

A New IAPWS Standard on the Fast Calculation of Real Fluid Properties with the Spline-Based Table Look-up Method (SBTL) and its Application in CFD

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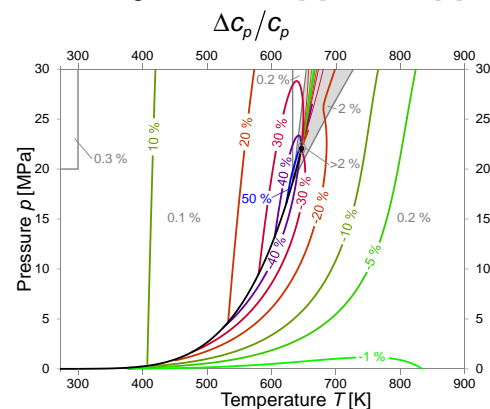
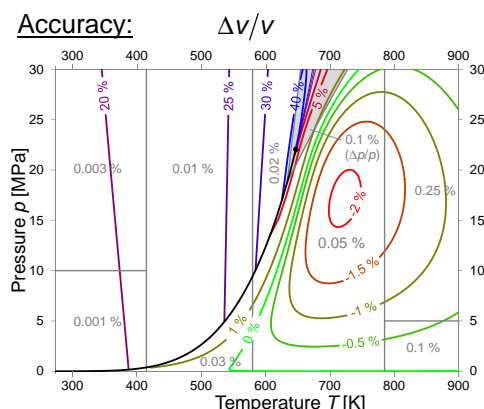
Motivation & Objectives

Problem Statement:

- Deviations in calculated fluid properties lead to inaccurate mass, energy, and entropy balances. → Property calculation algorithms need to be very accurate.
- Fluid properties are calculated extremely often, which consumes the majority of the computing time. → Property functions need to be extremely fast.
- CFD solvers require continuity and numerical consistency of the equations to be solved. → Property functions need to be continuous and consistent.

Real Fluid Properties in CFD (example: water and steam):

- Equations of State (EOS):**
 - Cubic EOS, e.g., Peng-Robinson EOS (PR-EOS)
 - Fundamental EOS, e.g., IAPWS-95 [1] or -IF97 [2]



Colored contours: deviations of PR-EOS from IAPWS-95
Gray figures: uncertainties of IAPWS-95 (those of IAPWS-IF97 are slightly higher)

Computing-Time Ratio (CTR):

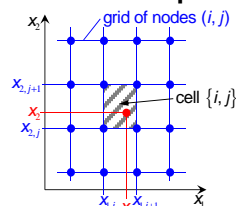
$$CTR = \frac{\text{Comp. Time of IAPWS-IF97 (-95)}}{\text{Comp. Time of PR-EOS}}$$

Function	IAPWS-IF97 Region	
	1 (liquid)	2 (vapor)
$p(v,u)$	4.8 (88)	9.0 (114)
$T(v,u)$	4.8 (91)	9.3 (115)
$T(p,h)$	0.41 ^{a)} (23)	0.60 ^{a)} (43)
$v(p,h)$	0.48 ^{a)} (23)	0.91 ^{a)} (43)

Phase/region tests are not included in these CTR values and increase the computing times even further!

a) IAPWS-IF97 backward equation and one Newton step

Table Look-Up Methods (interpolation from tabulated values):



Calculation of any property $z(x_1, x_2)$:

- Discrete values $z_{ij}(x_{1,i}, x_{2,j})$ are calculated at the nodes (i, j) from an equation of state and stored in a look-up table.
- During the CFD simulation, the cell $\{i, j\}$ in the grid of nodes is to be determined and $z(x_1, x_2)$ is interpolated.

Accuracy and computing speed depend on the structure of the grid of nodes and the applied interpolation algorithm.

Shortcomings of currently applied methods:

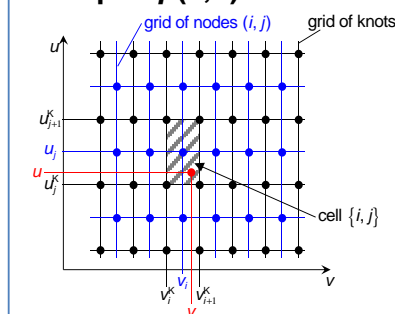
- Nodes are often clustered to consider the nonlinear behavior of the fluid property function, which leads to computationally intensive cell search algorithms.
- Most frequently applied property functions are often calculated from inverse functions, rather than from an explicit forward function.
- Bi-linear interpolation cannot provide continuous 1st derivatives.
- Bi-cubic interpolation leads to computationally intensive inverse functions.

Objectives of this Project:

- Development of new table look-up algorithms that overcome the shortcomings outlined above and provide:
- fast and accurate property functions with cont. 1st derivatives
 - fast and numerically consistent inverse functions

Spline-Based Table Look-up Method (SBTL)

Example: $p(v,u)$



- Variable transformations (e.g., $v \rightarrow \bar{v}$) to:
 - enhance accuracy (linearization)
 - to reshape the range of state
- Definition of a rectangular, piecewise equidistant grid of nodes (fast cell search alg.)
- Definition of cells in the grid of knots
- Calculation of all coefficients a_{ijkl} of the bi-quadratic spline-polynomial (cont. 1st derivatives):

$$p_{\{i,j\}}(\bar{v}, u) = \sum_{k=1}^3 \sum_{l=1}^3 a_{ijkl} (\bar{v} - \bar{v}_i)^{k-1} (u - u_j)^{l-1}$$

Inverse Functions, e.g., $u(p,v)$:

$$u_{\{i,j\}}^{NV}(p, \bar{v}) = \frac{-B \pm \sqrt{B^2 - 4AC}}{2A} + u_j$$

$$A = a_{ij13} + \Delta \bar{v}_i (a_{ij23} + a_{ij33} \Delta \bar{v}_i)$$

$$B = a_{ij12} + \Delta \bar{v}_i (a_{ij22} + a_{ij32} \Delta \bar{v}_i)$$

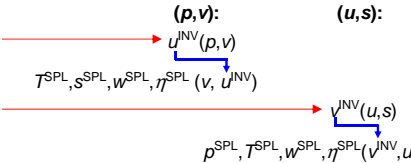
$$C = a_{ij11} + \Delta \bar{v}_i (a_{ij21} + a_{ij31} \Delta \bar{v}_i) - p$$

$$\Delta \bar{v}_i = \bar{v}_i (\bar{v} - \bar{v}_i) \quad (\pm) = \text{sign}(B)$$

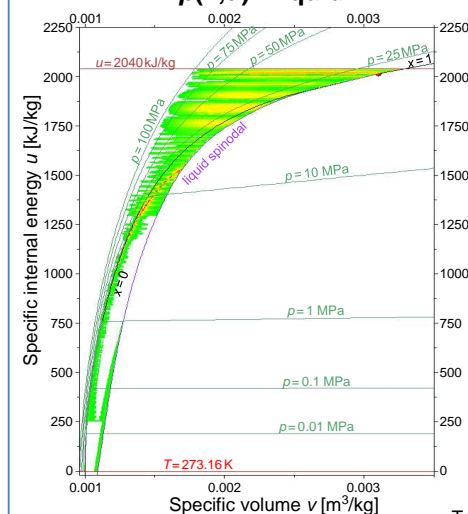
SBTL functions of (v,u) :

- Pressure $p^{SPL}(v,u)$
- Temperature $T^{SPL}(v,u)$
- Spec. entropy $s^{SPL}(v,u)$
- Speed of sound $w^{SPL}(v,u)$
- Dynamic viscosity $\eta^{SPL}(v,u)$

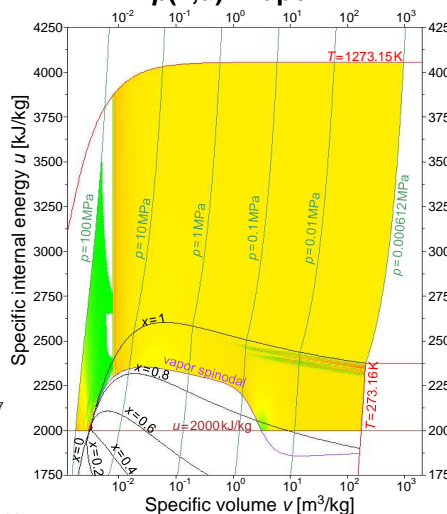
Calculation of inverse functions: $(p,v) \rightarrow (u,s)$:



$p(v,u)$ - liquid



$p(v,u)$ - vapor



Transformations:

$$\bar{v}(v,u) = \frac{v - v(u)}{v(u)_{p_{\max}} - v(u)_{p_{\max}}} (\bar{v}_{\max} - \bar{v}_{\min}) + \bar{v}_{\min}$$

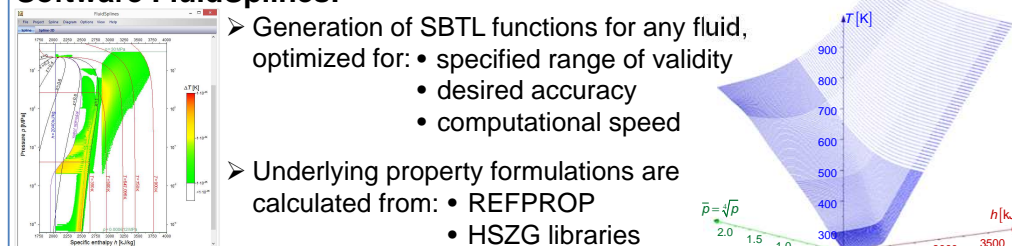
$$\bar{v}(v) = \ln(v)$$

Accuracy and Computing-Time Ratio (CTR):

Function	Max. deviation from IAPWS-IF97		IAPWS-IF97 Region		
	liquid	vapor	1 (liquid)	2 (vapor)	4 (two-phase)
$p(v,u)$	≤ 2.5 MPa: $ \Delta p/p < 0.12\%$ > 2.5 MPa: $ \Delta p < 0.6$ kPa	$ \Delta p/p < 0.001\%$	130	271	19.6
$T(v,u)$	$ \Delta T < 1$ mK	$ \Delta T < 1$ mK	161	250	20.6
$s(v,u)$	$ \Delta s < 10^{-6}$ kJ kg ⁻¹ K ⁻¹	$ \Delta s < 10^{-6}$ kJ kg ⁻¹ K ⁻¹	197	309	-
$w(v,u)$	$ \Delta w/w < 0.001\%$	$ \Delta w/w < 0.001\%$	2.0	6.4	5.6
$\eta(v,u)$	$ \Delta \eta/\eta < 0.001\%$	$ \Delta \eta/\eta < 0.001\%$	43.5	66.4	16.2

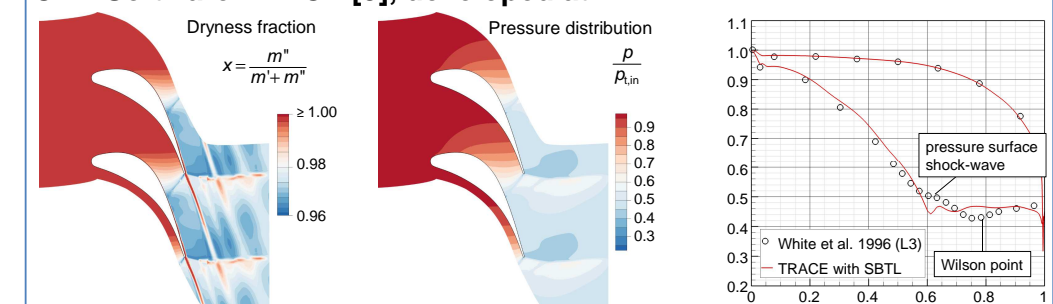
Software FluidSplines:

- Generation of SBTL functions for any fluid, optimized for:
 - specified range of validity
 - desired accuracy
 - computational speed
- Underlying property formulations are calculated from:
 - REFPROP
 - HSZG libraries



Application of the SBTL Method

Simulation of Condensing Steam Flow Around a Fixed Blade with the CFD-Software TRACE [3], developed at DLR:



Inlet: $p_{\text{in}} = 41.7$ kPa
 $T_{\text{in}} = 357.5$ K ($\Delta T_s = +7.5$ K)

Outlet: $p_{\text{out}} = 20.6$ kPa

Assumptions:

- equilibrium condensation (no sub-cooling considered)
- homogeneous two-phase flow

Key Results:

- The numerical results show negligible differences from those obtained with the direct application of IAPWS-IF97.
- Computing times for flow simulations considering the real fluid behavior are reduced by a factor of 10 with regard to simulations based on IAPWS-IF97.
- With regard to the application of the ideal-gas model, the computing times are increased by a factor of 1.4 only.

Further Applications (Selection):

- RELAP-7 (nuclear-reactor system safety analysis code, developed at the Idaho National Laboratory (INL)):**
 - simplified property calculation algorithms have been replaced with fast and accurate SBTL functions; applied in a 7-eq. non-equilibrium two-phase model
- KRAWAL (heat-cycle calculation software for power plant design, developed at SIEMENS PG):**
 - the overall computing time is reduced by 50% with regard to calculations based on IAPWS-IF97

Conclusions and Outlook

The newly developed SBTL method [4,5,6]:

- enables the consideration of the real fluid behavior in CFD and other computationally intensive process simulations with high accuracy and low computing times.
- can be applied to any fluid (SBTL functions can be generated with FluidSplines).
- is being applied successfully in numerical process simulations.
- is being extended for mixtures, e.g., humid air and humid combustion gases.

A nucleation model is being implemented in TRACE to consider sub-cooling.

References/Publications

- IAPWS, *Revised Release on the IAPWS Formulation 1995 for the Thermodynamic Properties of Ordinary Water Substance for General and Scientific Use* (2014), available at <http://www.iapws.org>.
- IAPWS, *Revised Release on the IAPWS Industrial Formulation 1997 for the Thermodynamic Properties of Water and Steam* (2007), available at <http://www.iapws.org>.
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