

**Zittau/Goerlitz University of Applied Sciences, Germany**  
**Department of Technical Thermodynamics**

[www.thermodynamics-zittau.de](http://www.thermodynamics-zittau.de)



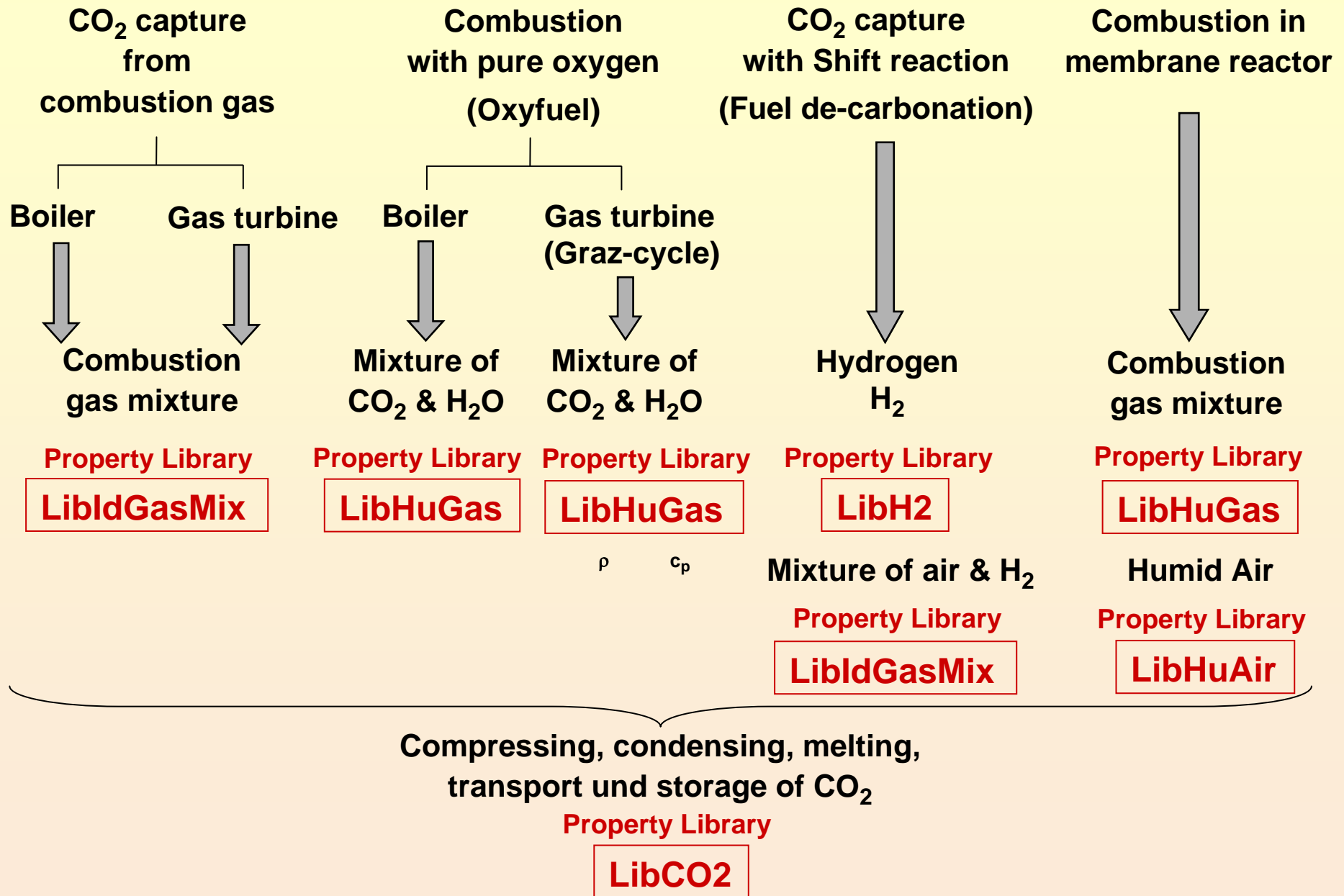
**H.-J. Kretzschmar, I. Stoecker, I. Jaehne, S. Herrmann, M. Kunick, B. Salomo**

## **Property Libraries for Working Fluids for Calculating Heat Cycles, Turbines, Heat Pumps, and Refrigeration Processes**

### **Contents**

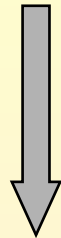
- 1 Property Libraries for Working Fluids**
- 2 Overview of the Property Libraries**
- 3 Property Functions**
- 4 Using the Property Libraries in Excel<sup>®</sup>, MATLAB<sup>®</sup>, and Mathcad<sup>®</sup>**
- 5 Property Libraries for Education and for Pocket Calculators**

# Energy Conversion Processes with CO<sub>2</sub> Capture



# Energy Storage and Hydrogen Supply

Compressed air storage



Humid Air  
at high pressures

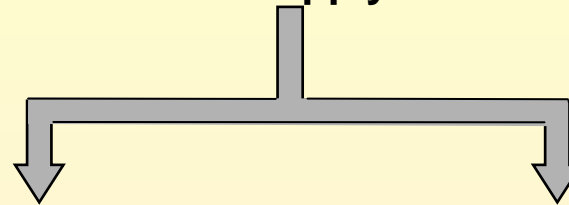
Property Library

**LibHuAir**

Ideal mixture of the  
real fluids dry air  
and steam, water or ice

$\rho$   $c_p$

Hydrogen storage and  
supply



Hydrogen  
at high pressures

Liquid  
hydrogen

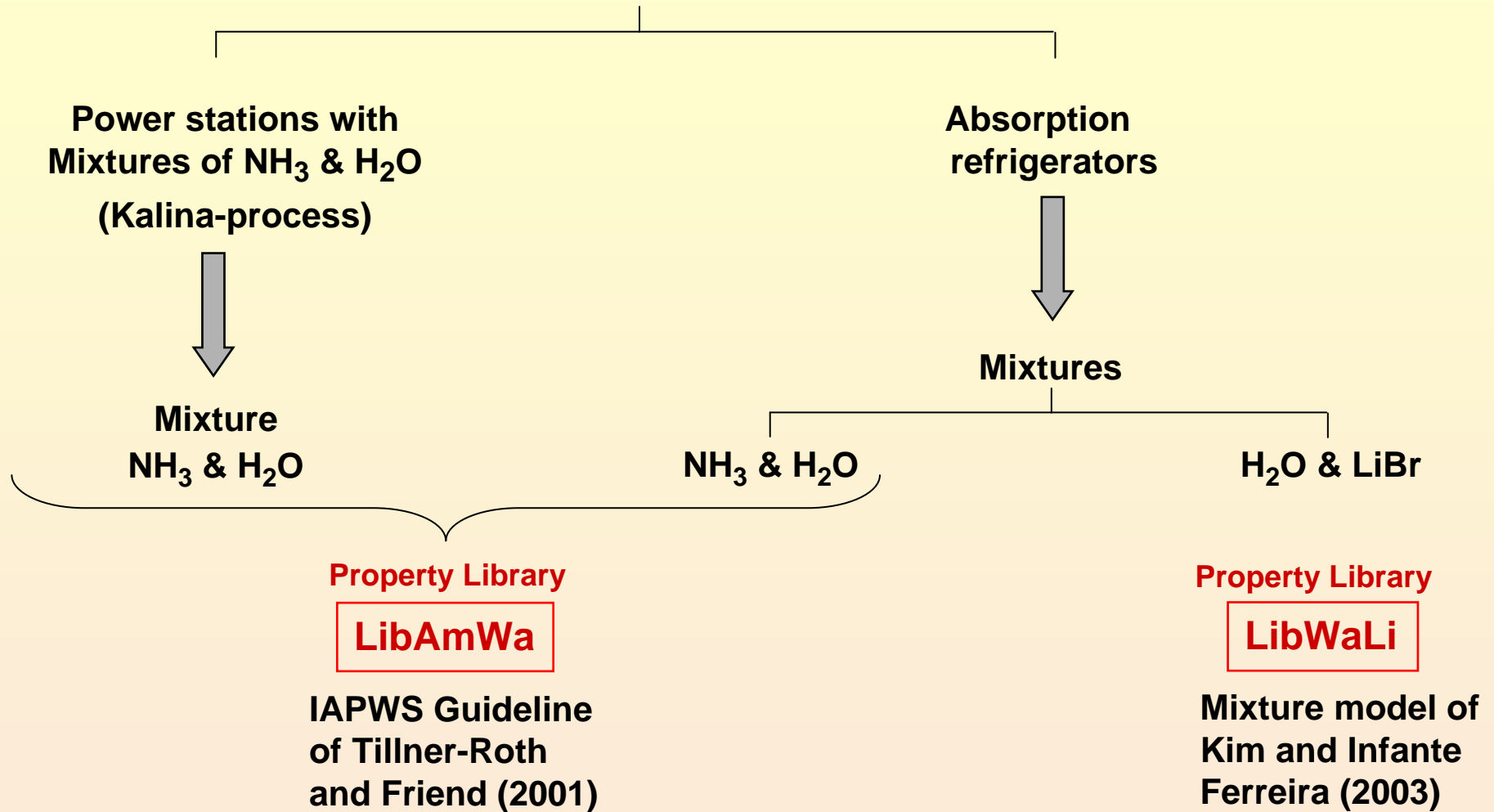
Property Library

**LibH2**

Equation of state of  
Leachman, Jacobson,  
and Lemmon

$\rho$   $c_p$

# Energy Conversion Processes with Working Fluid Mixtures



# Property Libraries

<p><b>Water and Steam</b></p> <p><b>Library LibIF97</b></p> <p>Industrial Formulation IAPWS-IF97</p>	<p><b>Humid Combustion Gases</b></p> <p><b>Library LibHuGas</b></p> <p>Ideal mixture of the real fluids</p> <p><b>Library LibIdGas</b></p> <p>Ideal gas mixture (VDI-Guideline 4670)</p>	<p><b>Humid Air</b></p> <p><b>Library LibAirWa</b></p> <p>Ideal mixture of the real fluids</p> <p><b>Library LibIdAir</b></p> <p>Ideal gas mixture</p>																												
<p><b>Carbon Dioxide</b></p> <p><b>Library LibCO2</b></p> <p>Formulation of Span and Wagner</p> <p><b>Hydrogen</b></p> <p><b>Library LibH2</b></p> <p>Formulation of Leachman et al.</p> <p><b>Helium</b></p> <p><b>Library LibHe</b></p> <p>Formulation of McCarty</p>	<p><b>Ideal Gas Mixtures</b></p> <p><b>Library LibIdGasMix</b></p> <p>Ideal mixture of the ideal fluids:</p> <table border="0" data-bbox="712 817 1447 1075"> <tbody> <tr> <td>Ar</td> <td>Air</td> <td>OH</td> <td>Ethylene</td> </tr> <tr> <td>Ne</td> <td>NO</td> <td>He</td> <td>Propylene</td> </tr> <tr> <td>N<sub>2</sub></td> <td>H<sub>2</sub>O</td> <td>F<sub>2</sub></td> <td>Propane</td> </tr> <tr> <td>O<sub>2</sub></td> <td>SO<sub>2</sub></td> <td>NH<sub>3</sub></td> <td>n-Butane</td> </tr> <tr> <td>CO</td> <td>H<sub>2</sub></td> <td>Methane</td> <td>Iso-Butane</td> </tr> <tr> <td>CO<sub>2</sub></td> <td>H<sub>2</sub>S</td> <td>Ethane</td> <td>Benzene</td> </tr> <tr> <td></td> <td></td> <td></td> <td>Methanol</td> </tr> </tbody> </table> <p><b>Mixtures in Absorption Processes</b></p> <p>Ammonia &amp; Water</p> <p><b>Library LibAmWa</b></p> <p>Water &amp; Lithiumbromide</p> <p><b>Library LibWaLi</b></p>	Ar	Air	OH	Ethylene	Ne	NO	He	Propylene	N <sub>2</sub>	H <sub>2</sub> O	F <sub>2</sub>	Propane	O <sub>2</sub>	SO <sub>2</sub>	NH <sub>3</sub>	n-Butane	CO	H <sub>2</sub>	Methane	Iso-Butane	CO <sub>2</sub>	H <sub>2</sub> S	Ethane	Benzene				Methanol	<p><b>Refrigerants</b></p> <p>Ammonia</p> <p><b>Library LibNH3</b></p> <p>R134a</p> <p><b>Library LibR134a</b></p> <p>Propane</p> <p><b>Library LibPropan</b></p> <p>Iso-Butane</p> <p><b>Library LibButan_Iso</b></p> <p>n-Butane</p> <p><b>Library LibButan_n</b></p>
Ar	Air	OH	Ethylene																											
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CO <sub>2</sub>	H <sub>2</sub> S	Ethane	Benzene																											
			Methanol																											

# The following **thermodynamic and transport properties** can be calculated:

## Thermodynamic Properties

- Saturation pressure  $p_s$
- Saturation temperature  $T_s$
- Density  $\rho$
- Specific volume  $v$
- Enthalpy  $h$
- Internal energy  $u$
- Entropy  $s$
- Exergy  $e$
- Isobaric heat capacity  $c_p$
- Isochoric heat capacity  $c_v$
- Isentropic exponent  $\kappa$
- Speed of sound  $w$
- Surface tension  $\sigma$

## Thermodynamic Derivatives

- All partial derivatives can be calculated.

## Transport Properties

- Dynamic viscosity  $\eta$
- Kinematic viscosity  $\nu$
- Thermal conductivity  $\lambda$
- *Prandtl*-number  $Pr$

## Backward Functions

- $T, v, s (p, h)$
- $T, v, h (p, s)$
- $p, T, v (h, s)$
- $p, T (v, h)$
- $p, T (v, u)$

## Example

Calculation of the specific enthalpy  $h$  for given pressure  $p$  and temperature  $t$  for steam using the Industrial Formulation IAPWS-IF97.

**Given Values:**       $p = 10 \text{ bar}$   
                               $T = 300 \text{ °C}$

**Calculation:**       $h = h(p, t, x)$

↑  
Vapor fraction  $x = -1$  formally for single-phase regions liquid or superheated steam

( $0 \leq x \leq 1$  for wet steam)

**Property library:**    **LibIF97**

**Function:**            **h\_ptx\_97**

**Interfaces:**

**Add-In FluidEXL<sup>Graphics</sup> for Excel<sup>®</sup>**

**Add-On FluidLAB for MATLAB<sup>®</sup>**

**Add-On FluidMAT for Mathcad<sup>®</sup>**



	A	B	C	D	E	F	G	H	I	J	K
1	<b>Example:</b>										
2	<b>Calculation of the Specific Enthalpy <math>h=f(p,t,x)</math> for Steam</b>										
3	<b>using IAPWS-IF97</b>										
4											
5	p	t	x	h	s						
6	bar	C	kg/kg	kJ/kg	kJ/kgK						
7	10	300	-1		7,1247						
8											
9											
10											
11											
12											
13	<div data-bbox="257 885 1198 1460" data-label="Complex-Block"> <p><b>Function Arguments</b></p> <p>h_ptx_97</p> <p>p in bar [A7] = 10</p> <p>t in °C [B7] = 300</p> <p>x in kg/kg [C7] = -1</p> <p>Specific enthalpy h in kJ/kg. = 3051,703186</p> <p><b>x in kg/kg</b> Vapor fraction</p> <p>Formula result = 3051,7032</p> <p><a href="#">Help on this function</a></p> <p>OK Cancel</p> </div>										
14											
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FluidEXL Graphics Eng

Calculate Diagrams Number Format

**Insert Function**

Search for a function:

Type a brief description of what you want to do and then click Go

Or select a category: Water IAPWS-IF97

Select a function:

- dv\_dT\_p\_ptx\_97
- e\_ptx\_tu\_97
- Eta\_ptx\_97
- h\_ptx\_97
- Kappa\_ptx\_97
- Lambda\_ptx\_97
- h\_ptx\_97 (p in bar)
- Specific enthalpy h in

[Help on this function](#)

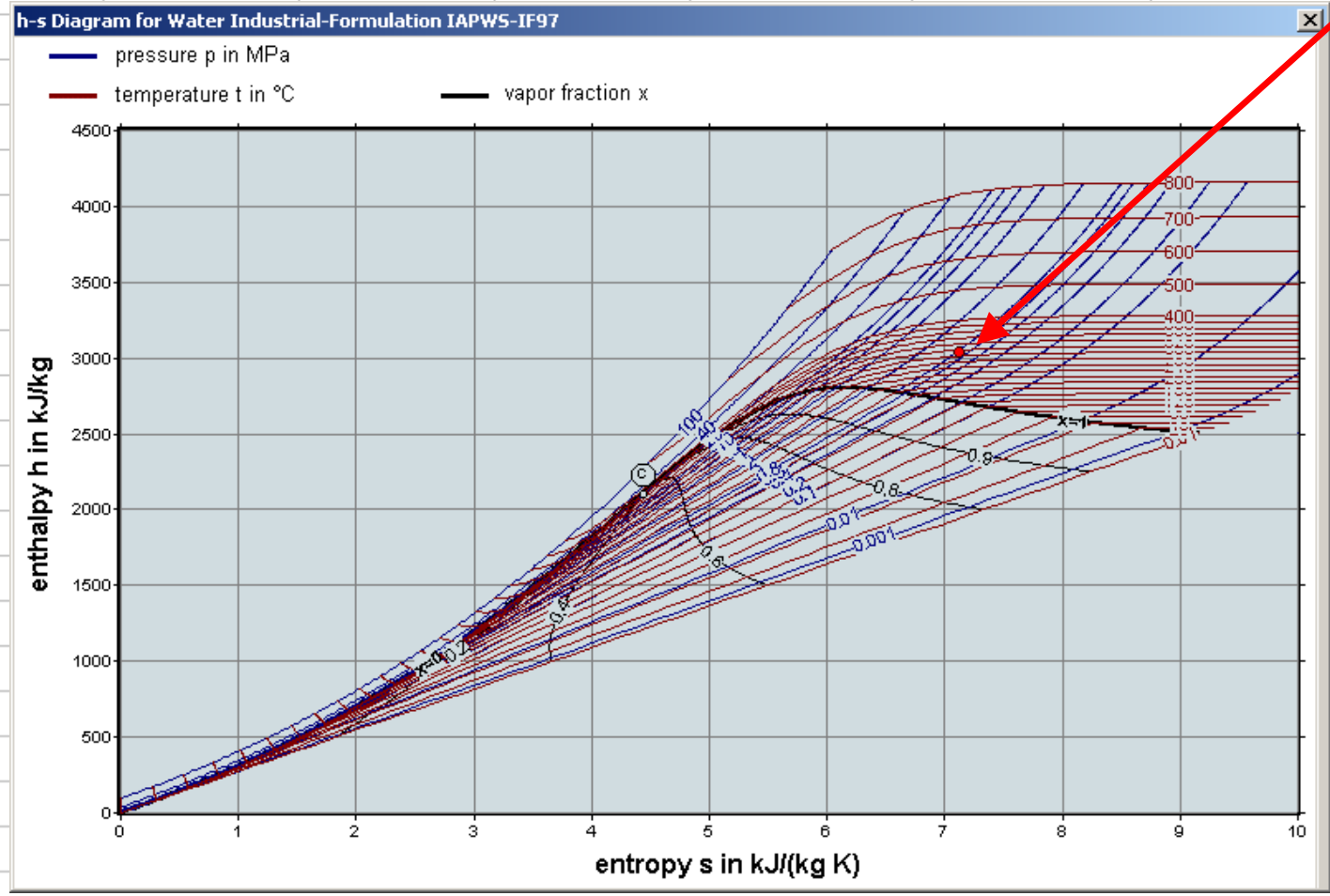
OK Cancel

	A	B	C	D	E	F	G	H	I	J	K
1	<b>Example:</b>										
2	<b>Calculation of the Specific Enthalpy <math>h = f(p,t,x)</math> for Steam</b>										
3	<b>using IAPWS-IF97</b>										
4											
5	p	t	x	h	s						
6	bar	C	kg/kg	kJ/kg	kJ/kgK						
7	10	300	-1	3051,7032	7,1247						

FluidEXL Graphics Eng

Calculate Diagrams Number Format

- T-s Diagram
- h-s Diagram**
- lg p-h Diagram
- lg p-lg v Diagram
- lg p-T Diagram
- p-T Diagram
- T-h Diagram
- T-lg v Diagram
- lg p-s Diagram
- h-lg v Diagram
- s-lg v Diagram
- h-x Diagram 0.101325 MPa
- h-x Diagram 0.11 MPa



MATLAB 7.3.0 (R2006b)

File Edit Debug Desktop Window Help

Current Directory: F:\Example\_h\_ptx\_97\_FluidLAB

Shortcuts How to Add What's New

Current Directory - F:\Example\_h\_ptx\_97\_FluidLAB

All Files	File Type	Description
Example_h_ptx_97.m	M-file	Example_h_ptx_97
h_ptx_97.mexw32	MEX-file	
LibIF97.dll	DLL File	
libifcoremdd.dll	DLL File	
libmmd.dll	DLL File	
libmmd.dll	DLL File	
msvc71d.dll	DLL File	

Editor - F:\Example\_h\_ptx\_97\_FluidLAB\Example\_h\_ptx\_97.m

```
1 % Example_h_ptx_97
2 %%
3 % Example:
4 % Calculation of the Specific Enthalpy h=f(p,t,x) for Steam
5 % Using IAPWS-IF97
6 %%
7 p= 10 ; % bar given pressure
8 t= 300 ; % °C given temperature
9 x= -1 ; % kg/kg vapor fraction in kg/kg (-1 for single phase region)
10 %%
11 h= h_ptx_97(p,t,x) % kJ/kg function call in FluidLAB
12 %
```

Function call of FluidLAB

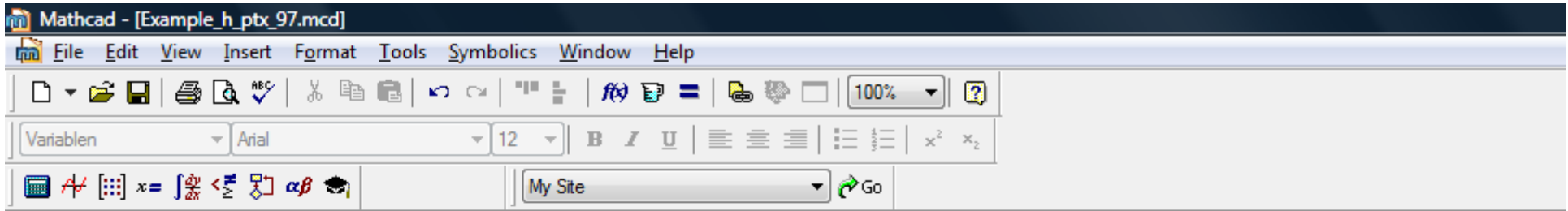
Command History

```
--->-- 05.11.07 11:33 -->
```

Command Window

```
h =
3.0517e+003
>> |
```

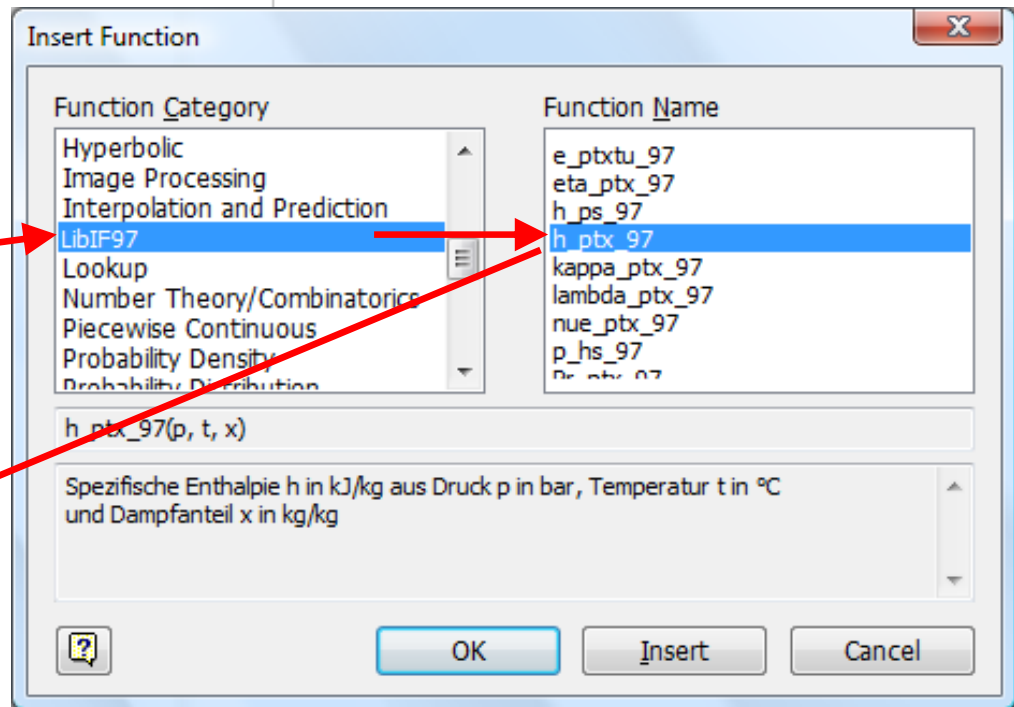
Result



**Example:**  
**Calculation of the Specific Enthalpy  $h = f(p,t,x)$  for Steam Using IAPWS-IF97**

$p := 10$  bar given pressure  
 $t := 300$  °C given temperature  
 $x := -1$   $\frac{\text{kg}}{\text{kg}}$  vapor fraction (-1 for single phase region)  
 $h :=$   $\frac{\text{kJ}}{\text{kg}}$  result for specific enthalpy

call a function of FluidMAT



**Result**

$h := h\_ptx\_97(p, t, x)$  call a function of FluidMAT  
 $h = 3051.703$   $\frac{\text{kJ}}{\text{kg}}$  result for specific enthalpy

# Property Software for Pocket Calculators

[www.steamtables-pocket-calculators.com](http://www.steamtables-pocket-calculators.com)

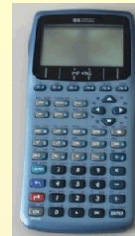
Software for calculating thermodynamic and transport properties for

- Water and steam
- Combustion Gases and
- Humid air

## FluidHP



HP 48



HP 49

## FluidCasio

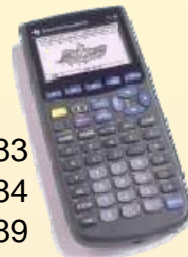


CFX-9850



FX1.0  
ALGEBRA  
FX 2.0

## FluidTI



TI 83  
TI 84  
TI 89

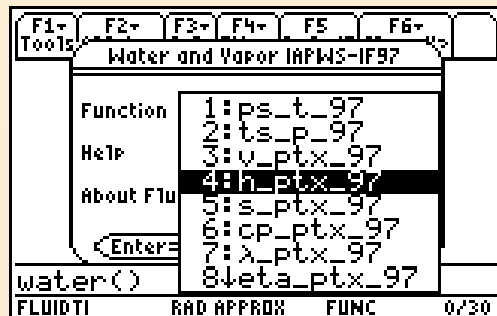


TI Voyage 200

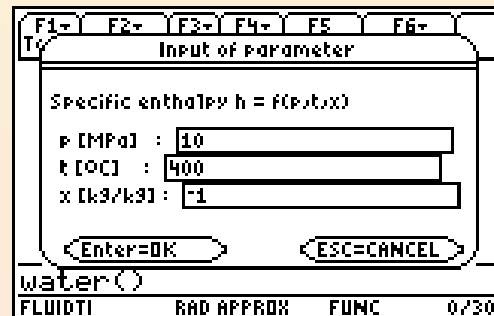


TI 92

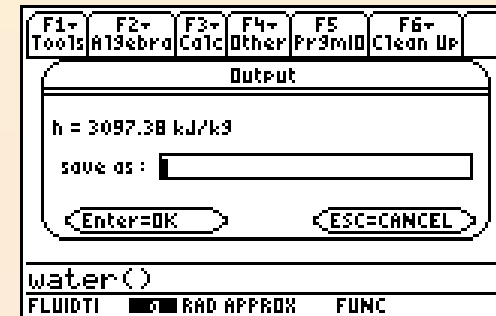
## Example: Calculation of the Enthalpy of Steam Using FluidTI



Choice of the function  $h = f(p,t,x)$



Input of the parameters  $p$ ,  $t$  and  $x$



Result for enthalpy

## Summary

- ▶ Property Libraries for working fluids used in energy conversion processes were developed.
- ▶ Thermodynamic properties, transport properties, thermodynamic derivatives, and backward functions can be calculated.
- ▶ The property libraries are available for
  - Excel<sup>®</sup>
  - MATLAB<sup>®</sup>
  - Mathcad<sup>®</sup>
  - Applications in Windows<sup>®</sup>, Unix<sup>®</sup> or Linux<sup>®</sup>
  - Pocket Calculators.
- ▶ Student versions of all property libraries are available.
- ▶ The libraries can be used by engineers, who routinely calculate heat cycles, turbines, boilers, heat pumps or other thermal or refrigeration processes.

**Paper available at: [www.thermodynamics-zittau.de](http://www.thermodynamics-zittau.de).**

