

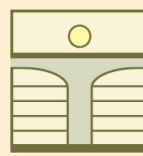
# Property Libraries and Software for Working Heat Cycles, Boilers, Turbines, Heat Pumps,

H.-J. Kretzschmar, I. Stöcker,

[www.thermodynamic-](http://www.thermodynamic-)

<p><b>Steam, Water, and Ice</b></p> <p><b>Libraries LibIF97, LibICE</b></p> <ul style="list-style-type: none"> <li>- Industrial Formulation IAPWS-IF97 (Revision 2007)</li> <li>- Supplementary Standards               <ul style="list-style-type: none"> <li>- IAPWS-IF97-S01</li> <li>- IAPWS-IF97-S03rev</li> <li>- IAPWS-IF97-S04</li> <li>- IAPWS-IF97-S05</li> </ul> </li> <li>- IAPWS Revised Advisory Note No. 3 on Thermodynamic Derivatives (2008)</li> <li>- Ice from IAPWS Formulation 2006</li> </ul>	<p><b>Humid Combustion Gas Mixtures</b></p> <p><b>Library LibHuGas</b></p> <p>Model: Ideal mixture of the real fluids:</p> <p>CO<sub>2</sub> - Span and Wagner      O<sub>2</sub> - Schmidt and Wagner          H<sub>2</sub>O - IAPWS-95              Ar - Tegeler et al.          N<sub>2</sub> - Span et al.</p> <p>and of the ideal gases:          SO<sub>2</sub>, CO, Ne (Scientific Formulation of Bückner et al.)</p> <p>Consideration of:          Dissociation from VDI Guideline 4670 und poynting effect</p> <p><b>Library LibIDGAS</b></p> <p>Model: Ideal gas mixture from VDI Guideline 4670</p>	<p><b>Humid Air</b></p> <p><b>Library LibHuAir</b></p> <p>Model: Ideal mixture of the real fluids:</p> <ul style="list-style-type: none"> <li>• Dry Air from Lemmon et al.</li> <li>• Steam, water, and ice from IAPWS-IF97 and IAPWS-06</li> </ul> <p>Consideration of</p> <ul style="list-style-type: none"> <li>• Condensation of steam</li> <li>• Dissociation from VDI Guideline 4670</li> <li>• Poynting effect from ASHRAE RP-1485</li> </ul> <p><b>Library LibIdAir</b></p> <p>Model: Ideal gas mixture from VDI Guideline 4670</p>																														
<p><b>Seawater</b></p> <p><b>Library LibSeaWa</b></p> <p>IAPWS-Formulation (2008) and IAPWS-IF97</p>	<p><b>Ideal Gas Mixtures</b></p> <p><b>Library LibIdGasMix</b></p> <p>Model: Ideal mixture of the ideal gases:</p> <table border="0"> <tr> <td>Ar</td> <td>H<sub>2</sub>O</td> <td>H<sub>2</sub>S</td> <td>Methane</td> <td>Butane</td> </tr> <tr> <td>Ne</td> <td>SO<sub>2</sub></td> <td>OH</td> <td>Ethane</td> <td>Isobutane</td> </tr> <tr> <td>N<sub>2</sub></td> <td>Dry air</td> <td>H<sub>2</sub></td> <td>Ethylene</td> <td>Benzene</td> </tr> <tr> <td>O<sub>2</sub></td> <td>Air nitrogen</td> <td>He</td> <td>Propylene</td> <td>Methanol</td> </tr> <tr> <td>CO</td> <td>NO</td> <td>F<sub>2</sub></td> <td>Propane</td> <td>Ammonia</td> </tr> <tr> <td>CO<sub>2</sub></td> <td></td> <td></td> <td></td> <td></td> </tr> </table> <p>Consideration of</p> <ul style="list-style-type: none"> <li>• Dissociation from VDI Guideline 4670</li> </ul>	Ar	H <sub>2</sub> O	H <sub>2</sub> S	Methane	Butane	Ne	SO <sub>2</sub>	OH	Ethane	Isobutane	N <sub>2</sub>	Dry air	H <sub>2</sub>	Ethylene	Benzene	O <sub>2</sub>	Air nitrogen	He	Propylene	Methanol	CO	NO	F <sub>2</sub>	Propane	Ammonia	CO <sub>2</sub>					<p><b>Dry Air</b></p> <p><b>Library LibRealAir</b></p> <p>Formulation of Lemmon et al. (2000)</p>
Ar	H <sub>2</sub> O	H <sub>2</sub> S	Methane	Butane																												
Ne	SO <sub>2</sub>	OH	Ethane	Isobutane																												
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<p><b>Carbon Dioxide and Dry Ice</b></p> <p><b>Library LibCO2</b></p> <p>Formulation of Span and Wagner (1994)</p>	<p><b>Ammonia / Water - Mixtures</b></p> <p><b>Library LibAmWa</b></p> <p>IAPWS Guideline 2001 of Tillner-Roth and Friend (1998)</p>	<p><b>Nitrogen</b></p> <p><b>Library LibN2</b></p> <p>Formulation of Span et al. (2000)</p>																														
<p><b>Ammonia</b></p> <p><b>Library LibNH3</b></p> <p>Formulation of Tillner-Roth (1995)</p>	<p><b>Water / Lithium Bromide - Mixtures</b></p> <p><b>Library LibWaLi</b></p> <p>Formulation of Kim and Infante Ferreira (2004)</p>	<p><b>Working Fluids for ORC Processes</b></p> <p><b>Siloxane C<sub>6</sub>H<sub>18</sub>OSi<sub>2</sub></b></p> <p><b>Library LibMM</b></p> <p><b>Siloxane C<sub>8</sub>H<sub>24</sub>O<sub>4</sub>Si<sub>4</sub></b></p> <p><b>Library LibD4</b></p> <p><b>Siloxane C<sub>10</sub>H<sub>30</sub>O<sub>5</sub>Si<sub>5</sub></b></p> <p><b>Library LibD5</b></p> <p><b>Siloxane C<sub>12</sub>H<sub>36</sub>O<sub>6</sub>Si<sub>6</sub></b></p> <p><b>Library LibD6</b></p> <p><b>Siloxane C<sub>8</sub>H<sub>24</sub>O<sub>2</sub>Si<sub>3</sub></b></p> <p><b>Library LibMDM</b></p> <p><b>Siloxane C<sub>10</sub>H<sub>30</sub>O<sub>3</sub>Si<sub>4</sub></b></p> <p><b>Library LibMD2M</b></p> <p><b>Siloxane C<sub>12</sub>H<sub>36</sub>O<sub>4</sub>Si<sub>5</sub></b></p> <p><b>Library LibMD3M</b></p> <p><b>Siloxane C<sub>14</sub>H<sub>42</sub>O<sub>5</sub>Si<sub>6</sub></b></p> <p><b>Library LibMD4M</b></p> <p>Formulationen of Colonna et al. (2006, 2008)</p>																														
<p><b>Methanol</b></p> <p><b>Library LibCH3OH</b></p> <p>Formulation of de Reuck and Craven</p>	<p><b>Propane</b></p> <p><b>Library LibPropane</b></p> <p>Formulation of Lemmon et al. (2008)</p>	<p><b>R134a</b></p> <p><b>Library LibR134a</b></p> <p>Formulation of Tillner-Roth and Baehr (1994)</p>																														
<p><b>Ethanol</b></p> <p><b>Library LibC2H5OH</b></p> <p>Formulation of Dillon and Penoncello (2004)</p>	<p><b>Iso-Butane</b></p> <p><b>Library LibButane_Iso</b></p> <p>Formulationen of Bückner et al. (2003)</p>	<p><b>n-Butane</b></p> <p><b>Library LibButane_n</b></p> <p>Formulationen of Bückner et al. (2003)</p>																														

# Fluids for Calculating and Refrigeration Processes



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## FluidEXL Graphics for Excel®

Calculating an isentropic expansion

Menu bar of FluidEXL

Name of the property library

Function in FluidEXL

Menu for input of given property values

Available diagrams for water and steam

Displaying the calculated property values in different diagrams

The following diagrams are available  
Water and Steam :  
T-s diagram  
h-s diagram  
log p-h diagram  
log p-s diagram  
p-T diagram  
log p-T diagram  
h-log v diagram  
log p-log v diagram  
T-h diagram  
T-log v diagram  
s-log v diagram  
Humid Air :  
h-x diagram for  $p = 0.101325$  MPa  
h-x diagram for  $p = 0.1$  MPa

## FluidMAT for Mathcad®

Name of the property library

Function call of FluidMAT

## FluidEES for Engineering Equation Solver® EES

Function call of FluidEES

## FluidDYM for DYMOLA®, SimulationX®

Function call of FluidDYM

## FluidLAB for MATLAB®

Function call of FluidLAB

## FluidVIEW for LabVIEW®

Function call of FluidVIEW

The following thermodynamic and transport properties can be calculated<sup>a</sup>

### Thermodynamic Properties

- Vapor pressure  $p_s$
- Saturation temperature  $T_s$
- Density  $\rho$
- Specific volume  $v$
- Enthalpy  $h$
- Internal energy  $u$
- Entropy  $s$
- Exergy  $e$
- Isobaric heat capacity  $c_p$
- Isochoric heat capacity  $c_v$
- Isentropic exponent  $\kappa$
- Speed of sound  $w$
- Surface tension  $\sigma$

### Transport Properties

- Dynamic viscosity  $\eta$
- Kinematic viscosity  $\nu$
- Thermal conductivity  $\lambda$
- Prandtl-number  $Pr$

### Backward Functions

- $T, v, s(p, h)$
- $T, v, h(p, s)$
- $p, T, v(h, s)$
- $p, T(v, h)$
- $p, T(v, u)$

### Thermodynamic Derivatives

- Partial derivatives can be calculated.

<sup>a</sup> Not all of these property functions are available in all property libraries listed before.