h_ptx_PROP = -1000** for input values:

Single phase region: $p > 1000$ bar or $p < p_s(t_t) = 1.7517 \cdot 10^{-9}$ bar or

(*x* = -1) $t > 326.85$ °C or $t < t_{mel}$

Wet steam region: at $p = -1000$ and $t > t_c = 96.74$ °C or $t < t_t = -187.625$ °C

at $t = -1000$ and $p > p_c = 42.512$ bar or $p < p_s(t_t) = 1.7517 \cdot 10^{-9}$ bar or

at $p > p_c = 42.512$ bar or $p < p_s(t_t) = 1.7517 \cdot 10^{-9}$ bar and

$t > t_c = 96.74$ °C or $t < t_t = -187.625$ °C

References: [22], [25]

Isentropic Exponent $\kappa = f(p,t,x)$

Function Name: **kappa_ptx_PROP**

Subroutine with function value: **REAL*8 FUNCTION KAPTXPROP(P,T,X)**
for call from Fortran REAL*8 P,T,X

Subroutine with parameter: **INTEGER*4 FUNCTION C_KAPTXPROP(KAP,P,T,X)**
for call from DLL REAL*8 KAP,P,T,X

Input Values:

P - Pressure *p* in bar

T - Temperature *t* in °C

X - Vapor fraction *x* (kg of saturated steam)/(kg wet steam)

Result

KAPTXPROP, **KAP** or **kappa_ptx_PROP** – Isentropic exponent $\kappa = \frac{w^2}{p \cdot v}$

Range of validity

Temperature range: from t_{mel} to 326.85 °C

Pressure range: from $p_s(t_t) = 1.7517 \cdot 10^{-9}$ bar to 1000 bar

Details on the vapor fraction *x* and on the calculation of saturated liquid and saturated steam

The wet steam region is calculated automatically by the subprograms. For this purpose the following fixed details on the vapor fraction *x* are to be considered:

If the state point to be calculated is located in the single-phase region (liquid or superheated steam) x = –1 must be entered as a pro-forma value.

If the state point to be calculated is located on the saturated liquid line, x = 0 must be entered. When calculating saturated steam (saturated vapor line) x = 1 must be entered.
The calculation for *x*-values between 0 and 1 is not possible.

When calculating saturated liquid or saturated steam, it is adequate to enter either the given value for *t* and p = -1000, or the given value for *p* and t = -1000, plus the value for *x* (x = 0 or x = 1). If *p* and *t* and *x* are entered as given values, the program will consider *p* and *t* to be appropriate to represent the vapor pressure curve.

Saturated liquid and saturated vapor line :

Temperature ranges from $t_t = -187.625$ °C to $t_c = 96.74$ °C

Pressure ranges from $p_s(t_t) = 1.7517 \cdot 10^{-9}$ bar to $p_c = 42.512$ bar

Results for wrong input values

Result **KAPTXPROP**, **KAP = -1000** or **kappa_ptx_PROP = -1000** for input values:

Single phase region: $p > 1000$ bar or $p < p_s(t_t) = 1.7517 \cdot 10^{-9}$ bar or
(*x* = -1) $t > 326.85$ °C or $t < t_{mel}$

Saturation lines: at $p = -1000$ and $t > t_c = 96.74$ °C or $t < t_t = -187.625$ °C

at $t = -1000$ and $p > p_c = 42.512$ bar or $p < p_s(t_t) = 1.7517 \cdot 10^{-9}$ bar or

at $p > p_c = 42.512$ bar or $p < p_s(t_t) = 1.7517 \cdot 10^{-9}$ bar and
$t > t_c = 96.74$ °C or $t < t_t = -187.625$ °C

References: [22], [25]

Thermal Conductivity $\lambda = f(p,t,x)$

Function Name: **lambda_ptx_PROP**

Subroutine with function value: **REAL*8 FUNCTION LAMPTXPROP(P,T,X)**
for call from Fortran REAL*8 P,T,X

Subroutine with parameter: **INTEGER*4 FUNCTION C_LAMPTXPROP(LAM,P,T,X)**
for call from DLL REAL*8 LAM,P,T,X

Input Values:

P - Pressure *p* in bar

T - Temperature *t* in °C

X - Vapor fraction *x* (kg of saturated steam)/(kg wet steam)

Result

LAMPTXPROP, **LAM** or **lambda_ptx_PROP** – Thermal conductivity λ in W / m K

Range of validity

Temperature range: from t_{mel} to 326.85 °C

Pressure range: from $p_s(t_t) = 1.7517 \cdot 10^{-9}$ bar to 1000 bar

Details on the vapor fraction *x* and on the calculation of saturated liquid and saturated steam

The wet steam region is calculated automatically by the subprograms. For this purpose the following fixed details on the vapor fraction *x* are to be considered:

If the state point to be calculated is located in the single-phase region (liquid or superheated steam) x = –1 must be entered as a pro-forma value.

If the state point to be calculated is located on the saturated liquid line, x = 0 must be entered. When calculating saturated steam (saturated vapor line) x = 1 must be entered.
The calculation for *x*-values between 0 and 1 is not possible.

When calculating saturated liquid or saturated steam, it is adequate to enter either the given value for *t* and p = -1000, or the given value for *p* and t = -1000, plus the value for *x* (x = 0 or x = 1). If *p* and *t* and *x* are entered as given values, the program will consider *p* and *t* to be appropriate to represent the vapor pressure curve.

Saturated liquid and saturated vapor line:

Temperature ranges from $t_t = -187.625$ °C to $t_c = 96.74$ °C

Pressure ranges from $p_s(t_t) = 1.7517 \cdot 10^{-9}$ bar to $p_c = 42.512$ bar

Results for wrong input values

Result **LAMPTXPROP = -1000**, **LAM = -1000** or **lambda_ptx_PROP = -1000** for input values:

Single phase region: $p > 1000$ bar or $p < p_s(t_t) = 1.7517 \cdot 10^{-9}$ bar or
(x = -1) $t > 326.85$ °C or $t < t_{mel}$

Saturation lines: at $p = -1000$ and $t > t_c = 96.74$ °C or $t < t_t = -187.625$ °C

at $t = -1000$ and $p > p_c = 42.512$ bar or $p < p_s(t_t) = 1.7517 \cdot 10^{-9}$ bar or

at $p > p_c = 42.512$ bar or $p < p_s(t_t) = 1.7517 \cdot 10^{-9}$ bar and
$t > t_c = 96.74$ °C or $t < t_t = -187.625$ °C

References: [22], [25], [30]

Kinematic Viscosity $\nu = f(p,t,x)$

Function Name: **ny_ptx_PROP**

Subroutine with function value: **REAL*8 FUNCTION NYPTXPROP(P,T,X)**
for call from Fortran REAL*8 P,T,X

Subroutine with parameter: **INTEGER*4 FUNCTION C_NYPTXPROP(NY,P,T,X)**
for call from DLL REAL*8 NY,P,T,X

Input Values:

P - Pressure *p* in bar

T - Temperature *t* in °C

X - Vapor fraction *x* (kg of saturated steam)/(kg wet steam)

Result

NYPTXPROP, **NY** or **ny_ptx_PROP** – Kinematic viscosity $\nu = \eta \cdot v$ in m² / s

Range of validity

Temperature range: from t_{mel} to 326.85 °C

Pressure range: from $p_s(t_t) = 1.7517 \cdot 10^{-9}$ bar to 1000 bar

Details on the vapor fraction *x* and on the calculation of saturated liquid and saturated steam

The wet steam region is calculated automatically by the subprograms. For this purpose the following fixed details on the vapor fraction *x* are to be considered:

If the state point to be calculated is located in the single-phase region (liquid or superheated steam) x = –1 must be entered as a pro-forma value.

If the state point to be calculated is located on the saturated liquid line, x = 0 must be entered. When calculating saturated steam (saturated vapor line) x = 1 must be entered.
The calculation for *x*-values between 0 and 1 is not possible.

When calculating saturated liquid or saturated steam, it is adequate to enter either the given value for *t* and p = -1000, or the given value for *p* and t = -1000, plus the value for *x* (x = 0 or x = 1). If *p* and *t* and *x* are entered as given values, the program will consider *p* and *t* to be appropriate to represent the vapor pressure curve.

Saturated liquid and saturated vapor line:

Temperature ranges from $t_t = -187.625$ °C to $t_c = 96.74$ °C

Pressure ranges from $p_s(t_t) = 1.7517 \cdot 10^{-9}$ bar to $p_c = 42.512$ bar

Results for wrong input values

Result **NYPTXPROP = -1000**, **NY = -1000** or **ny_ptx_PROP = -1000** for input values:

Single phase region: $p > 1000$ bar or $p < p_s(t_t) = 1.7517 \cdot 10^{-9}$ bar or
(*x* = -1) $t > 326.85$ °C or $t < t_{mel}$

Saturation lines: at $p = -1000$ and $t > t_c = 96.74$ °C or $t < t_t = -187.625$ °C

at $t = -1000$ and $p > p_c = 42.512$ bar or $p < p_s(t_t) = 1.7517 \cdot 10^{-9}$ bar or

at $p > p_c = 42.512$ bar or $p < p_s(t_t) = 1.7517 \cdot 10^{-9}$ bar and
$t > t_c = 96.74$ °C or $t < t_t = -187.625$ °C

References: [22], [25], [29]

Melting Pressure $p_{mel} = f(t)$

Function Name:	**pmel_t_PROP**
Subroutine with function value: for call from Fortran	**REAL*8 FUNCTION PMELPROP(T)** REAL*8 T
Subroutine with parameter: for call from DLL	**INTEGER*4 FUNCTION C_PMELPROP(PMEL,T)** REAL*8 PMEL,P,T,X

Input Values:

T - Temperature *t* in °C

Result

PMELTPROP, **PMEL** or **pmel_t_ PROP** – Melting pressure p_{mel} in bar

Range of validity

Temperature range: from $t_t = -187.625$°C to -178.537 °C

Results for wrong input values

Result **PMELTPROP = -1000**, **PMEL = -1000** or **pmel_t_PROP = -1000** for input values:

$t < t_t = -187.625$°C or $t >$ -178.537 °C

References: [28], [25]

Prandtl-Number *Pr* = f(*p*,*t*,*x*)

Function Name: **Pr_ptx_PROP**

Subroutine with function value: **REAL*8 FUNCTION PRPTXPROP(P,T,X)**
for call from Fortran REAL*8 P,T,X

Subroutine with parameter: **INTEGER*4 FUNCTION C_PRPTXPROP(PR,P,T,X)**
for call from DLL REAL*8 PR,P,T,X

Input Values:

P - Pressure *p* in bar

T - Temperature *t* in °C

X - Vapor fraction *x* (kg of saturated steam)/(kg wet steam)

Result

PRPTXPROP, **PR** or **Pr_ptx_PROP** – Prandtl-Number $Pr = \frac{\eta * c_p}{\lambda}$

Range of validity

Temperature range: from t_{mel} to 326.85 °C

Pressure range: from $p_s(t_t) = 1.7517 \cdot 10^{-9}$ bar to 1000 bar

Details on the vapor fraction *x* and on the calculation of saturated liquid and saturated steam

The wet steam region is calculated automatically by the subprograms. For this purpose the following fixed details on the vapor fraction *x* are to be considered:

If the state point to be calculated is located in the single-phase region (liquid or superheated steam) x = –1 must be entered as a pro-forma value.

If the state point to be calculated is located on the saturated liquid line, x = 0 must be entered. When calculating saturated steam (saturated vapor line) x = 1 must be entered.
The calculation for *x*-values between 0 and 1 is not possible.

When calculating saturated liquid or saturated steam, it is adequate to enter either the given value for *t* and p = -1, or the given value for *p* and t = -1, plus the value for *x* (x = 0 or x = 1). If *p* and *t* and *x* are entered as given values, the program will consider *p* and *t* to be appropriate to represent the vapor pressure curve.

Saturated liquid and saturated vapor line:

Temperature ranges from $t_t = -187.625$ °C to $t_c = 96.74$ °C

Pressure ranges from $p_s(t_t) = 1.7517 \cdot 10^{-9}$ bar to $p_c = 42.512$ bar

Results for wrong input values

Result **PRPTXPROP = -1000**, **PR = -1000** or **Pr_ptx_PROP = -1000** for input values:

Single phase region: $p > 1000$ bar or $p < p_s(t_t) = 1.7517 \cdot 10^{-9}$ bar or
(*x* = -1) $t > 326.85$ °C or $t < t_{mel}$

Saturation lines: at $p = -1000$ and $t > t_c = 96.74$ °C or $t < t_t = -187.625$ °C

at $t = -1000$ and $p > p_c = 42.512$ bar or $p < p_s(t_t) = 1.7517 \cdot 10^{-9}$ bar or

at $p > p_c = 42.512$ bar or $p < p_s(t_t) = 1.7517 \cdot 10^{-9}$ bar and
$t > t_c = 96.74$ °C or $t < t_t = -187.625$ °C

References: [22], [25], [29], [30]

Vapor Pressure $p_s = f(t)$

Function Name:	**ps_t_PROP**
Subroutine with function value: for call from Fortran	**REAL*8 FUNCTION PSTPROP(T)** REAL*8 T
Subroutine with parameter: for call from DLL	**INTEGER*4 FUNCTION C_PSTPROP(PS,T)** REAL*8 PS,T

Input Values:

T - Temperature t in °C

Result

PSTPROP, **PS** or **ps_t_PROP** – Vapor pressure p_s in bar

Range of validity

Temperature range: from $t_t = -187.625$°C to $t_c = 96.74$°C

Results for wrong input values

Result **PSTPROP = -1000**, **PS = -1000** or **ps_t_PROP = -1000** for input values:

$t < t_t = -187.625$°C or $t > t_c = 96.74$°C

References: [22], [25]

Density $\rho = f(p,t,x)$

Function Name:	**rho_ptx_PROP**
Subroutine with function value: for call from Fortran	**REAL*8 FUNCTION ROPTXPROP(P,T,X)** REAL*8 P,T,X
Subroutine with parameter: for call from DLL	**INTEGER*4 FUNCTION C_ROPTXPROP(RHO,P,T,X)** REAL*8 RHO,P,T,X

Input Values:

P - Pressure *p* in bar

T - Temperature *t* in °C

X - Vapor fraction *x* (kg of saturated steam)/(kg wet steam)

Result

RHOPTXPROP, **RHO** or **rho_ptx_PROP** – Density ρ in kg / m^3

Range of validity

Temperature range: from t_{mel} to 326.85 °C

Pressure range: from $p_s(t_t) = 1.7517 \cdot 10^{-9}$ bar to 1000 bar

Details on the vapor fraction *x* and on the calculation of wet steam

The wet steam region is calculated automatically by the subprograms. For this purpose the following fixed details on the vapor fraction *x* are to be considered:

If the state point to be calculated is located in the single-phase region (liquid or superheated steam) x = –1 must be entered as a pro-forma value.

If the state point to be calculated is located in the wet steam region, a value for *x* between 0 and 1 (x = 0 for saturated liquid, x = 1 for saturated steam) must be entered.

When calculating wet steam either the given value for *t* and p = -1 or the given value for *p* and t = -1 and in both cases the value for *x* between 0 and 1 must be entered.

If *p* and *t* and *x* are entered as given values, the program considers *p* and *t* to be appropriate to represent the vapor pressure curve.

Wet steam region: Temperature ranges from $t_t = -187.625$ °C to $t_c = 96.74$ °C

Pressure ranges from $p_s(t_t) = 1.7517 \cdot 10^{-9}$ bar to $p_c = 42.512$ bar

Results for wrong input values

Result **RHOPTXPROP = -1000**, **RHO = -1000** or **rho_ptx_PROP = -1000** for input values:

Single phase region: $p > 1000$ bar or $p < p_s(t_t) = 1.7517 \cdot 10^{-9}$ bar or

(*x* = -1) $t > 326.85$ °C or $t < t_{mel}$

Wet steam region: at $p = -1000$ and $t > t_c = 96.74$ °C or $t < t_t = -187.625$ °C

at $t = -1000$ and $p > p_c = 42.512$ bar or $p < p_s(t_t) = 1.7517 \cdot 10^{-9}$ bar or

at $p > p_c = 42.512$ bar or $p < p_s(t_t) = 1.7517 \cdot 10^{-9}$ bar and

$t > t_c = 96.74$ °C or $t < t_t = -187.625$ °C

References: [22], [25]

Specific Entropy *s* = f(*p*,*t*,*x*)

Function Name:	**s_ptx_PROP**
Subroutine with function value: for call from Fortran	**REAL*8 FUNCTION SPTXPROP(P,T,X)** REAL*8 P,T,X
Subroutine with parameter: for call from DLL	**INTEGER*4 FUNCTION C_SPTXPROP(S,P,T,X)** REAL*8 S,P,T,X

Input Values:

P - Pressure *p* in bar

T - Temperature *t* in °C

X - Vapor fraction *x* (kg of saturated steam)/(kg wet steam)

Result

SPTXPROP, **S** or **s_ptx_PROP** - Specific entropy *s* in kJ/kg K

Range of validity

Temperature range: from t_{mel} to 326.85 °C

Pressure range: from $p_s(t_t) = 1.7517 \cdot 10^{-9}$ bar to 1000 bar

Details on the vapor fraction *x* and on the calculation of wet steam

The wet steam region is calculated automatically by the subprograms. For this purpose the following fixed details on the vapor fraction *x* are to be considered:

If the state point to be calculated is located in the single-phase region (liquid or superheated steam) x = –1 must be entered as a pro-forma value.

If the state point to be calculated is located in the wet steam region, a value for *x* between 0 and 1 (x = 0 for saturated liquid, x = 1 for saturated steam) must be entered.

When calculating wet steam either the given value for *t* and p = -1000 or the given value for *p* and t = -1000 and in both cases the value for *x* between 0 and 1 must be entered.

If *p* and *t* and *x* are entered as given values, the program considers *p* and *t* to be appropriate to represent the vapor pressure curve.

Wet steam region: Temperature ranges from $t_t = -187.625$ °C to $t_c = 96.74$ °C

Pressure ranges from $p_s(t_t) = 1.7517 \cdot 10^{-9}$ bar to $p_c = 42.512$ bar

Results for wrong input values

Result **SPTXPROP = -1000**, **S = -1000** or **s_ptx_PROP = -1000** for input values:

Single phase region: $p > 1000$ bar or $p < p_s(t_t) = 1.7517 \cdot 10^{-9}$ bar or

(*x* = -1) $t > 326.85$ °C or $t < t_{mel}$

Wet steam region: at $p = -1000$ and $t > t_c = 96.74$ °C or $t < t_t = -187.625$ °C

at $t = -1000$ and $p > p_c = 42.512$ bar or $p < p_s(t_t) = 1.7517 \cdot 10^{-9}$ bar or

at $p > p_c = 42.512$ bar or $p < p_s(t_t) = 1.7517 \cdot 10^{-9}$ bar and

$t > t_c = 96.74$ °C or $t < t_t = -187.625$ °C

References: [22], [25]

Backward Function: Temperature t = f(p,h)

Function Name:	**t_ph_PROP**
Subroutine with function value: for call from Fortran	**REAL*8 FUNCTION TPHPROP(P,H)** REAL*8 P,H
Subroutine with parameter: for call from DLL	**INTEGER*4 FUNCTION C_TPHPROP(T,P,H)** REAL*8 T,P,H

Input Values:

P - Pressure p in bar

H - Specific enthalpy h in kJ/kg

Result

TPHPROP, **T** or **t_ph_PROP** - Temperature t in °C

Range of validity

Temperature range: from t_{mel} to 326.85 °C

Pressure range: from $p_s(t_t) = 1.7517 \cdot 10^{-9}$ bar to 1000 bar

Details on the calculation of wet steam

The wet steam region is calculated automatically. This means that from the given values of p and h the function will determine whether the state point to be calculated is located within the single-phase region (liquid or steam) or the wet steam region. Afterwards the calculation of t in the appropriate region will be carried out.

Wet steam region: Pressure ranges from $p_s(t_t) = 1.7517 \cdot 10^{-9}$ bar to $p_c = 42.512$ bar

Results for wrong input values

Result **TPHPROP**, **T = -1000** or **t_ph_PROP = -1000** for input values:

Single phase region:	$p > 1000$ bar or $p < p_s(t_t) = 1.7517 \cdot 10^{-9}$ bar or
(x = -1)	$t > 326.85$ °C , $t < t_t = -187.625$ °C or $t < t_{mel}(p)$
Wet steam region:	at $p > p_c = 42.512$ bar or $p < p_s(t_t) = 1.7517 \cdot 10^{-9}$ bar or
	at result $t > t_c = 96.74$ °C or $t < t_t = -187.625$ °C

References: [22], [25]

Backward Function: Temperature t = f(p,s)

Function Name:	**t_ps_PROP**
Subroutine with function value: for call from Fortran	**REAL*8 FUNCTION TPSPROP(P,S)** REAL*8 P,S
Subroutine with parameter: for call from DLL	**INTEGER*4 FUNCTION C_TPSPROP(T,P,S)** REAL*8 T,P,S

Input Values:

P - Pressure p in bar

S - Specific entropy s in kJ/(kg K)

Result

TPSPROP, **T** or **t_ps_PROP** - Temperature t in °C

Range of validity

Temperature range: from t_{mel} to 326.85 °C

Pressure range: from $p_s(t_t) = 1.7517 \cdot 10^{-9}$ bar to 1000 bar

Details on the calculation of wet steam

The wet steam region is calculated automatically. This means that from the given values of p and s the function will determine whether the state point to be calculated is located within the single-phase region (liquid or steam) or the wet steam region. Afterwards the calculation of t in the appropriate region will be carried out.

Wet steam region: Pressure ranges from $p_s(t_t) = 1.7517 \cdot 10^{-9}$ bar to $p_c = 42.512$ bar

Results for wrong input values

Result **TPSPROP**, **T = -1000** or **t_ps_PROP = -1000** for input values:

Single phase region:	$p > 1000$ bar or $p < p_s(t_t) = 1.7517 \cdot 10^{-9}$ bar or
(x = -1)	$t > 326.85$ °C , $t < t_t = -187.625$ °C or $t < t_{mel}(p)$
Wet steam region:	at $p > p_c = 42.512$ bar or $p < p_s(t_t) = 1.7517 \cdot 10^{-9}$ bar or at result $t > t_c = 96.74$ °C or $t < t_t = -187.625$ °C

References: [22], [25]

Saturation Temperature $t_s = f(p)$

Function Name:	**ts_p_PROP**
Subroutine with function value: for call from Fortran	**REAL*8 FUNCTION TSPPROP(P)** REAL*8 P
Subroutine with parameter: for call from DLL	**INTEGER*4 FUNCTION C_TSPPROP(TS,P)** REAL*8 TS,P

Input Values:

P - Pressure p in bar

Result

TSPPROP, **TS** or **ts_p_PROP** – Saturation temperature t_s in °C

Range of validity

Pressure range: from $p_s(t_t) = 1.7517 \cdot 10^{-9}$ bar to $p_c = 42.512$ bar

Results for wrong input values

Result **TSPPROP = -1000**, **TS = -1000** or **ts_p_PROP = -1000** for input values:

$p < p_s(t_t) = 1.7517 \cdot 10^{-9}$ bar or $p > p_c = 42.512$ bar

References: [22], [25]

Melting Temperature $t_{mel} = f(p)$

Function Name:	**tmel_p_PROP**
Subroutine with function value: for call from Fortran	**REAL*8 FUNCTION TMELPROP(P)** REAL*8 P
Subroutine with parameter: for call from DLL	**INTEGER*4 FUNCTION C_TMELPROP(TMEL,P)** REAL*8 TMEL,P

Input Values:

P - Pressure p in bar

Result

TMELPROP, **TMEL** or **tmel_p_PROP** – Melting temperature t_{mel} in °C

Range of validity

Pressure range: from $p_s(t_t) = 1.7517 \cdot 10^{-9}$ bar to 1000 bar

Results for wrong input values

Result **TMELPROP = -1000**, **TMEL = -1000** or **tmel_p_PROP = -1000** for input values:

$p < p_s(t_t) = 1.7517 \cdot 10^{-9}$ bar or $p > p_c = 42.512$ bar

References: [28], [25]

Specific Internal Energy *u* = f(*p*,*t*,*x*)

Function Name:	**u_ptx_PROP**
Subroutine with function value: for call from Fortran	**REAL*8 FUNCTION UPTXPROP(P,T,X)** REAL*8 P,T,X
Subroutine with parameter: for call from DLL	**INTEGER*4 FUNCTION C_UPTXPROP(H,P,T,X)** REAL*8 H,P,T,X

Input Values:

P - Pressure *p* in bar

T - Temperature *t* in °C

X - Vapor fraction *x* (kg of saturated steam)/(kg wet steam)

Result

UPTXPROP, **U** or **u_ptx_PROP** - Specific internal energy *u* in kJ/kg

Range of validity

Temperature range: from t_{mel} to 326.85 °C

Pressure range: from $p_s(t_t) = 1.7517 \cdot 10^{-9}$ bar to 1000 bar

Details on the vapor fraction *x* and on the calculation of wet steam

The wet steam region is calculated automatically by the subprograms. For this purpose the following fixed details on the vapor fraction *x* are to be considered:

If the state point to be calculated is located in the single-phase region (liquid or superheated steam) x = –1 must be entered as a pro-forma value.

If the state point to be calculated is located in the wet steam region, a value for *x* between 0 and 1 (x = 0 for saturated liquid, x = 1 for saturated steam) must be entered.

When calculating wet steam either the given value for *t* and p = -1000 or the given value for *p* and t = -1000 and in both cases the value for *x* between 0 and 1 must be entered.

If *p* and *t* and *x* are entered as given values, the program considers *p* and *t* to be appropriate to represent the vapor pressure curve.

Wet steam region: Temperature ranges from $t_t = -187.625$ °C to $t_c = 96.74$ °C

Pressure ranges from $p_s(t_t) = 1.7517 \cdot 10^{-9}$ bar to $p_c = 42.512$ bar

Results for wrong input values

Result **UPTXPROP = -1000**, **H = -1000** or **u_ptx_PROP = -1000** for input values:

Single phase region: $p > 1000$ bar or $p < p_s(t_t) = 1.7517 \cdot 10^{-9}$ bar or

(*x* = -1) $t > 326.85$ °C or $t < t_{mel}$

Wet steam region: at $p = -1000$ and $t > t_c = 96.74$ °C or $t < t_t = -187.625$ °C

at $t = -1000$ and $p > p_c = 42.512$ bar or $p < p_s(t_t) = 1.7517 \cdot 10^{-9}$ bar or

at $p > p_c = 42.512$ bar or $p < p_s(t_t) = 1.7517 \cdot 10^{-9}$ bar and

$t > t_c = 96.74$ °C or $t < t_t = -187.625$ °C

References: [22], [25]

Specific Volume v = f(p,t,x)

Function Name: **v_ptx_PROP**

Subroutine with function value: **REAL*8 FUNCTION VPTXPROP(P,T,X)**
for call from Fortran REAL*8 P,T,X

Subroutine with parameter: **INTEGER*4 FUNCTION C_VPTXPROP(V,P,T,X)**
for call from DLL REAL*8 V,P,T,X

Input Values:

P - Pressure p in bar

T - Temperature t in °C

X - Vapor fraction x (kg of saturated steam)/(kg wet steam)

Result

VPTXPROP, **V** or **v_ptx_PROP** – Specific volume v in m^3 / kg

Range of validity

Temperature range: from t_{mel} to 326.85 °C

Pressure range: from $p_s(t_t) = 1.7517 \cdot 10^{-9}$ bar to 1000 bar

Details on the vapor fraction x and on the calculation of wet steam

The wet steam region is calculated automatically by the subprograms. For this purpose the following fixed details on the vapor fraction x are to be considered:

If the state point to be calculated is located in the single-phase region (liquid or superheated steam) x = –1 must be entered as a pro-forma value.

If the state point to be calculated is located in the wet steam region, a value for x between 0 and 1 (x = 0 for saturated liquid, x = 1 for saturated steam) must be entered.

When calculating wet steam either the given value for t and p = -1000 or the given value for p and t = -1000 and in both cases the value for x between 0 and 1 must be entered.

If p and t and x are entered as given values, the program considers p and t to be appropriate to represent the vapor pressure curve.

Wet steam region: Temperature ranges from $t_t = -187.625$ °C to $t_c = 96.74$ °C

Pressure ranges from $p_s(t_t) = 1.7517 \cdot 10^{-9}$ bar to $p_c = 42.512$ bar

Results for wrong input values

Result **VPTXPROP = -1000**, **V = -1000** or **v_ptx_PROP = -1000** for input values:

Single phase region: $p > 1000$ bar or $p < p_s(t_t) = 1.7517 \cdot 10^{-9}$ bar or
(x = -1) $t > 326.85$ °C or $t < t_{mel}$

Wet steam region: at $p = -1000$ and $t > t_c = 96.74$ °C or $t < t_t = -187.625$ °C

at $t = -1000$ and $p > p_c = 42.512$ bar or $p < p_s(t_t) = 1.7517 \cdot 10^{-9}$ bar or

at $p > p_c = 42.512$ bar or $p < p_s(t_t) = 1.7517 \cdot 10^{-9}$ bar and
$t > t_c = 96.74$ °C or $t < t_t = -187.625$ °C

References: [22], [25]

Isentropic Speed of Sound *w* = f(*p*,*t*,*x*)

Function Name:	**w_ptx_PROP**
Subroutine with function value: for call from Fortran	**REAL*8 FUNCTION WPTXPROP(P,T,X)** REAL*8 P,T,X
Subroutine with parameter: for call from DLL	**INTEGER*4 FUNCTION C_WPTXPROP(W,P,T,X)** REAL*8 W,P,T,X

Input Values:

P - Pressure *p* in bar

T - Temperature *t* in °C

X - Vapor fraction *x* (kg of saturated steam)/(kg wet steam)

Result

WPTXPROP, **W** or **w_ptx_PROP** - Speed of sound *w* in m/s

Range of validity

Temperature range: from t_{mel} to 326.85 °C

Pressure range: from $p_s(t_t) = 1.7517 \cdot 10^{-9}$ bar to 1000 bar

Details on the vapor fraction *x* and on the calculation of saturated liquid and saturated steam

The wet steam region is calculated automatically by the subprograms. For this purpose the following fixed details on the vapor fraction *x* are to be considered:

If the state point to be calculated is located in the single-phase region (liquid or superheated steam) x = –1 must be entered as a pro-forma value.

If the state point to be calculated is located on the saturated liquid line, x = 0 must be entered. When calculating saturated steam (saturated vapor line) x = 1 must be entered.
The calculation for *x*-values between 0 and 1 is not possible.

When calculating saturated liquid or saturated steam, it is adequate to enter either the given value for *t* and p = -1, or the given value for *p* and t = -1, plus the value for *x* (x = 0 or x = 1). If *p* and *t* and *x* are entered as given values, the program will consider *p* and *t* to be appropriate to represent the vapor pressure curve.

Saturated liquid and saturated vapor line :

Temperature ranges from $t_t = -187.625$ °C to $t_c = 96.74$ °C

Pressure ranges from $p_s(t_t) = 1.7517 \cdot 10^{-9}$ bar to $p_c = 42.512$ bar

Results for wrong input values

Result **WPTXPROP = -1000** or **w_ptx_PROP = -1000** for input values:

Single phase region:	$p > 1000$ bar or $p < p_s(t_t) = 1.7517 \cdot 10^{-9}$ bar or
(*x* = -1)	$t > 326.85$ °C or $t < t_{mel}$
Saturation lines:	at $p = -1000$ and $t > t_c = 96.74$ °C or $t < t_t = -187.625$ °C
	at $t = -1000$ and $p > p_c = 42.512$ bar or $p < p_s(t_t) = 1.7517 \cdot 10^{-9}$ bar or
	at $p > p_c = 42.512$ bar or $p < p_s(t_t) = 1.7517 \cdot 10^{-9}$ bar and $t > t_c = 96.74$ °C or $t < t_t = -187.625$ °C

References: [22], [25]

Backward Function: Vapor Fraction *x* = f(*p*,*h*)

Function Name:	**x_ph_PROP**
Subroutine with function value: for call from Fortran	**REAL*8 FUNCTION XPHPROP(P,H)** REAL*8 P,H
Subroutine with parameter: for call from DLL	**INTEGER*4 FUNCTION C_XPHPROP(T,P,H)** REAL*8 X,P,H

Input Values:

P - Pressure *p* in bar

H - Specific enthalpy *h* in kJ/kg

Result

XPHPROP, **X** or **x_ph_PROP** - Vapor fraction *x* in (kg saturated steam/kg wet steam)

Range of validity

Temperature range: from t_{mel} to 326.85 °C

Pressure range: from $p_s(t_t) = 1.7517 \cdot 10^{-9}$ bar to 1000 bar

Details on the calculation of wet steam

The wet steam region is calculated automatically. This means that from the given values of *p* and *h* the function will determine whether the state point to be calculated is located within the single-phase region (liquid or steam) or the wet steam region. When calculating wet steam the value for x between 0 and 1 is calculated (0 for saturated liquid, 1 for saturated steam). If the state point to be calculated is located in the single-phase region the result x = - 1 will be returned.

Wet steam region: Pressure ranges from $p_s(t_t) = 1.7517 \cdot 10^{-9}$ bar to $p_c = 42.512$ bar

Results for wrong input values

Result **X_PH_PROP**, **X =** -1 or **x_ph_PROP =** -1 for input values:

If the state point is located in the single phase region

$p > p_c = 42.512$ bar or $p < p_s(t_t) = 1.7517 \cdot 10^{-9}$ bar

References: [22], [25]

Backward Function: Vapor Fraction *x* = f(*p*,*s*)

Function Name:	**x_ps_PROP**
Subroutine with function value: for call from Fortran	**REAL*8 FUNCTION XPSPROP(P,S)** REAL*8 P,S
Subroutine with parameter: for call from DLL	**INTEGER*4 FUNCTION C_XPSPROP(X,P,S)** REAL*8 X,P,S

Input Values:

P - Pressure *p* in bar

S - Specific entropy *s* in kJ/(kg K)

Result

XPSPROP, **X** or **x_ps_PROP** - Vapor fraction *x* in (kg saturated steam/kg wet steam)

Range of validity

Temperature range: from t_{mel} to 326.85 °C

Pressure range: from $p_s(t_t) = 1.7517 \cdot 10^{-9}$ bar to 1000 bar

Details on the calculation of wet steam

The wet steam region is calculated automatically. This means that from the given values of *p* and *s* the function will determine whether the state point to be calculated is located within the single-phase region (liquid or steam) or the wet steam region. When calculating wet steam the value for x between 0 and 1 is calculated (0 for saturated liquid, 1 for saturated steam). If the state point to be calculated is located in the single-phase region the result x = - 1 will be returned.

Wet steam region: Pressure ranges from $p_s(t_t) = 1.7517 \cdot 10^{-9}$ bar to $p_c = 42.512$ bar

Results for wrong input values

Result **X_PS_PROP**, **X = -1** or **x_ps_PROP = -1** for input values:

If the state point is located in the single phase region

$p > p_c = 42.512$ bar or $p < p_s(t_t) = 1.7517 \cdot 10^{-9}$ bar

References: [22], [25]

KCE ThermoFluidProperties

KCE-ThermoFluidProperties
www.thermofluidprop.com

Hochschule Zittau/Görlitz
UNIVERSITY OF APPLIED SCIENCES

Property Libraries for Calculating Heat Cycles, Boilers, Turbines and Refrigerators

Water and Steam

Library LibIF97

- Industrial Formulation IAPWS-IF97 (Revision 2007)
- Supplementary Standards IAPWS-IF97-S01, -S03rev, -S04, and -S05
- IAPWS Revised Advisory Note No. 3 on Thermo-dynamic Derivatives (2008)

Library LibIF97_META

- Industrial Formulation IAPWS-IF97 (Revision 2007) for metastable steam

Humid Combustion Gas Mixtures

Library LibHuGas

Model: Ideal mixture of the real fluids:

CO_2 - Span, Wagner H_2O - IAPWS-95
O_2 - Schmidt, Wagner N_2 - Span et al.
Ar - Tegeler et al.

and of the ideal gases:

SO_2, CO, Ne
(Scientific Formulation of Bücker et al.)

Consideration of:

- Dissociation from VDI 4670
- Poynting effect

Humid Air

Library LibHuAir

Model: Ideal mixture of the real fluids:

- Dry air from Lemmon et al.
- Steam, water and ice from IAPWS-IF97 and IAPWS-06

Consideration of:

- Condensation and freezing of steam
- Dissociation from VDI 4670
- Poynting effect from ASHRAE RP-1485

Extremely Fast Property Calculations

Spline-Based Table Look-up Method (SBTL)

Library LibSBTL_IF97
Library LibSBTL_95
Library LibSBTL_HuAir

For steam, water, humid air, carbon dioxide and other fluids and mixtures according IAPWS Guideline 2015 for Computational Fluid Dynamics (CFD), real-time and non-stationary simulations

Carbon Dioxide Including Dry Ice

Library LibCO2

Formulation of Span and Wagner (1996)

Seawater

Library LibSeaWa

IAPWS Industrial Formulation 2013

Ice

Library LibICE

Ice from IAPWS-06, Melting and sublimation pressures from IAPWS-08, Water from IAPWS-IF97, Steam from IAPWS-95 and -IF97

Ideal Gas Mixtures

Library LibIdGasMix

Model: Ideal mixture of the ideal gases:

Ar	NO	He	Propylene
Ne	H_2O	F_2	Propane
N_2	SO_2	NH_3	Iso-Butane
O_2	H_2	Methane	n-Butane
CO	H_2S	Ethane	Benzene
CO_2	OH	Ethylene	Methanol
Air			

Consideration of:

- Dissociation from the VDI Guideline 4670

Library LibIDGAS

Model: Ideal gas mixture from VDI Guideline 4670

Consideration of:

- Dissociation from the VDI Guideline 4670

Humid Air

Library ASHRAE LibHuAirProp

Model: Virial equation from ASHRAE Report RP-1485 for real mixture of the real fluids:
- Dry air
- Steam

Consideration of:

- Enhancement of the partial saturation pressure of water vapor at elevated total pressures

www.ashrae.org/bookstore

Dry Air Including Liquid Air

Library LibRealAir

Formulation of Lemmon et al. (2000)

Refrigerants

Ammonia

Library LibNH3

Formulation of Tillner-Roth et al. (1993)

R134a

Library LibR134a

Formulation of Tillner-Roth and Baehr (1994)

Iso-Butane

Library LibButane_Iso

Formulation of Bücker and Wagner (2006)

n-Butane

Library LibButane_n

Formulation of Bücker and Wagner (2006)

Mixtures for Absorption Processes

Ammonia/Water Mixtures

Library LibAmWa

IAPWS Guideline 2001 of Tillner-Roth and Friend (1998)

Helmholtz energy equation for the mixing term

(also useable for calculating the Kalina Cycle)

Water/Lithium Bromide Mixtures

Library LibWaLi

Formulation of Kim and Infante Ferreira (2004)

Gibbs energy equation for the mixing term

Liquid Coolants

Liquid Secondary Refrigerants

Library LibSecRef

Liquid solutions of water with

$C_2H_6O_2$	Ethylene glycol
$C_3H_8O_2$	Propylene glycol
C_2H_5OH	Ethanol
CH_3OH	Methanol
$C_3H_8O_3$	Glycerol
K_2CO_3	Potassium carbonate
$CaCl_2$	Calcium chloride
$MgCl_2$	Magnesium chloride
NaCl	Sodium chloride
$C_2H_3KO_2$	Potassium acetate
$CHKO_2$	Potassium formate
LiCl	Lithium chloride
NH_3	Ammonia

Formulation of the International Institute of Refrigeration (IIR 2010)

Ethanol

Library LibC2H5OH

Formulation of
Schroeder et al. (2014)

Methanol

Library LibCH3OH

Formulation of
de Reuck and Craven (1993)

Propane

Library LibPropane

Formulation of
Lemmon et al. (2009)

Siloxanes as ORC Working Fluids

Octamethylcyclotetrasiloxane $C_8H_{24}O_4Si_4$ **Library LibD4**

Decamethylcyclopentasiloxane $C_{10}H_{30}O_5Si_5$ **Library LibD5**

Tetradecamethylhexasiloxane $C_{14}H_{42}O_5Si_6$ **Library LibMD4M**

Hexamethyldisiloxane $C_6H_{18}OSi_2$ **Library LibMM**

Formulation of Colonna et al. (2006)

Dodecamethylcyclohexasiloxane $C_{12}H_{36}O_6Si_6$ **Library LibD6**

Decamethyltetrasiloxane $C_{10}H_{30}O_3Si_4$ **Library LibMD2M**

Dodecamethylpentasiloxane $C_{12}H_{36}O_4Si_5$ **Library LibMD3M**

Octamethyltrisiloxane $C_8H_{24}O_2Si_3$ **Library LibMDM**

Formulation of Colonna et al. (2008)

Nitrogen and Oxygen

**Libraries
LibN2 and LibO2**

Formulations of Span et al. (2000)
and Schmidt and Wagner (1985)

Hydrogen

Library LibH2

Formulation of
Leachman et al. (2009)

Helium

Library LibHe

Formulation of
Arp et al. (1998)

Hydrocarbons

Decane $C_{10}H_{22}$ **Library LibC10H22**

Isopentane C_5H_{12} **Library LibC5H12_Iso**

Neopentane C_5H_{12} **Library LibC5H12_Neo**

Isohexane C_6H_{14} **Library LibC6H14**

Toluene C_7H_8 **Library LibC7H8**

Formulation of Lemmon and Span (2006)

Further Fluids

Carbon monoxide **CO** **Library LibCO**

Carbonyl sulfide **COS** **Library LibCOS**

Hydrogen sulfide H_2S **Library LibH2S**

Nitrous oxide N_2O **Library LibN2O**

Sulfur dioxide SO_2 **Library LibSO2**

Acetone C_3H_6O **Library LibC3H6O**

Formulation of Lemmon and Span (2006)

KCE
ThermoFluidProperties

For more information please contact:

KCE-ThermoFluidProperties UG & Co. KG
Prof. Dr. Hans-Joachim Kretzschmar
Wallotstr. 3
01307 Dresden, Germany

Internet: www.thermofluidprop.com
Email: info@thermofluidprop.com
Phone: +49-351-27597860
Mobile: +49-172-7914607
Fax: +49-3222-1095810

The following thermodynamic and transport properties can be calculated[a]:

Thermodynamic Properties

- Vapor pressure p_s
- Saturation temperature T_s
- Density ρ
- Specific volume v
- Enthalpy h
- Internal energy u
- Entropy s
- Exergy e
- Isobaric heat capacity c_p
- Isochoric heat capacity c_v
- Isentropic exponent κ
- Speed of sound w
- Surface tension σ

Transport Properties

- Dynamic viscosity η
- Kinematic viscosity ν
- Thermal conductivity λ
- Prandtl number Pr
- Thermal diffusivity a

Backward Functions

- T, v, s (p,h)
- T, v, h (p,s)
- p, T, v (h,s)
- p, T (v,h)
- p, T (v,u)

Thermodynamic Derivatives

- Partial derivatives used in process modeling can be calculated.

[a] Not all of these property functions are available in all property libraries.

www.thermofluidprop.com

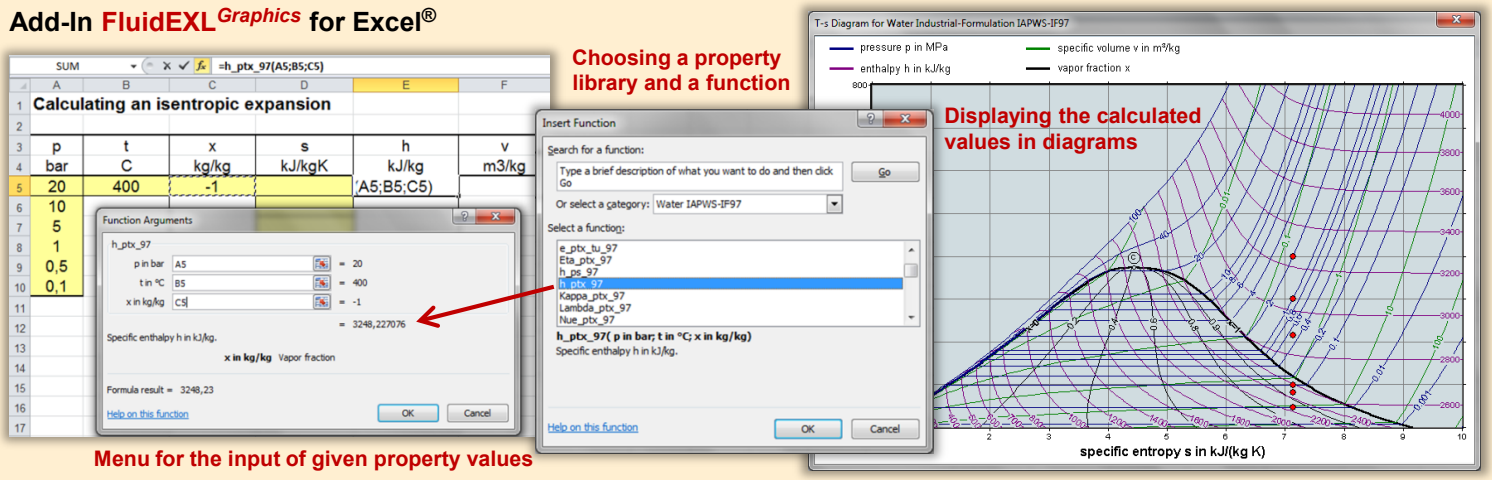
KCE-ThermoFluidProperties
www.thermofluidprop.com

KCE ThermoFluidProperties

Hochschule Zittau/Görlitz
UNIVERSITY OF APPLIED SCIENCES

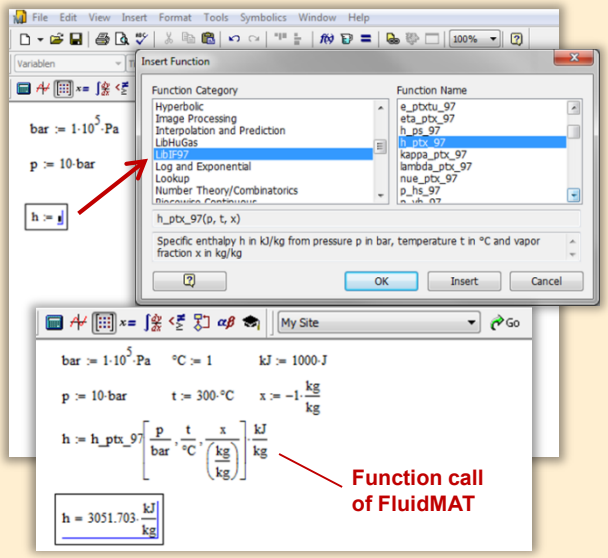
Property Software for Calculating Heat Cycles, Boilers, Turbines and Refrigerators

Add-In FluidEXL*Graphics* for Excel®



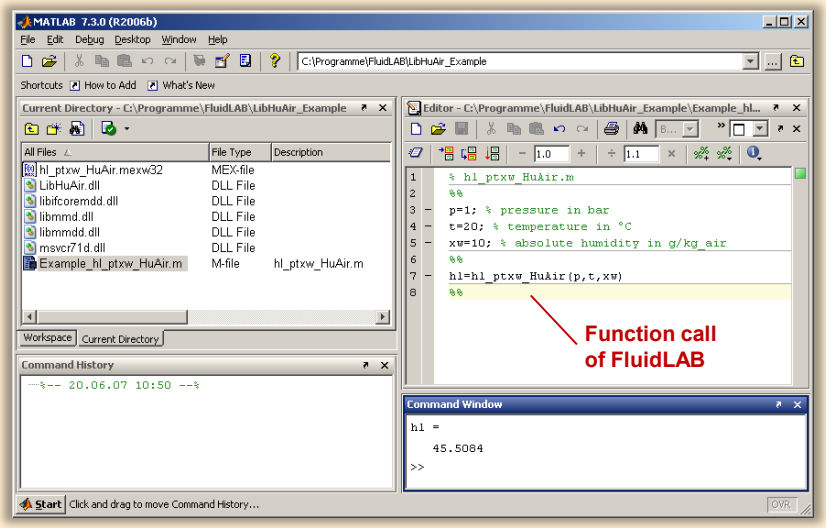
Add-On FluidMAT for Mathcad®
Add-On FluidPRIME for Mathcad Prime®

The property libraries can be used in Mathcad® and Mathcad Prime®.



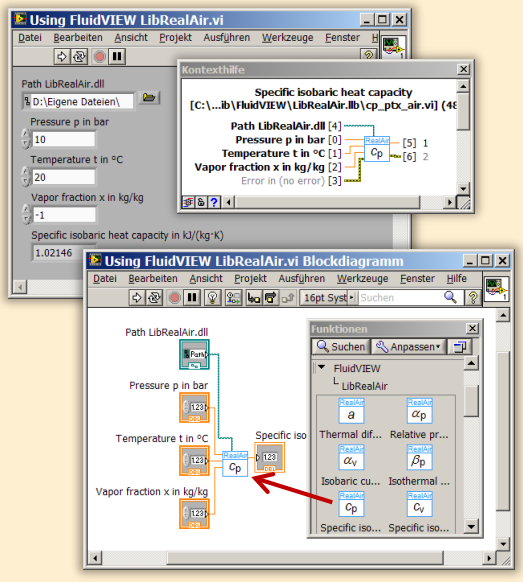
Add-On FluidLAB for MATLAB® and SIMULINK®

Using the Add-In FluidLAB the property functions can be called in MATLAB® and SIMULINK®.



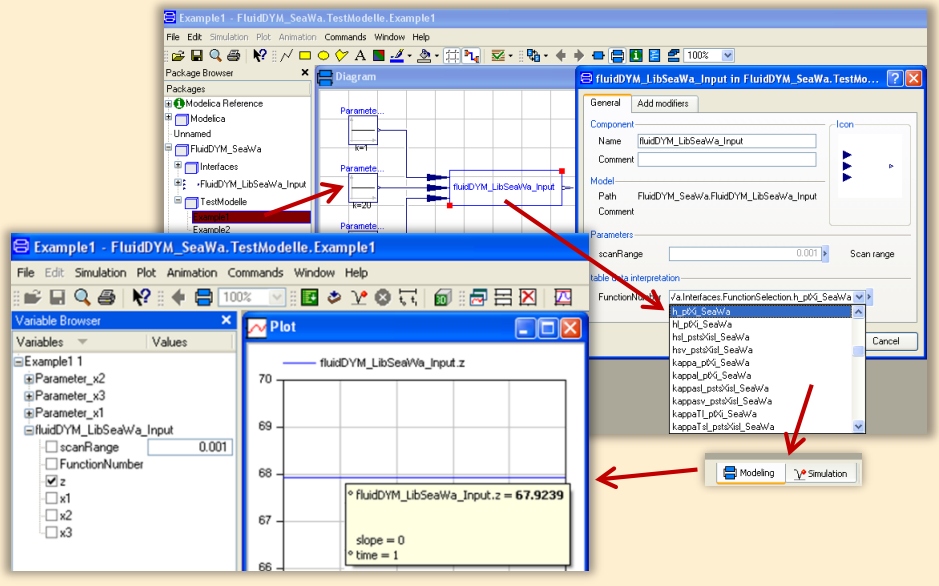
Add-On FluidVIEW for LabVIEW™

The property functions can be calculated in LabVIEW™.

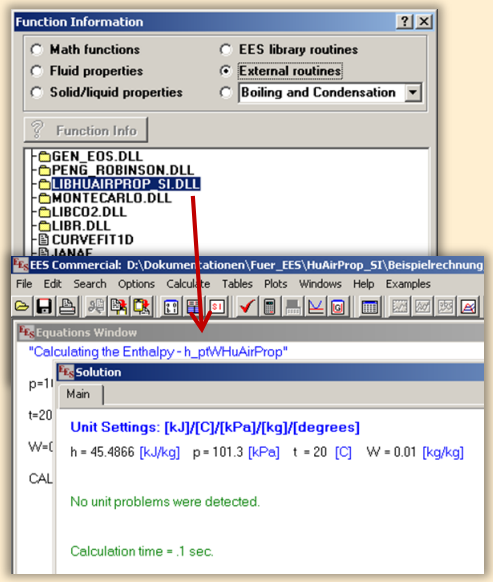


Add-On FluidDYM for DYMOLA® (Modelica) and SimulationX®

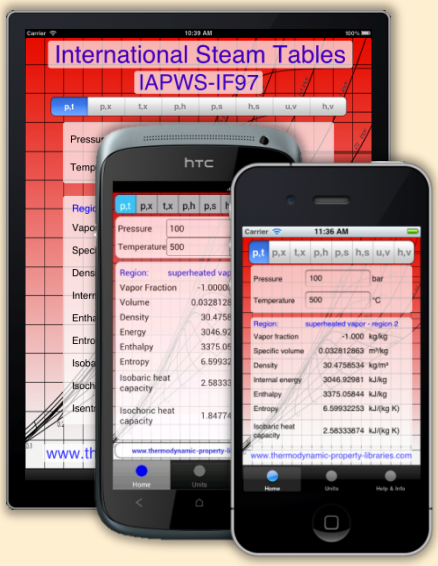
The property functions can be called in DYMOLA® and SimulationX®.



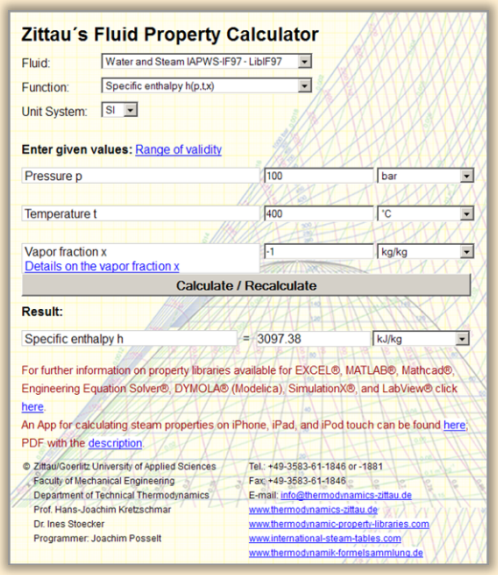
Add-On FluidEES for Engineering Equation Solver®



App International Steam Tables for iPhone, iPad, iPod touch, Android Smartphones and Tablets



Online Property Calculator at www.thermofluidprop.com



Property Software for Pocket Calculators

FluidCasio

fx 9750 G II

CFX 9850 fx-GG20

CFX 9860 G Graph 85

ALGEBRA FX 2.0

FluidHP

HP 48

HP 49

FluidTI

TI Nspire CX CAS
TI Nspire CAS

TI 83
TI 84
TI 89

TI Voyage 200

TI 92

For more information please contact:

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Phone: +49-351-27597860
Mobile: +49-172-7914607
Fax: +49-3222-1095810

The following thermodynamic and transport properties[a] can be calculated in Excel®, MATLAB®, Mathcad®, Engineering Equation Solver® (EES), DYMOLA® (Modelica), SimulationX® and LabVIEW™:

Thermodynamic Properties

- Vapor pressure p_s
- Saturation temperature T_s
- Density ρ
- Specific volume v
- Enthalpy h
- Internal energy u
- Entropy s
- Exergy e
- Isobaric heat capacity c_p
- Isochoric heat capacity c_v
- Isentropic exponent κ
- Speed of sound w
- Surface tension σ

Transport Properties

- Dynamic viscosity η
- Kinematic viscosity ν
- Thermal conductivity λ
- Prandtl number Pr
- Thermal diffusivity a

Backward Functions

- T, v, s (p,h)
- T, v, h (p,s)
- p, T, v (h,s)
- p, T (v,h)
- p, T (v,u)

Thermodynamic Derivatives

- Partial derivatives used in process modeling can be calculated.

[a] Not all of these property functions are available in all property libraries.

www.thermofluidprop.com

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6. Satisfied Customers

Date: 07/2019

The following companies and institutions use the property libraries:

- FluidEXL*Graphics* for Excel®
- FluidLAB for MATLAB® and Simulink
- FluidMAT for Mathcad®
- FluidPRIME for Mathcad Prime®
- FluidEES for Engineering Equation Solver® EES
- FluidDYM for Dymola® (Modelica) and SimulationX®
- FluidVIEW for LabVIEW™
- DLLs for Windows™
- Shared Objects for Linux®.

2019

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MIBRAG, Zeitz	06/2019
Pöyry, Zürich, Switzerland	06/2019
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Norsk Energi, Oslo, Norway	05/2019
STEAG Essen	05/2019
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TU Dresden, Institute for Energy Engineering, Dresden	04/2017
SAINT-GOBAIN, Vaujours, France	03/2017
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KAESER Kompressoren, Gera	03/2017
F&R, Praha, Czech Republic	03/2017
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JS Energie & Beratung, Erding	02/2017
Kelvion Brazed PHE, Nobitz-Wilchwitz	02/2017
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SHELL Deutschland Oil, Wesseling	01/2017
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SynErgy Thermal Management, Krefeld	01/2017

2016

BOGE Druckluftsysteme, Bielefeld	12/2016
BFT Planung, Aachen	11/2016
Midiplan, Bietigheim-Bissingen	11/2016
BBE Barnich IB	11/2016
Wenisch IB,	11/2016
INL, Idaho Falls	11/2016
TU Kältetechnik, Dresden	11/2016
Kopf SynGas, Sulz	11/2016
INTVEN, Bellevne (USA)	11/2016
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Webasto Thermo & Comfort SE, Gliching	08/2016
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Planungsbüro Waidhas GmbH, Chemnitz	07/2016
EEB Enerko, Aldershoven	07/2016
IHEBA Naturenergie GmbH & Co. KG, Pfaffenhofen	07/2016
SSP Kälteplaner AG, Wolfertschwenden	07/2016
EEB ENERKO Energiewirtschaftliche Beratung GmbH, Berlin	07/2016
BOGE Kompressoren Otto BOGE GmbH & Co KG, Bielefeld	06/2016
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INWAT, Lodzi, Poland	04/2016
Planungsbüro WAIDHAS GmbH, Chemnitz	04/2016
STEAG Energy Services GmbH, Laszlo Küppers, Zwingenberg	03/2016
WULFF & UMAG Energy Solutions GmbH, Husum	03/2016
FH Bielefeld, Bielefeld	03/2016
EWT Eckert Wassertechnik GmbH, Celle	03/2016
ILK Institut für Luft- und Kältetechnik GmbH, Dresden	02/2016, 06/2016
IEV KEMA - DNV GV – Energie, Dresden	02/2016
Allborg University, Department of Energie, Aalborg, Denmark	02/2016
G.A.M. Heat GmbH, Gräfenhainichen	02/2016
Institut für Luft- und Kältetechnik, Dresden	02/2016, 05/2016, 06/2016
Bosch, Stuttgart	02/2016
INL Idaho National Laboratory, Idaho, USA	11/2016, 01/2016
Friedl ID, Wien, Austria	01/2016
Technical University of Dresden, Dresden	01/2016

2015

EES Enerko, Aachen	12/2015
Ruldolf IB, Strau, Austria	12/2015
Allborg University, Department of Energie, Aalborg, Denmark	12/2015
University of Lyubljana, Slovenia	12/2015
Steinbrecht IB, Berlin	11/2015
Universidad Carlos III de Madrid, Madrid, Spain	11/2015
STEAK, Essen	11/2015
Bosch, Lohmar	10/2015
Team Turbo Machines, Rouen, France	09/2015
BTC – Business Technology Consulting AG, Oldenburg	07/2015
KIT Karlsruhe Institute of Technology, Eggenstein-Leopoldshafen	07/2015
ILK, Dresden	07/2015
Schniewindt GmbH & Co. KG, Neuenwalde	08/2015

2014

PROJEKTPLAN, Dohna	04/2014
Technical University of Vienna, Austria	04/2014
MTU Aero Engines AG, Munich	04/2014
GKS, Schweinfurt	03/2014
Technical University of Nuremberg	03/2014
EP-E, Niederstetten	03/2014
Rückert NatUrgas GmbH, Lauf	03/2014
YESS-World, South Korea	03/2014
ZAB, Dessau	02/2014
KIT-TVT, Karlsruhe	02/2014
Stadtwerke Neuburg	02/2014
COMPAREX, Leipzig for RWE Essen	02/2014
Technical University of Prague, Czech Republic	02/2014
HS Augsburg	02/2014
Envi-con, Nuremberg	01/2014
DLR, Stuttgart	01/2014
Doosan Lentjes, Ratingen	01/2014
Technical University of Berlin	01/2014
Technical University of Munich	01/2014
Technical University of Braunschweig	01/2014
M&M Turbinentechnik, Bielefeld	01/2014

2013

TRANTER-GmbH, Artern	12/2013
SATAKE, Shanghai, China	12/2013
VOITH, Kunshan, China	12/2013
ULT, Löbau	12/2013
MAN, Copenhagen, Dänemark	11/2013
DREWAG, Dresden	11/2013
Haarslev Industries, Herlev, Dänemark	11/2013
STEAG, Herne	11/2013, 12/2013
Ingersoll-Rand, Oberhausen	11/2013
Wilhelm-Büchner HS, Darmstadt	10/2013
IAV, Chemnitz	10/2013
Technical University of Regensburg	10/2013
PD-Energy, Bitterfeld	09/2013
Thermofin, Heinsdorfergrund	09/2013
SHI, New Jersey, USA	09/2013
M&M Turbinentechnik, Bielefeld	08/2013
BEG-BHV, Bremerhaven	08/2013
TIG-Group, Husum	08/2013
COMPAREX, Leipzig for RWE Essen	08/2013, 11/2013 12/2013
University of Budapest, Hungary	08/2013
Siemens, Frankenthal	08/2013, 10/2013

	11/2013
VGB, Essen	07/2013, 11/2013
Brunner Energieberatung, Zurich, Switzerland	07/2013
Technical University of Deggendorf	07/2013
University of Maryland, USA	07/2013, 08/2013
University of Princeton, USA	07/2013
NIST, Boulder, USA	06/2013
IGUS GmbH, Dresden	06/2013
BHR Bilfinger, Essen	06/2013
SÜDSALZ, Bad Friedrichshall	06/2013, 12/2013
Technician School of Berlin	05/2013
KIER, Gajeong-ro, Südkorea	05/2013
Schwing/Stetter GmbH, Memmingen	05/2013
Vattenfall, Berlin	05/2013
AUTARK, Kleinmachnow	05/2013
STEAG, Zwingenberg	05/2013
Hochtief, Düsseldorf	05/2013
University of Stuttgart	04/2013
Technical University -Bundeswehr, Munich	04/2013
Rerum Cognitio Forschungszentrum, Frankfurt	04/2013
Kältetechnik Dresen + Bremen, Alfhausen	04/2013
University Auckland, New Zealand	04/2013
MASDAR Institut, Abu Dhabi, United Arab Emirates	03/2013
Simpelkamp, Dresden	02/2013
VEO, Eisenhüttenstadt	02/2013
ENTEC, Auerbach	02/2013
Caterpillar, Kiel	02/2013
Technical University of Wismar	02/2013
Technical University of Dusseldorf	02/2013
ILK, Dresden	01/2013, 08/2013
Fichtner IT, Stuttgart	01/2013, 11/2013
Schnepf Ingeniuerbüro, Nagold	01/2013
Schütz Engineering, Wadgassen	01/2013
Endress & Hauser, Reinach, Switzerland	01/2013
Oschatz GmbH, Essen	01/2013
frischli Milchwerke, Rehburg-Loccum	01/2013

2012

Voith, Bayreuth	12/2012
Technical University of Munich	12/2012
Dillinger Huette	12/2012
University of Stuttgart	11/2012
Siemens, Muehlheim	11/2012
Sennheiser, Hannover	11/2012
Oschatz GmbH, Essen	10/2012
Fichtner IT, Stuttgart	10/2012, 11/2012
Helbling Technik AG, Zurich, Switzerland	10/2012
University of Duisburg	10/2012

Rerum Cognitio Forschungszentrum, Frankfurt	09/2012
Pöyry Deutschland GmbH, Dresden	08/2012
Extracciones, Guatemala	08/2012
RWE, Essen	08/2012
Weghaus Consulting Engineers, Wuerzburg	08/2012
GKS, Schweinfurt	07/2012
COMPAREX, Leipzig for RWE Essen	07/2012
GEA, Nobitz	07/2012
Meyer Werft, Papenburg	07/2012
STEAG, Herne	07/2012
GRS, Cologne	06/2012
Fichtner IT Consult, Chennai, India	06/2012
Siemens, Freiburg	06/2012
Nikon Research of America, Belmont, USA	06/2012
Niederrhein University of Applied Sciences, Krefeld	06/2012
STEAG, Zwingenberg	06/2012
Mainova, Frankfurt on Main via Fichtner IT Consult	05/2012
Endress & Hauser	05/2012
PEU, Espenheim	05/2012
Luzern University of Applied Sciences, Switzerland	05/2012
BASF, Ludwigshafen (general license) via Fichtner IT Consult	05/2012
SPX Balcke-Dürr, Ratingen	05/2012, 07/2012
Gruber-Schmidt, Wien, Austria	04/2012
Vattenfall, Berlin	04/2012
ALSTOM, Baden	04/2012
SKW, Piesteritz	04/2012
TERA Ingegneria, Trento, Italy	04/2012
Siemens, Erlangen	04/2012, 05/2012
LAWI Power, Dresden	04/2012
Stadtwerke Leipzig	04/2012
SEITZ, Wetzikon, Switzerland	03/2012, 07/2012
M & M, Bielefeld	03/2012
Sennheiser, Wedemark	03/2012
SPG, Montreuil Cedex, France	02/2012
German Destilation, Sprendlingen	02/2012
Lopez, Munguia, Spain	02/2012
Endress & Hauser, Hannover	02/2012
Palo Alto Research Center, USA	02/2012
WIPAK, Walsrode	02/2012
Freudenberg, Weinheim	01/2012
Fichtner, Stuttgart	01/2012
airinotec, Bayreuth	01/2012, 07/2012
University Auckland, New Zealand	01/2012
VPC, Vetschau	01/2012
Franken Guss, Kitzingen	01/2012

2011

XRG-Simulation, Hamburg	12/2011
Smurfit Kappa PPT, AX Roermond, Netherlands	12/2011
AWTEC, Zurich, Switzerland	12/2011
eins-energie, Bad Elster	12/2011
BeNow, Rodenbach	11/2011
Luzern University of Applied Sciences, Switzerland	11/2011
GMVA, Oberhausen	11/2011
CCI, Karlsruhe	10/2011
W.-Büchner University of Applied Sciences, Pfungstadt	10/2011
PLANAIR, La Sagne, Switzerland	10/2011
LAWI, Dresden	10/2011
Lopez, Munguia, Spain	10/2011
University of KwaZulu-Natal, Westville, South Africa	10/2011
Voith, Heidenheim	09/2011
SpgBe Montreal, Canada	09/2011
SPG TECH, Montreuil Cedex, France	09/2011
Voith, Heidenheim-Mergelstetten	09/2011
MTU Aero Engines, Munich	08/2011
MIBRAG, Zeitz	08/2011
RWE, Essen	07/2011
Fels, Elingerode	07/2011
Weihenstephan University of Applied Sciences	07/2011, 09/2011, 10/2011
Forschungszentrum Juelich	07/2011
RWTH Aachen University	07/2011, 08/2011
INNEO Solutions, Ellwangen	06/2011
Caliqua, Basel, Switzerland	06/2011
Technical University of Freiberg	06/2011
Fichtner IT Consulting, Stuttgart	05/2011, 06/2011, 08/2011
Salzgitter Flachstahl, Salzgitter	05/2011
Helbling Beratung & Bauplanung, Zurich, Switzerland	05/2011
INEOS, Cologne	04/2011
Enseleit Consulting Engineers, Siebigerode	04/2011
Witt Consulting Engineers, Stade	03/2011
Helbling, Zurich, Switzerland	03/2011
MAN Diesel, Copenhagen, Denmark	03/2011
AGO, Kulmbach	03/2011
University of Duisburg	03/2011, 06/2011
CCP, Marburg	03/2011
BASF, Ludwigshafen	02/2011
ALSTOM Power, Baden, Switzerland	02/2011
Universität der Bundeswehr, Munich	02/2011
Calorifer, Elgg, Switzerland	01/2011
STRABAG, Vienna, Austria	01/2011
TUEV Sued, Munich	01/2011

ILK Dresden	01/2011
Technical University of Dresden	01/2011, 05/2011
	06/2011, 08/2011

2010

Umweltinstitut Neumarkt	12/2010
YIT Austria, Vienna, Austria	12/2010
MCI Innsbruck, Austria	12/2010
University of Stuttgart	12/2010
HS Cooler, Wittenburg	12/2010
Visteon, Novi Jicin, Czech Republic	12/2010
CompuWave, Brunntal	12/2010
Stadtwerke Leipzig	12/2010
MCI Innsbruck, Austria	12/2010
EVONIK Energy Services, Zwingenberg	12/2010
Caliqua, Basel, Switzerland	11/2010
Shanghai New Energy Resources Science & Technology, China	11/2010
Energieversorgung Halle	11/2010
Hochschule für Technik Stuttgart, University of Applied Sciences	11/2010
Steinmueller, Berlin	11/2010
Amberg-Weiden University of Applied Sciences	11/2010
AREVA NP, Erlangen	10/2010
MAN Diesel, Augsburg	10/2010
KRONES, Neutraubling	10/2010
Vaillant, Remscheid	10/2010
PC Ware, Leipzig	10/2010
Schubert Consulting Engineers, Weißenberg	10/2010
Fraunhofer Institut UMSICHT, Oberhausen	10/2010
Behringer Consulting Engineers, Tagmersheim	09/2010
Saacke, Bremen	09/2010
WEBASTO, Neubrandenburg	09/2010
Concordia University, Montreal, Canada	09/2010
Compañía Eléctrica de Sochagota, Bogota, Colombia	08/2010
Hannover University of Applied Sciences	08/2010
ERGION, Mannheim	07/2010
Fichtner IT Consulting, Stuttgart	07/2010
TF Design, Matieland, South Africa	07/2010
MCE, Berlin	07/2010, 12/2010
IPM, Zittau/Goerlitz University of Applied Sciences	06/2010
TUEV Sued, Dresden	06/2010
RWE IT, Essen	06/2010
Glen Dimplex, Kulmbach	05/2010, 07/2010
	10/2010
Hot Rock, Karlsruhe	05/2010
Darmstadt University of Applied Sciences	05/2010
Voith, Heidenheim	04/2010
CombTec, Zittau	04/2010
University of Glasgow, Great Britain	04/2010

Universitaet der Bundeswehr, Munich	04/2010
Technical University of Hamburg-Harburg	04/2010
Vattenfall Europe, Berlin	04/2010
HUBER Consulting Engineers, Berching	04/2010
VER, Dresden	04/2010
CCP, Marburg	03/2010
Offenburg University of Applied Sciences	03/2010
Technical University of Berlin	03/2010
NIST Boulder CO, USA	03/2010
Technical University of Dresden	02/2010
Siemens Energy, Nuremberg	02/2010
Augsburg University of Applied Sciences	02/2010
ALSTOM Power, Baden, Switzerland	02/2010, 05/2010
MIT Massachusetts Institute of Technology Cambridge MA, USA	02/2010
Wieland Werke, Ulm	01/2010
Siemens Energy, Goerlitz	01/2010, 12/2010
Technical University of Freiberg	01/2010
ILK, Dresden	01/2010, 12/2010
Fischer-Uhrig Consulting Engineers, Berlin	01/2010

2009

ALSTOM Power, Baden, Schweiz	01/2009, 03/2009 05/2009
Nordostschweizerische Kraftwerke AG, Doettingen, Switzerland	02/2009
RWE, Neurath	02/2009
Brandenburg University of Technology, Cottbus	02/2009
Hamburg University of Applied Sciences	02/2009
Kehrein, Moers	03/2009
EPP Software, Marburg	03/2009
Bernd Münstermann, Telgte	03/2009
Suedzucker, Zeitz	03/2009
CPP, Marburg	03/2009
Gelsenkirchen University of Applied Sciences	04/2009
Regensburg University of Applied Sciences	05/2009
Gatley & Associates, Atlanta, USA	05/2009
BOSCH, Stuttgart	06/2009, 07/2009
Dr. Nickolay, Consulting Engineers, Gommersheim	06/2009
Ferrostal Power, Saarlouis	06/2009
BHR Bilfinger, Essen	06/2009
Intraserv, Wiesbaden	06/2009
Lausitz University of Applied Sciences, Senftenberg	06/2009
Nuernberg University of Applied Sciences	06/2009
Technical University of Berlin	06/2009
Fraunhofer Institut UMSICHT, Oberhausen	07/2009
Bischoff, Aurich	07/2009
Fichtner IT Consulting, Stuttgart	07/2009
Techsoft, Linz, Austria	08/2009
DLR, Stuttgart	08/2009

Wienstrom, Vienna, Austria	08/2009
RWTH Aachen University	09/2009
Vattenfall, Hamburg	10/2009
AIC, Chemnitz	10/2009
Midiplan, Bietigheim-Bissingen	11/2009
Institute of Air Handling and Refrigeration ILK, Dresden	11/2009
FZD, Rossendorf	11/2009
Techgroup, Ratingen	11/2009
Robert Sack, Heidelberg	11/2009
EC, Heidelberg	11/2009
MCI, Innsbruck, Austria	12/2009
Saacke, Bremen	12/2009
ENERKO, Aldenhoven	12/2009

2008

Pink, Langenwang	01/2008
Fischer-Uhrig, Berlin	01/2008
University of Karlsruhe	01/2008
MAAG, Kuesnacht, Switzerland	02/2008
M&M Turbine Technology, Bielefeld	02/2008
Lentjes, Ratingen	03/2008
Siemens Power Generation, Goerlitz	04/2008
Evonik, Zwingenberg (general EBSILON program license)	04/2008
WEBASTO, Neubrandenburg	04/2008
CFC Solutions, Munich	04/2008
RWE IT, Essen	04/2008
Rerum Cognitio, Zwickau	04/2008, 05/2008
ARUP, Berlin	05/2008
Research Center, Karlsruhe	07/2008
AWECO, Neukirch	07/2008
Technical University of Dresden, Professorship of Building Services	07/2008
Technical University of Cottbus, Chair in Power Plant Engineering	07/2008, 10/2008
Ingersoll-Rand, Unicov, Czech Republic	08/2008
Technip Benelux BV, Zoetermeer, Netherlands	08/2008
Fennovoima Oy, Helsinki, Finland	08/2008
Fichtner Consulting & IT, Stuttgart	09/2008
PEU, Espenhain	09/2008
Poyry, Dresden	09/2008
WINGAS, Kassel	09/2008
TUEV Sued, Dresden	10/2008
Technical University of Dresden, Professorship of Thermic Energy Machines and Plants	10/2008, 11/2008
AWTEC, Zurich, Switzerland	11/2008
Siemens Power Generation, Erlangen	12/2008

2007

Audi, Ingolstadt	02/2007
ANO Abfallbehandlung Nord, Bremen	02/2007
TUEV NORD SysTec, Hamburg	02/2007
VER, Dresden	02/2007
Technical University of Dresden, Chair in Jet Propulsion Systems	02/2007
Redacom, Nidau, Switzerland	02/2007
Universität der Bundeswehr, Munich	02/2007
Maxxtec, Sinsheim	03/2007
University of Rostock, Chair in Technical Thermodynamics	03/2007
AGO, Kulmbach	03/2007
University of Stuttgart, Chair in Aviation Propulsions	03/2007
Siemens Power Generation, Duisburg	03/2007
ENTHAL Haustechnik, Rees	05/2007
AWECO, Neukirch	05/2007
ALSTOM, Rugby, Great Britain	06/2007
SAAS, Possendorf	06/2007
Grenzebach BSH, Bad Hersfeld	06/2007
Reichel Engineering, Haan	06/2007
Technical University of Cottbus, Chair in Power Plant Engineering	06/2007
Voith Paper Air Systems, Bayreuth	06/2007
Egger Holzwerkstoffe, Wismar	06/2007
Tissue Europe Technologie, Mannheim	06/2007
Dometic, Siegen	07/2007
RWTH Aachen University, Institute for Electrophysics	09/2007
National Energy Technology Laboratory, Pittsburg, USA	10/2007
Energieversorgung Halle	10/2007
AL-KO, Jettingen	10/2007
Grenzebach BSH, Bad Hersfeld	10/2007
Wiesbaden University of Applied Sciences, Department of Engineering Sciences	10/2007
Endress+Hauser Messtechnik, Hannover	11/2007
Munich University of Applied Sciences, Department of Mechanical Engineering	11/2007
Rerum Cognitio, Zwickau	12/2007
Siemens Power Generation, Erlangen	11/2007
University of Rostock, Chair in Technical Thermodynamics	11/2007, 12/2007

2006

STORA ENSO Sachsen, Eilenburg	01/2006
Technical University of Munich, Chair in Energy Systems	01/2006
NUTEC Engineering, Bisikon, Switzerland	01/2006, 04/2006
Conwel eco, Bochov, Czech Republic	01/2006
Offenburg University of Applied Sciences	01/2006
KOCH Transporttechnik, Wadgassen	01/2006
BEG Bremerhavener Entsorgungsgesellschaft	02/2006
Deggendorf University of Applied Sciences, Department of Mechanical Engineering and Mechatronics	02/2006
University of Stuttgart,	02/2006

Department of Thermal Fluid Flow Engines	
Technical University of Munich,	02/2006
Chair in Apparatus and Plant Engineering	
Energietechnik Leipzig (company license),	02/2006
Siemens Power Generation, Erlangen	02/2006, 03/2006
RWE Power, Essen	03/2006
WAETAS, Pobershau	04/2006
Siemens Power Generation, Goerlitz	04/2006
Technical University of Braunschweig,	04/2006
Department of Thermodynamics	
EnviCon & Plant Engineering, Nuremberg	04/2006
Brassel Engineering, Dresden	05/2006
University of Halle-Merseburg,	05/2006
Department of USET Merseburg incorporated society	
Technical University of Dresden,	05/2006
Professorship of Thermic Energy Machines and Plants	
Fichtner Consulting & IT Stuttgart	05/2006
(company licenses and distribution)	
Suedzucker, Ochsenfurt	06/2006
M&M Turbine Technology, Bielefeld	06/2006
Feistel Engineering, Volkach	07/2006
ThyssenKrupp Marine Systems, Kiel	07/2006
Caliqua, Basel, Switzerland (company license)	09/2006
Atlas-Stord, Rodovre, Denmark	09/2006
Konstanz University of Applied Sciences,	10/2006
Course of Studies Construction and Development	
Siemens Power Generation, Duisburg	10/2006
Hannover University of Applied Sciences,	10/2006
Department of Mechanical Engineering	
Siemens Power Generation, Berlin	11/2006
Zikesch Armaturentechnik, Essen	11/2006
Wismar University of Applied Sciences, Seafaring Department	11/2006
BASF, Schwarzheide	12/2006
Enertech Energie und Technik, Radebeul	12/2006

2005

TUEV Nord, Hannover	01/2005
J.H.K Plant Engineering and Service, Bremerhaven	01/2005
Electrowatt-EKONO, Zurich, Switzerland	01/2005
FCIT, Stuttgart	01/2005
Energietechnik Leipzig (company license)	02/2005, 04/2005
	07/2005
eta Energieberatung, Pfaffenhofen	02/2005
FZR Forschungszentrum, Rossendorf/Dresden	04/2005
University of Saarbruecken	04/2005
Technical University of Dresden	04/2005
Professorship of Thermic Energy Machines and Plants	
Grenzebach BSH, Bad Hersfeld	04/2005
TUEV Nord, Hamburg	04/2005

Technical University of Dresden, Waste Management	05/2005
Siemens Power Generation, Goerlitz	05/2005
Duesseldorf University of Applied Sciences, Department of Mechanical Engineering and Process Engineering	05/2005
Redacom, Nidau, Switzerland	06/2005
Dumas Verfahrenstechnik, Hofheim	06/2005
Alensys Engineering, Erkner	07/2005
Stadtwerke Leipzig	07/2005
SaarEnergie, Saarbruecken	07/2005
ALSTOM ITC, Rugby, Great Britain	08/2005
Technical University of Cottbus, Chair in Power Plant Engineering	08/2005
Vattenfall Europe, Berlin (group license)	08/2005
Technical University of Berlin	10/2005
Basel University of Applied Sciences, Department of Mechanical Engineering, Switzerland	10/2005
Midiplan, Bietigheim-Bissingen	11/2005
Technical University of Freiberg, Chair in Hydrogeology	11/2005
STORA ENSO Sachsen, Eilenburg	12/2005
Energieversorgung Halle (company license)	12/2005
KEMA IEV, Dresden	12/2005

2004

Vattenfall Europe (group license)	01/2004
TUEV Nord, Hamburg	01/2004
University of Stuttgart, Institute of Thermodynamics and Heat Engineering	02/2004
MAN B&W Diesel A/S, Copenhagen, Denmark	02/2004
Siemens AG Power Generation, Erlangen	02/2004
Ulm University of Applied Sciences	03/2004
Visteon, Kerpen	03/2004, 10/2004
Technical University of Dresden, Professorship of Thermic Energy Machines and Plants	04/2004
Rerum Cognitio, Zwickau	04/2004
University of Saarbruecken	04/2004
Grenzebach BSH, Bad Hersfeld	04/2004
SOFBID Zwingenberg (general EBSILON program license)	04/2004
EnBW Energy Solutions, Stuttgart	05/2004
HEW-Kraftwerk, Tiefstack	06/2004
h s energieanlagen, Freising	07/2004
FCIT, Stuttgart	08/2004
Physikalisch Technische Bundesanstalt (PTB), Braunschweig	08/2004
Mainova Frankfurt	08/2004
Rietschle Energieplaner, Winterthur, Switzerland	08/2004
MAN Turbo Machines, Oberhausen	09/2004
TUEV Sued, Dresden	10/2004
STEAG Kraftwerk, Herne	10/2004, 12/2004
University of Weimar	10/2004
energeticals (e-concept), Munich	11/2004
SorTech, Halle	11/2004

Enertech EUT, Radebeul (company license)	11/2004
Munich University of Applied Sciences	12/2004
STORA ENSO Sachsen, Eilenburg	12/2004
Technical University of Cottbus, Chair in Power Plant Engineering	12/2004
Freudenberg Service, Weinheim	12/2004

2003

Paper Factory, Utzenstorf, Switzerland	01/2003
MAB Plant Engineering, Vienna, Austria	01/2003
Wulff Energy Systems, Husum	01/2003
Technip Benelux BV, Zoetermeer, Netherlands	01/2003
ALSTOM Power, Baden, Switzerland	01/2003, 07/2003
VER, Dresden	02/2003
Rietschle Energieplaner, Winterthur, Switzerland	02/2003
DLR, Leupholdhausen	04/2003
Emden University of Applied Sciences, Department of Technology	05/2003
Petterssson+Ahrends, Ober-Moerlen	05/2003
SOFBID ,Zwingenberg (general EBSILON program license)	05/2003
Ingenieurbuero Ostendorf, Gummersbach	05/2003
TUEV Nord, Hamburg	06/2003
Muenstermann GmbH, Telgte-Westbevern	06/2003
University of Cali, Colombia	07/2003
Atlas-Stord, Rodovre, Denmark	08/2003
ENERKO, Aldenhoven	08/2003
STEAG RKB, Leuna	08/2003
eta Energieberatung, Pfaffenhofen	08/2003
exergie, Dresden	09/2003
AWTEC, Zurich, Switzerland	09/2003
Energie, Timelkam, Austria	09/2003
Electrowatt-EKONO, Zurich, Switzerland	09/2003
LG, Annaberg-Buchholz	10/2003
FZR Forschungszentrum, Rossendorf/Dresden	10/2003
EnviCon & Plant Engineering, Nuremberg	11/2003
Visteon, Kerpen	11/2003
VEO Vulkan Energiewirtschaft Oderbruecke, Eisenhuettenstadt	11/2003
Stadtwerke Hannover	11/2003
SaarEnergie, Saarbruecken	11/2003
Fraunhofer-Gesellschaft, Munich	12/2003
Erfurt University of Applied Sciences, Department of Supply Engineering	12/2003
SorTech, Freiburg	12/2003
Mainova, Frankfurt	12/2003
Energieversorgung Halle	12/2003

2002

Hamilton Medical AG, Rhaezuens, Switzerland	01/2002
Bochum University of Applied Sciences, Department of Thermo- and Fluid Dynamics	01/2002

SAAS, Possendorf/Dresden	02/2002
Siemens, Karlsruhe	02/2002
(general license for the WinIS information system)	
FZR Forschungszentrum, Rossendorf/Dresden	03/2002
CompAir, Simmern	03/2002
GKS Gemeinschaftskraftwerk, Schweinfurt	04/2002
ALSTOM Power Baden, Switzerland (group licenses)	05/2002
InfraServ, Gendorf	05/2002
SoftSolutions, Muehlhausen (company license)	05/2002
DREWAG, Dresden (company license)	05/2002
SOFBID, Zwingenberg	06/2002
(general EBSILON program license)	
Kleemann Engineering, Dresden	06/2002
Caliqua, Basel, Switzerland (company license)	07/2002
PCK Raffinerie, Schwedt (group license)	07/2002
Fischer-Uhrig Engineering, Berlin	08/2002
Fichtner Consulting & IT, Stuttgart	08/2002
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Stadtwerke Duisburg	08/2002
Stadtwerke Hannover	09/2002
Siemens Power Generation, Goerlitz	10/2002
Energieversorgung Halle (company license)	10/2002
Bayer, Leverkusen	11/2002
Dillinger Huette, Dillingen	11/2002
G.U.N.T. Geraetebau, Barsbuettel	12/2002
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